

Investigation of Variability of Primary Materials on the Intrinsic Dissolution Behavior of Carbamazepine

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1. Summary

Carbamazepine (CBZ) is a poorly water soluble drug, classified as class II according to the Biopharmaceutics Classification System and exhibits at least four polymorphic forms and a dihydrate. CBZ polymorphs have different crystal structures and exhibit different melting points, chemical reactivity, solubility and compactibility, all of which can contribute to the differences in their bioavailability. In aqueous solution, CBZ anhydrous has ability to convert to dihydrate form, and the kinetic of that conversion is important for the dissolution of the drug. Commercially available raw material can contain a mixture of CBZ polymorphs as well as amorphous parts.

The aim of the present study was to investigate the effect of the variability of different commercially available CBZ samples on the intrinsic dissolution behavior in order to recommend a strategy to maintain product quality by monitoring the variability of critical parameters of the bulk drug.

Therefore, extensive physical characterization of nine anhydrous CBZ samples from three different sources was carried out. Polymorphism (by X-ray powder diffraction - XRPD and Fourier transformation infrared - FTIR microspectroscopy), thermal behavior (by differential scanning calorimetry - DSC, hot stage microscopy - HSM), particle size/particle size distribution, morphology, and solubility were investigated.

The results showed that the commercial anhydrous CBZ samples exhibited the same polymorphic form, but different morphology, particle size and size distribution, which led to a variation in the kinetics of conversion from anhydrous to the dihydrate form of CBZ and therefore to variation in the kinetics of solubility. The detected variability was suggested to be attributed to variations in the manufacturing processes, such as the use of different solvents in the crystallization stage and/or grinding of the crystals in the final stage of the manufacture of CBZ.

Furthermore, disc intrinsic dissolution rate (DIDR) tests of the CBZ samples were conducted in the order to investigate if the DIDR test can provide information about the kinetics of conversion of anhydrous CBZ to its dihydrate form. For that purpose, compacts of pure raw material were prepared using Zwick material tester. The compacts were imbedded in paraffin leaving only one side free to be exposed to the dissolution media.

CBZ anhydrous samples showed different intrinsic dissolution behavior. Moreover examined compacts within one sample have shown high standard deviation. Intrinsic dissolution parameters were determined with scope to calculate the transition point of anhydrous to dihydrate conversion for each sample, which was found to vary among the CBZs obtained from different sources between 15 and 25 minutes.

Carbamazepine dihydrate samples were crystallized from anhydrous samples in order to be tested on intrinsic dissolution behavior and were characterized by XRPD and DSC to confirm complete dihydrate formation. It was found that all previously detected variations between the different samples were significantly reduced, and all nine samples had constant characteristics. When dihydrate samples were investigated on intrinsic dissolution behavior, the results showed that deviation within one group of samples were reduced and the variations between dihydrates prepared from anhydrous CBZ from different sources did not exist anymore.

Considering that excipients can influence phase transformation of CBZ anhydrous to its dihydrate form, binary mixtures of CBZ (from different sources) and Fast Flo[®] lactose were investigated in this study. Mixtures with different ratios of drug and excipient were compacted to the same porosity, and disintegration time and intrinsic dissolution behavior of the produced compacts were studied. The results showed that the selected excipient had no influence on the anhydrate dihydrate conversion.

As a final step in this study, it was proposed to examine if the results obtained for the transition point of anhydrous form to dihydrate can be used to predict the dissolution behavior of CBZ in model formulation. For this purpose, formulations of CBZ were prepared by direct compaction process using different CBZs and Ludipress[®], which were subsequently analyzed for disintegration time and dissolution. It turned out that the amount of CBZ dissolved after 15 minutes showed the same order (CBZ B > CBZ A > CBZ P) being identical to the time event of the transition point determined by intrinsic dissolution test, meaning CBZ B had the earliest and CBZ P the latest transition point. Therefore, the intrinsic dissolution test turned out to be a valuable and simple monitoring tool for characterization of CBZ raw materials, to detect the variability of primary material, to be employed for the determination of the transition point and to be used for estimation of CBZ dissolution behavior.

2. Introduction

2.1. PAT

The aim of process analytical technology (PAT) is to understand and control the manufacturing process which is consistent with the following quality system: quality should not be tested into products; it should be built-in or should be by design. PAT is a new concept for designing, analyzing and controlling manufacturing through timely measurements (i.e. during processing) of critical quality and performance attributes of raw and in-process materials and also of processes with the goal of ensuring final product quality (FDA, 2004).

There are many current and new process analytical tools available that enable scientific and risk-managed pharmaceutical development, manufacture, and quality assurance. These tools, when used within a system can provide effective and efficient means for acquiring information to facilitate process understanding, develop risk-mitigation strategies, achieve continuous improvement, and share information and knowledge. In the PAT framework, these tools can be categorized as:

- multivariate data acquisition and analysis tools
- modern process analyzers or process analytical chemistry tools
- process and endpoint monitoring and control tools
- continuous improvement and knowledge management tools

A desired goal of the PAT framework is to design and develop processes that can consistently ensure a predefined quality at the end of the manufacturing process. Such procedures would be consistent with the basic tenet of quality by design and could reduce risks to quality and regulatory concerns while improving efficiency. Gains in quality, safety and/or efficiency will vary depending on the product and are likely to come from:

- reducing production cycle times by using on-, in-, and/or at-line measurements and controls
- preventing rejects, scrap, and re-processing
- considering the possibility of real time release
- increasing automation to improve operator safety and reduce human error

- facilitating continuous processing to improve efficiency and manage variability by using small-scale equipment (to eliminate certain scale-up issues) and dedicated manufacturing facilities or by improving energy and material use and increasing capacity (FDA, 2004).

2.2. Preformulation

Preformulation is a stage of drug development during which physicochemical and mechanical properties of a compound are investigated, understood and effectively utilized. In other words, the objective of preformulation studies is to develop a portfolio of information about the drug substance to serve as a set of parameters against which detailed formulation design can be carried out (Augsburger et al., 2002). Preformulation investigations are designed to identify those physicochemical properties of drug substances and excipients that may influence the formulation design, method of manufacture, and pharmacokinetic-biopharmaceutical properties of the resulting product. Preformulation studies include the evaluation of different parameters which are summarized in table 2.1.

Identifying the key issues (critical parameters) prior to development will ultimately expedite product development minimizing risk-associated mistakes. Preformulation testing provides the necessary physicochemical and physicomachanical properties of drug and excipient at the early stage of development to allow a logical, scientific approach to formulation optimization. The best products can be regarded as being those that are simple, elegant and robust. There is a greater chance of achieving such a product if the correct foundations are laid and an understanding of the potential problems has been obtained by rigorous preformulation testing (Augsburger et al., 2002).

The term “preformulation studies” is often used for a development of newly synthesized drug compounds, but it is also an extremely important stage during the development of generic drugs. For a generic drug to be approved by the authorities it must be shown to be pharmaceutically equivalent and bioequivalent to the reference drug product. Pharmaceutically equivalent means the identical amounts of the same active ingredient in the same dosage form and for the same route of administration.

Table 2.1 Preformulation parameters

	properties	Importance
Identity/ content		An essential part of preformulation is to be able to monitor the drug compound, degradation products or related substances
Solid state properties	Polymorphism/ pseudopolymorphism Crystal habit Crystal defects	E.g. metastable polymorphs have a faster dissolution rate than the stable forms, apparently have a greater equilibrium solubility and bioavailability. But by definition, metastable forms will tend to convert to stable ones and transition can occur gradually or can be accelerated by changes in storage conditions or just by mechanical treatment of the drug (mixing, milling, tableting) Powder flow, compressibility/ compactibility influence on dissolution rate, e.g. 1) needle-like particles show better compressibility/compactibility than plate shaped particles; e.g. 2) needle particles have bigger surface and therefore higher dissolution rate is expected but they will have poorer flow properties Disruption in crystal lattice can result in major changes in the processing of the drug e.g. high number of crystal defect is characteristic for brittle materials, very low number of crystal defect is leads to plasticity of material; its chemical reactivity, dissolution rate and then bioavailability
Physico- mechanical properties	Particle size distribution Density (true, bulk and tap) Surface area Wettability Hygroscopicity Flowability Compressibility/compactibility	Processability and dissolution rate for computation of void volume or porosity of packed powder beds, flowability, compressibility dissolution rate, bioavailability Poorly wettable compounds have limited interface with the liquid, which slows dissolution, the ability of compound to absorb the water can lead to chemical instability Good powder flow properties are essential for uniform filling into dies of tableting machines and therefore for accurate dosing Mechanical behavior of powder with elastic, plastic or brittle behavior under pressure; essential to avoid problems of capping of tablets mechanical behavior of powder with elastic, plastic or brittle behavior under pressure
Solubility analysis	Solubility, pH-solubility profiles pK _a , partition coefficient dissolution profile	Solubility properties are essential for dissolution and bioavailability Important information about chemical stability of drug prediction for a drug to move from an aqueous compartment into a membrane
Stability	Chemical stability Compatibility	Degradation process has to be predicted Influence of excipient on stability or solubility of the drug

Bioequivalence is defined as the absence of a significant difference in the bioavailability of the drug when administered at the same molar dose under similar conditions.

The development of a drug formulation for the commercial market requires a tremendous effort in order to assure constant quality of the product, i.e. its ability to deliver the therapeutic effect for which it was intended.

The generic industry relies in major part on the publicly available information and through literature research it tries to minimize unnecessary experimentation. Unfortunately sometimes only small amount of data is available and if the preformulation studies are not conducted formulators must rely on their experience to predictions based on the reactivity of the functional groups present in the active pharmaceutical ingredient (API) and thus they design a product using excipient that will minimize the anticipated degradation.

Variability in the properties of the primary materials, both active and excipients can “spoil” the enormous effort spent on the development if the effects of such variability are not well understood.

Since many of generic companies are not synthesizing active ingredients for their formulation, they are directly dependent on drug producers. As the formulator cannot rely only on the specification provided by the supplier of bulk drug, preformulation studies in that case are extremely important during selection of the best raw material for the formulation of the dosage form and the most reliable manufacturer which will provide the active materials of consistently high quality and without batch to batch variation. Moreover, the generic product manufacturer must sometimes change the source of bulk drug due to market fluctuation. Hence, it is necessary to specify the critical parameters for each drug which will be monitored in order to control variability during the selection of new raw materials if there is a need for it.

3. Theoretical section

3.1. Crystal Structure

Crystal is a solid in which the constituent atoms, molecules or ions are packed in regularly ordered, repeating pattern extending in all dimensions. The three-dimensional geometric arrangement of atoms, molecules or ions (unit cells) composing a crystal is called *crystal lattice*. In the solid state, the atoms of a molecule may be arranged in one of seven fundamental unit cells: triclinic, monoclinic, orthorhombic, tetragonal, trigonal, hexagonal or cubic (Brittain, 1999, Florence et al., 1998). These seven types of unit cells may have atoms or molecules not only at each corner of the unit cell but certain of them may also have unit cell with atoms or molecules at the center of the top and bottom faces, *end-centered* (monoclinic and orthorhombic), at the center of every face, *face-centered* (cubic and orthorhombic) or with a single atom in the center of the crystal *body-centered* (cubic, tetragonal or orthorhombic). All together there are 14 possible types of unit cell - *Bravais lattices*. All the crystalline forms which are known in organic or inorganic chemistry may be encountered (figure 3.2) (Brittain,1999).

The crystal of a given substance may vary in size, relative development of the given faces and the number and kind of faces present which means that they have different *crystal habit*. The crystal habit describes the shape of crystal in rather general term and includes for example acicular (needle), prismatic, pyramidal, tabular, columnar, lamellar types etc. Figure 3.1 shows the some of the crystal habits of hexagonal crystal. The habit of crystal is of pharmaceutical importance, since it affects the compression characteristics and flow properties of the drug during tableting (Florence et al., 1998).

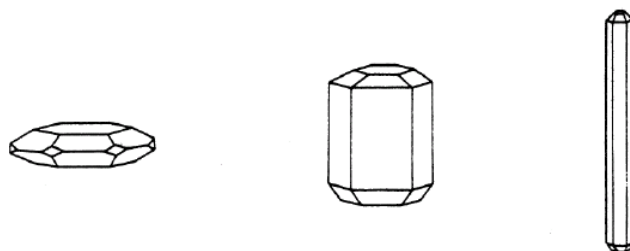
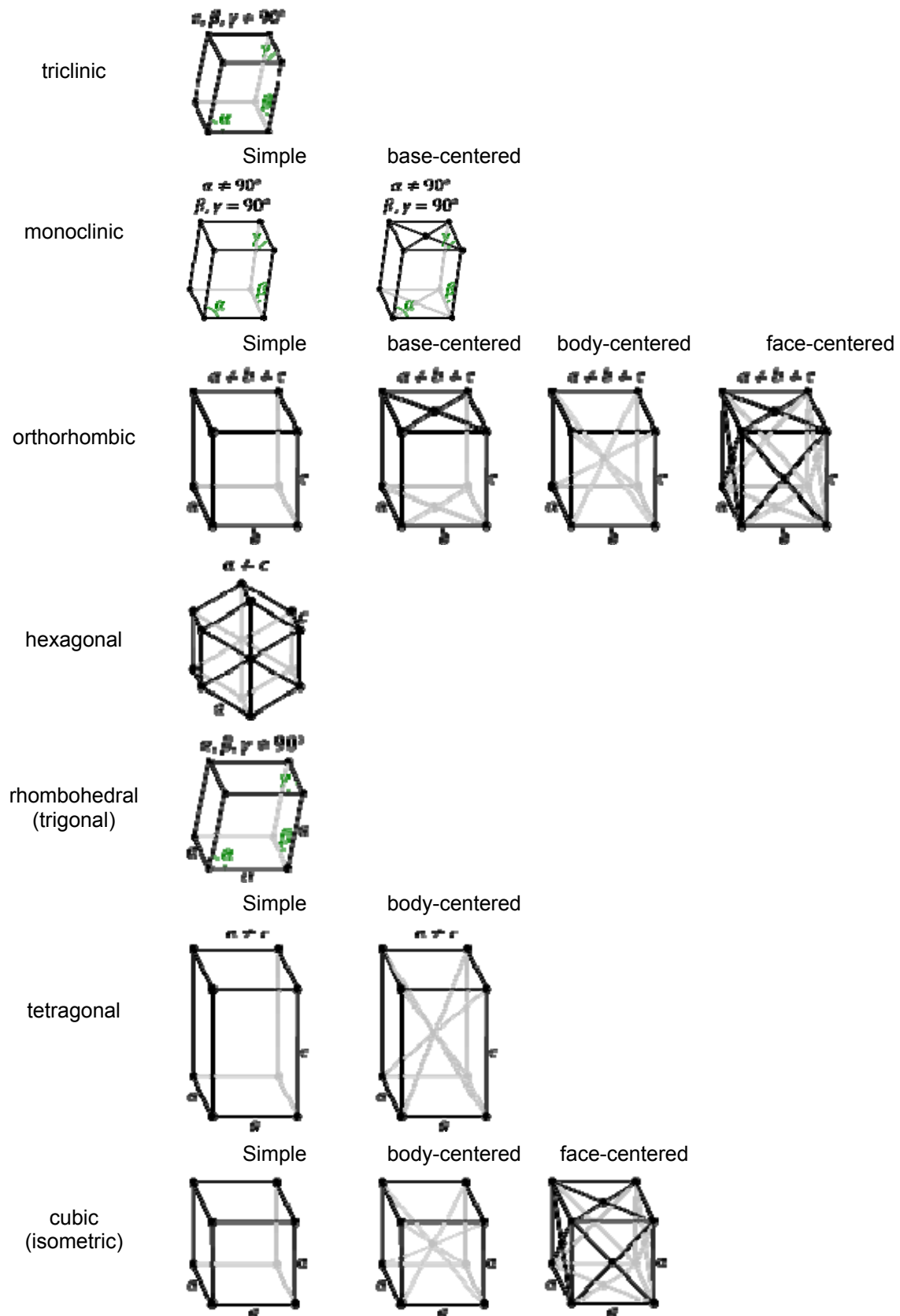


Figure 3.1 Different shapes of crystal (plate, prismatic, needle)

Crystal system

Lattices:



3.2. Polymorphism

Many pharmaceutical solids can exist in different physical forms. Polymorphism may be defined as the ability of a compound to crystallize in two or more crystalline phases with different arrangements and/or conformations of the molecule in the crystal lattice. Therefore, polymorphs are different crystalline forms of the same pure chemical compound. The phenomenon of polymorphism in molecular crystals is analogous to allotropism among elements (Grant, 1989).

Solvates (pseudo-polymorphs) are crystalline solid adducts containing either stoichiometric or nonstoichiometric amounts of a solvent incorporated within the crystal structure. If the incorporated solvent is water, the solvates are also commonly known as hydrates (Grant, 1989).

Hydrates are the most important subclass of solvates. They can be classified into three categories (Vippaguanta et al., 2001):

- isolated site hydrates, where the water molecules are isolated from direct contact with other water molecules by drug molecules,
- channel hydrates, where the water molecules are located next to each other along one direction in the lattice, forming “channels” through the crystal,
- ion associated hydrates, which contain metal ion coordinated water.

In hydrates, water occupies definite position in the crystal lattice, usually by forming hydrogen bonds with the anhydrate molecules. The stability of hydrates, beside by pressure and temperature, is governed by the water activity of the environment and the intermolecular bonding and arrangement of molecules in the lattice. The critical water activity determines whether the stable form is the anhydrate or the hydrate one.

Grant and Higuchi have established the following relationship to describe the equilibrium between a hydrate and anhydrate (Grant et al., 1990):



$$K_h = \frac{a[A \cdot mH_2O(solid)]}{a[A(solid)]a[H_2O]^m} \quad \text{Equation 3.2}$$

where:

K_h is the equilibrium constant for the process,

$a[A \cdot mH_2O(solid)]$, $a[A(solid)]$ and $a[H_2O]$ are thermodynamic activities of the hydrate, the anhydrate and water,

m is the number of water moles taken up by one mole of the anhydrate.

When $a[H_2O] > [a[A \cdot mH_2O(solid)] / a[A(solid)]K_h]^{1/m}$, the more stable form is hydrate (Grant et al., 1990).

In other words, hydrates are more stable than their anhydrate counterparts at conditions below dehydration temperature and above critical water activity, such as high humidity or saturated solution. Isolated hydrates usually dehydrate at relatively high temperature. The dehydration process of such hydrates is destructive for the crystal since it requires rearrangement of the molecules in the unit cell in order to allow water molecules to escape the lattice.

Channel hydrates usually dehydrate at lower temperatures than isolated site hydrates. In ion associated hydrates the bonding between the metal ion and water molecule can be strong, which results in very high dehydration temperature (Aaltonen, 2007).

Many pharmaceutical solids can exist in a not crystalline form - amorphous form. Amorphous solids consist of disordered arrangements of molecules and do not possess a distinguishable crystal lattice nor unit cell and consequently have zero crystallinity. In amorphous forms, the molecules display no long-range order, although the short-range intermolecular forces give rise to the short-range order typical of that between nearest neighbors. Thermodynamically, the absence of stabilizing lattice energy causes the molar internal energy or molar enthalpy of the amorphous form to exceed that of the crystalline state (Grant, 1989). The name "glassy state" is given to amorphous products which liquefy by undergoing a glass transition.

Polymorphs, solvates, amorphous are schematically presented in figure 3.3.

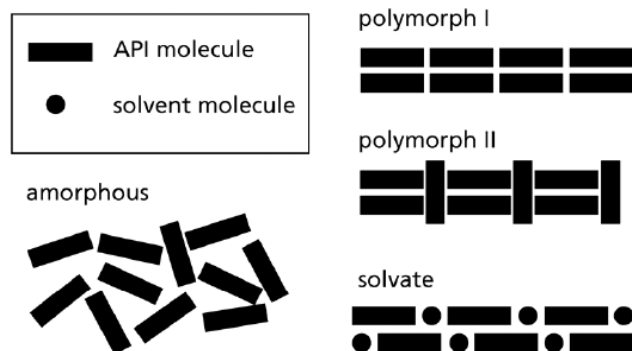


Figure 3.3 Schematic view of various types of solid forms (Hilfiker et al., 2006)

According to McCrone (McCrone, 1965), every compound has different polymorphic forms, and the number of forms known for a given compound is proportional to the time and money spent in research on that compound. Approximately one-third of organic compounds and about 80% of marketed pharmaceuticals exhibit polymorphism under experimentally accessible conditions. On account of the different arrangement and/or conformation of molecules, polymorphs and/or solvates of a pharmaceutical solid exhibit different chemical and physical properties such as melting point, chemical reactivity, apparent solubility, dissolution rate, optical and electrical properties, vapor pressure, and density (table 3.1).

Table 3.1 List of physical properties that differ among various polymorphic forms (Grant, 1989)

Packing properties	Molar volume/density; Refractive index; Conductivity; Hygroscopicity
Thermodynamic properties	Melt/sublimation temperature; Internal energy; Enthalpy; Heat capacity; Entropy; Free energy; Thermodynamic activity, Vapor pressure, Solubility
Spectroscopic properties	Electronic transitions, Vibrational transitions, Rotational transitions, Nuclear spin transitions
Kinetic properties	Dissolution rate; Solid state reaction rate; Stability
Surface properties	Surface free energy; Interfacial tensions; Habit (shape)
Mechanical properties	Hardness; Tensile strength; Compactibility/tableting; Handling, flowability, blending

These properties can have a direct impact on the processability of drug substances and the quality/performance of drug products, such as stability, dissolution, and bioavailability.

There are two different mechanisms in which different crystal lattices can be formed: *packing polymorphism* by which molecules that are conformationally relatively rigid can be packed into different three-dimensional structures and *conformational polymorphism* by which conformationally flexible molecule can fold into different shapes that pack into different dimensional structures (Lohani et al., 2006).

The relative stability of polymorphs depends on their free energy, the lower the free energy the more stable polymorph. Under a defined set of experimental conditions (with the exception of transition points) only one polymorph has the lowest free energy. This is the thermodynamically stable form and the other polymorphs are termed as metastable forms. A metastable form is one that is unstable thermodynamically but has a finite existence as a result of relatively slow rate of transformation (thermodynamic tendency to reduce its free energy by transforming into stable form).

In the pharmaceutical industry the most stable polymorphic form of a drug substance is often used because it has the lowest potential for conversion from one polymorphic form to another. However, the metastable form is sometimes desirable on account of its special properties, such as higher solubility and bioavailability, better behavior during grinding and compaction or lower hygroscopicity (Lohani et al., 2006).

Solid-state reactions include solid-state phase transformations, dehydration/desolvation processes, and chemical reactions. One polymorph may convert to another during manufacturing and storage, particularly when a metastable form is used. Since an amorphous form is thermodynamically less stable than any crystalline form, inadvertent crystallization from an amorphous drug substance may occur. As a consequence of the higher mobility and ability to interact with moisture, amorphous drug substances are also more likely to undergo solid-state reactions.

Amorphous states may appear in some proportion in each crystallization or drying process. Typically obtained during lyophilisation, spray-drying, granulation, grinding or

milling, the amorphous form is responsible for the higher reactivity of some batches (Giron, 1995).

Phase conversions of one polymorphic form to another one are possible when exposed to a range of manufacturing processes. Milling/micronization operations may result in polymorphic form conversion of a drug substance. In the case of wet granulation processes, where the usual solvents are aqueous, one may encounter a variety of interconversions between anhydrides and hydrates, or between different hydrates. Spray-drying processes have been shown to produce amorphous drug substances (Hilfiker et al., 2006).

3.2.1. Thermodynamics of polymorphs

The relationship between different phases of a substance is governed by Gibbs's phase rule (Britain, 1999, Giron, 1995):

$$P + F = C + 2 \quad \text{Equation 3.3}$$

where:

C is the number of components,

P is the number of phases that exist in equilibrium,

F is the number of degrees of freedom.

In the case of single substances exhibiting polymorphism, C equals unity. If one phase (polymorph) is present, $P = 1$, $F = 2$. If $F = 2$ means that both temperature and pressure may be varied without changing number of phases. If two phases (polymorphs) are in equilibrium ($P=2$), the variance $F=1$, means that at chosen pressure, the temperature of the system is fixed at the *transition temperature* (T_t). The conclusion of Gibb's phase rule is that only one phase (polymorph) can exist at a any given temperature and pressure, except the transition temperature, in which case at defined pressure, usually atmospheric one, two phases (polymorphs) exist in equilibrium.

The process of transformation of one polymorph into another is phase transition and according to the phase rule may occur at given pressure by changing the temperature. If the phase transition is reversible, two polymorphs are *enantiotropes* and energy transition on heating is endothermic. If the phase transition is not reversible, the polymorphs are *monotropes*, in which case only one form is stable whatever the temperature and the transformation of unstable form to the stable one is exothermic.

For kinetic reason, an unstable form may exist for time outside the region assigned by the phase diagram and the phase rule, and it is termed as *metastable* form (Britain, 1999, Giron, 2001, Giron, 1995).

Some of characteristic of enantiotropic and monotropic systems according to Burger rules are presented in the table 3.2.

Table 3.2 Thermodynamic rules for polymorphic transition according to Burger, form I is higher melting form (Burger et al., 1979)

Enantiotropy	Monotropy
I stable > transition	I always stable
II stable < transition	II not stable at any temperature
Transition reversible	Transition irreversible
Solubility I higher < transition	Solubility I always lower than II
Transition II to I endothermic	Transition II to I exothermic
$\Delta H_f^I < \Delta H_f^{II}$	$\Delta H_f^I > \Delta H_f^{II}$
IR peak I before II	IR peak I after II
Density I < density II	Density I > density II

Two types of graphs are used to describe the thermodynamic behavior of polymorphs. These are energy-temperature diagrams and pressure-temperature diagrams, and both of them will be explained below.

The ability of a system to perform work and to undergo a spontaneous change at constant pressure is measured by Gibbs free energy, see equation 3.4 and is applied in thermal analysis (Britain, 1999, Giron, 2001, Giron, 1995).

$$\Delta G = \Delta H - T\Delta S \quad \text{Equation 3.4}$$

where:

G is Gibbs free energy (J)

H is enthalpy (J),

T is temperature (K) and

S is entropy of system (JK^{-1}).

In general, the thermodynamic relationship between two polymorphic phases is represented by plotting the Gibbs free energy as a function of temperature for each form (figure 3.4). At a given temperature, if the two curves intersect below the melting point of each polymorph, a reversible transition occurs at T_t of the intersection. At the temperature below T_t polymorph A has the lower free energy and is therefore the thermodynamically stable form, while above T_t polymorph B is stable. In the case of monotropy, the higher melting form is the thermodynamically stable form (Giron, 2001).

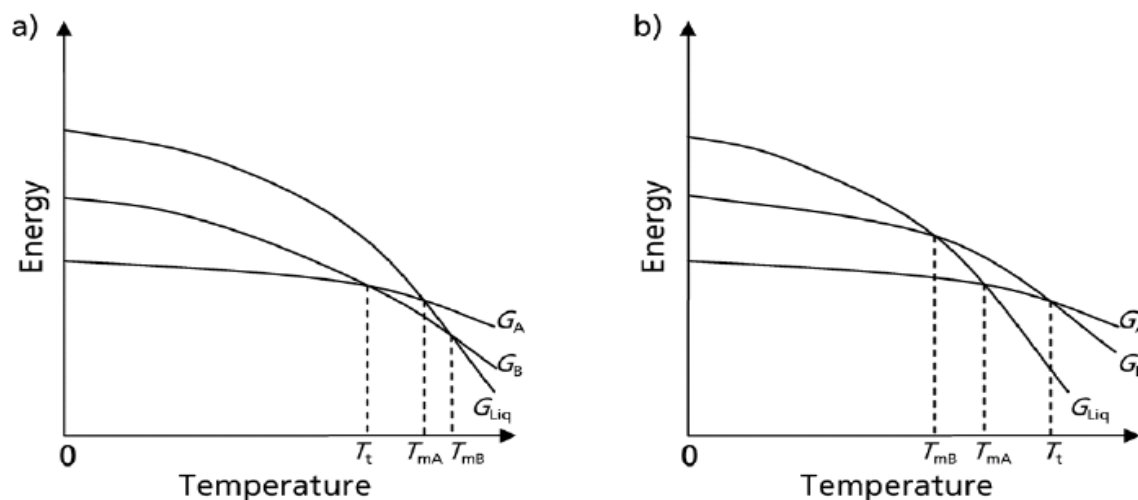


Figure 3.4 Relation between Gibbs energy G and temperature T for two modifications A and B in the cases of enantiotropy (a) and monotropy (b); Liq represents liquid phase; T_t is transition point between A and B and T_{mA} and T_{mB} are the melting points of A and B respectively (Giron, 2001).

Energy - temperature diagrams were introduced by Burger et al. (Burger et al., 1979) when they plotted free energy and the enthalpy as a function of temperature (figure 3.5 a and b).

A pair of polymorphs is said to be enantiotropic if exist the transition point T_t below the melting point of both polymorphs. In figure 3.5a the melting point of a polymorph can be defined as the temperature at which free energy isobar of polymorphs intersect the free energy isobar of the liquid. T_t is defined as the temperature where both polymorphs have equal free energy and they are in the equilibrium with each other.

In the case of the monotropy (figure 3.5b) one of the polymorphs is always stable below the melting point of both polymorphs. The free energy of polymorph A is always less than that of polymorph B at all temperatures below melting point of form A. Consequently polymorph B can undergo a spontaneous exothermic transformation into polymorph A at any temperature. Transition point T_t between two polymorphs in a monotropic system is virtual because it lies above the melting point of both polymorphs (Lohani et al., 2006).

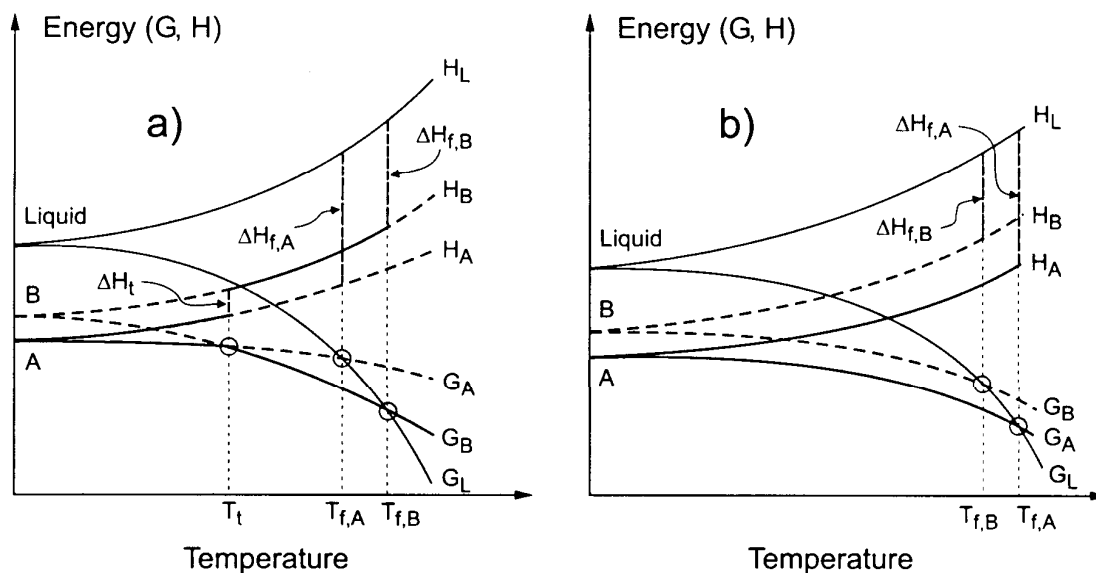


Figure 3.5 Energy – temperature plots for enantiotropic and monotropic system. G is Gibbs free energy, H is enthalpy, T is the temperature, subscripts A, B and L refer to form A, B and liquid phase respectively, while subscript f, t and m refer to fusion, transition point and melting point respectively (Lohani et al., 2006).

Second type of graphs commonly used to describe the thermodynamical behavior of polymorphs is pressure-temperature diagram. Phase diagrams of pressure versus

temperature illustrate the different equilibrium curves of the transitions solid-solid or solid-liquid or solid-gas. Diagrams in figure 3.6 are also presenting enantiotropic (a) and monotropic systems (b). Each form has a solid-liquid equilibrium curve and a solid-vapor equilibrium curve. In the case of enantiotropy, the liquid-vapor equilibrium curve (CD) meets the two solid-vapor curves after the point of intersection of the solid-solid equilibrium curve, and there is a solid A to solid B equilibrium curve (BF) and a reversible transition point A to B at a specific pressure. At the transition point, the free energy of the two forms is the same. AB is the equilibrium solid I - vapor, BC the equilibrium solid II-vapor, FB the equilibrium solid I-solid II, FC the equilibrium solid II-liquid and CD the equilibrium liquid-vapor (figure 3.6a). In the case of monotropy the liquid-vapor curve crosses the solid I-vapor curve before the points B and C. In figure 3.6b, the equilibrium curves are AE for solid I-vapor, FE for the solid-liquid equilibrium and ED for the liquid-vapor equilibrium. In both cases the dashed curves represent metastable curves (Giron, 1995).

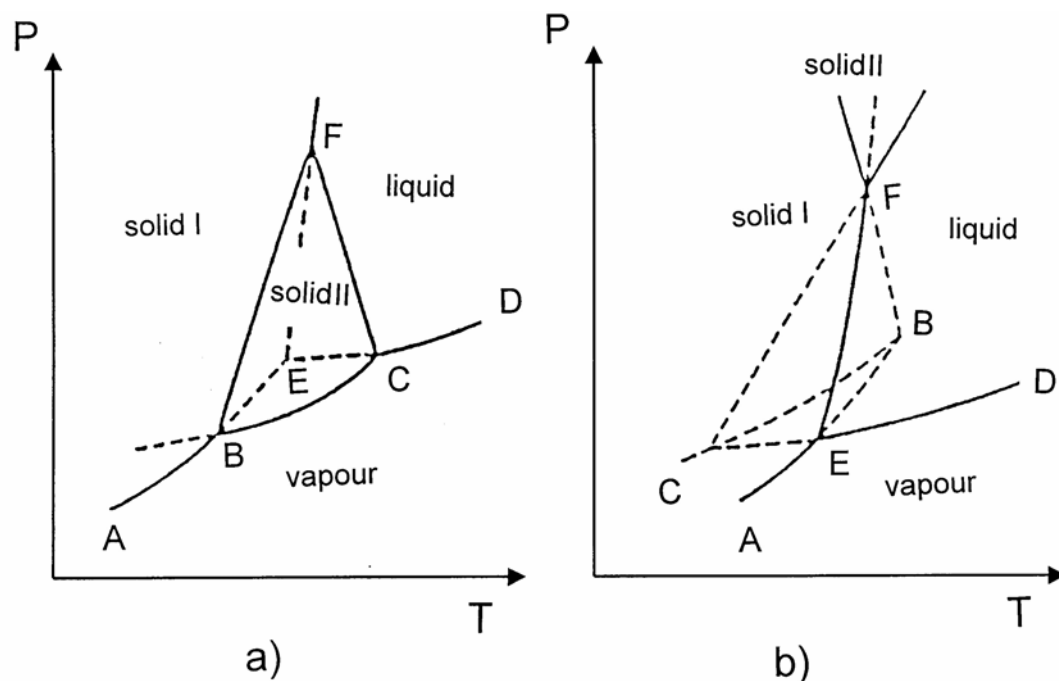


Figure 3.6 Pressure-temperature plots phase diagram for a single component with polymorphic behavior: a) enantiotropy and b) monotropy (Giron, 1995).

3.2.2. Phase mechanism and transformation

The solid-state properties of the API and the excipients must be understood in order to ensure consistent product performance. During product development it is necessary to identify the solid phases and recognize the transitions among them under relevant conditions. Knowledge of the mechanism of phase transitions becomes helpful in identifying the potential for such transitions and the factors affecting their kinetics which allows then rational formulation design and the selection of robust processes to ensure consistent product manufacturing and performance (Zhang et al., 2004).

There are four different underlying mechanisms for phase transformation:

- solid – state
- melt
- solution
- solution – mediated

Phase transitions which occur in the solid-state without passing through intervening transient liquid or vapor phases are defined to have solid state mechanism. In general, the kinetics of phase transition via a solid-state mechanism is influenced by the environment (T , P , RH, etc.), the presence of crystalline defects, particle size and distribution, and impurities (Van Campen et al., 1984).

By melting mechanism it is considered when a compound is heated above its melting point, and then subsequently cooled back to the ambient temperatures and the original solid phase may not be regenerated. In this case the phase transition may occur through heating/cooling cycle. Among the factors determining the final solid phase are the relative rates of nucleation, crystal growth, and cooling. Impurities or excipients are also likely to affect the course of crystallization (Zhang et al., 2004).

If the drug is dissolved or partially dissolved in a solvent during processing and if subsequent solvent removal induces a transformation, this transformation mechanism is considered as solution mechanism. The final solid may be a single phase or a mixture of amorphous and crystal forms depending on the rate of solvent removal, the ease of nucleation and crystal growth of the possible crystal forms under the processing conditions. It is important to note that the transition can be from a metastable phase to the stable phase or from the stable phase to one or more metastable phases (Zhang et al., 2004).

As opposed to the solution mechanism, the solution-mediated mechanism only allows the transition from a metastable phase to the stable phase. This type of transformation is driven by the difference in solubility between the two phases. In contrast to the solution mechanism where transformation occurs during drying, the solution-mediated mechanism operates when the metastable phase is in contact with the saturated solution. Three steps are involved in a solution-mediated transformation (Rodríguez-Hornedo et al., 1992): 1) initial dissolution of the metastable phase into the solution to reach and exceed the solubility of the stable phase; 2) nucleation of the stable phase; 3) crystal growth of the stable phase coupled with the continuous dissolution of the metastable phase.

If step 2 is rate-determining any factor that affects nucleation (solubility, solubility difference between the phases, temperature, contact surfaces, agitation, and soluble excipients/impurities) will influence the overall transformation. When step 3 is the rate-controlling step, the kinetics of the conversion is determined by solubility difference, solid/solvent ratio, agitation, process temperature, particle size of the original phase, and soluble excipients/impurities.

These four general phase mechanisms can lead to three classes of phase transitions: polymorphic, hydration/dehydration, and vitrification/amorphous crystallization (Zhang et al., 2004).

The term polymorphic transition refers to the interconversion among polymorphic forms. As it was already discussed above, the stability relationship between a pair of polymorphs can be categorized as monotropic or enantiotropic. Only one polymorph is stable throughout the temperature range for a monotropic system.

In the case of a monotropic system, a metastable polymorph can undergo a polymorphic transition to the stable polymorph during processing via all four mechanisms. In the solid-state these transitions are kinetically prevented due to molecular mobility. Stressing such systems either with heat or mechanical forces (drying, milling, or compaction) accelerates the transition to the stable polymorph. When the drug loading is low and the solubility in the processing solvent is high, transformation to a different solid phase via the solution mechanism is likely. On the other hand, the solution-mediated mechanism is more likely to occur if a high drug load

formulation is wet granulated and the solubility of the drug in the processing solvent is low. Polymorphic transitions from the stable to the metastable polymorph can only proceed via the melt or solution mechanisms (Zhang et al., 2004).

In the case of an enantiotropic system, if the temperature is raised above the transition temperature T_t , polymorphic transitions between the two phases can proceed via any of the four mechanisms. It has to be noted that for transitions that proceed via the solid-state mechanism, super-heating is much less likely than super-cooling near the T_t , because of the large temperature dependence of molecular mobility. Therefore, conversion to the low-temperature metastable form and thus the high-temperature stable form at temperatures above the T_t upon heating may not be reversed during cooling.

For both monotropic and enantiotropic systems, a sequence of phase transitions is often responsible for an overall polymorphic transition. For instance, a process may begin with hydration and then proceed through dehydration, or begin with vitrification and then proceed through crystallization (Zhang et al., 2004).

Hydration/dehydration is the type of transition which can be described as the conversion between crystalline anhydrates and hydrates, and between lower hydrates and higher hydrates. At constant temperature, one crystal form is stable over a range of water activities (or relative humidities, RH). At the critical water activities, the anhydrate/hydrate or lower hydrate/higher hydrate pairs can coexist. With increasing temperature, the critical water activity usually shifts to a lower value because of the endothermic nature of dehydration.

Hydration typically proceeds via solution or solution-mediated mechanisms. Sometimes for channel-type hydrates hydration may proceed via the solid-state mechanism. Dehydration can proceed via solid-state, solution, and occasionally via the melt mechanism. In the case when a nonaqueous solvent is used this process may occur by the solution-mediated mechanism. Mechanical treatments, such as milling, tend to accelerate the kinetics of dehydration by generating surface/defects and by local heating.

Vitrification and amorphous crystallization correspond to the interconversion between the amorphous phase and crystalline polymorphs or hydrates. The amorphous phase,

as being non stable one, is always disposed to crystallization at all temperatures, via solid-state, solution, or solution-mediated mechanisms.

Vitrification, which is a transition from a crystalline to an amorphous phase often proceeds via melt and solution mechanisms. In both mechanisms, the crystal nucleation or growth rates are slow compared with the rate of cooling or solvent evaporation. Vitrification may also proceed via the solid-state mechanism under mechanical stresses and upon dehydration (Zhang et al., 2004).

3.3. Characterization of Polymorphs

A number of methods have been employed for characterizing polymorphs in pharmaceutical solids. Of all methods available for the physical characterization of solid materials, it is generally agreed that crystallography, microscopy, thermal analysis, solubility studies, vibrational spectroscopy and nuclear magnetic resonance are the most useful.

3.3.1. X – ray diffraction

The x-ray crystallography technique whether performed using single crystals or powdered solids is concerned mainly with structural analysis and is therefore eminently suited for the characterization of polymorphs and solvates.

Diffraction is a scattering phenomenon. When x-rays are incident on the crystalline solids, they are scattered in all direction. In some of these directions, the scattered beams are completely in phase and reinforce one another to form the diffracted beams (Brittain, 1999). The Bragg law describes the conditions under which this occurs. It is assumed that perfectly parallel and monochromatic x-ray beam, of wavelength λ , is incident on a crystalline sample at an angle θ ($^{\circ}$). Diffraction will occur if:

$$n \cdot \lambda = 2 \cdot d \cdot \sin \cdot \theta \quad \text{Equation 3.5}$$

where:

d is distance between successive molecular planes in the crystal and

n is order of the diffraction pattern.

Most of drug substances are obtained as microcrystalline powders, from which is difficult to obtain crystals adequate for crystallography because the different crystal faces are oriented randomly in all possible direction of the powder. Furthermore it is usually sufficient to establish only the polymorphic identity of solid and verify that certain compound has desirable structure. For these reasons and for the simplicity of performance, powder x-ray diffraction is a predominant tool in the characterization of the polymorphs and solvates and it can also be used to quantify the amorphous content.

3.3.2. Microscopy (Light Microscopy and Scanning Electron Microscopy)

An extremely important tool for the characterization is that of microscopy, since observable habits of differing crystal structures must necessarily be different and therefore useful for characterization of such systems. Both, optical and electron microscopy may be used. Polarization microscopy is based on the way that examined crystal affects polarized light that is transmitted through the crystal in different angles. The method can be also used to differ between amorphous and crystalline material (Brittain, 1999). Optical microscopy is more limited in the range of magnification suitable for routine work because beyond 600X is difficult for observation of microcrystalline materials. On the other hand, electron microscopy can use high magnifications, up to 90000X and the images can contain a considerable degree of three-dimensional information. These two microscopic methods are complementary in that each one can provide the information which the other can not. Scanning electron microscopy uses electrons rather than light to form an image.

This technique is a powerful tool for characterization of pharmaceutical solids, but because it is descriptive and not quantitative it is often used in combination with other techniques. A conventional SEM can be thought of as an inverted light microscope, consisting of an electron gun for electron beam generation (illumination), a column with lenses for beam focusing, a sample chamber and a detector. The conventional type

exhibits a resolution of approximately 100Å and its large depth of field yields three-dimensional images. High vacuum is required for the electron source and sample chamber (Brittain, 1999).

Hot-stage microscopy (thermal microscopy or fusion microscopy) is extremely valuable tool for characterization of polymorphs and solvates because allows observation of the substance during the heating and cooling of just few milligrams of substance on a microscope slide. It is possible to conduct rapid analysis using small quantities of material and the entire phase diagram of drug material can be deduced upon the conduct of suitably designed experiments (Brittain, 1999, McCauley et al., 1995).

3.3.3. Thermal Analyses

Thermal analysis methods are differential scanning calorimetry (DSC) and thermogravimetric analysis (TGA), differential thermal analysis etc. These are techniques in which property of the examined material is determined as a function of an externally applied temperature. By using of a thermal analysis it is possible to evaluate physical and chemical changes that may take place in a heated sample. The nature of thermal reactions can be:

- endothermic (melting, boiling, sublimation, vaporization, desolvation, solid-solid phase transitions, chemical degradation etc) or
- exothermic (crystallization, oxidative decomposition etc).

Thermal analyses are widely used in pharmaceutical industry for the characterization of compound purity, salvation, degradation, and excipient compatibility. They also are employed to distinguish between enantiotropic and monotropic systems. For an enantiotropic system, the relative stability of a pair of solid forms inverts at some transition temperature beneath the melting point while a single form is always more stable beneath the melting point in a monotropic system (Brittain, 1999).

DSC measures the temperature and the flow associated with the transition in materials as a function of time and temperature. The sample and the reference materials are maintained at the same temperature and what is measured is the heat flow required to keep the equality in temperature. DSC plots are obtained as the differential rate of heating (in units of W/s, cal/s or J/s) against temperature. The area under the DSC peak

is directly proportional to the heat absorbed or evolved by the specific thermal event. There are two type of DSC instruments currently used, presented in figure 3.7:

- *power-compensation* DSC where the sample and reference material (pan) are kept at the same temperature by using individual heating elements, parameters recorded is the difference in power inputs to the two heaters and
- *heat-flux* DSC where the heat differential between the sample and reference material are monitored.(Brittain, 1999)

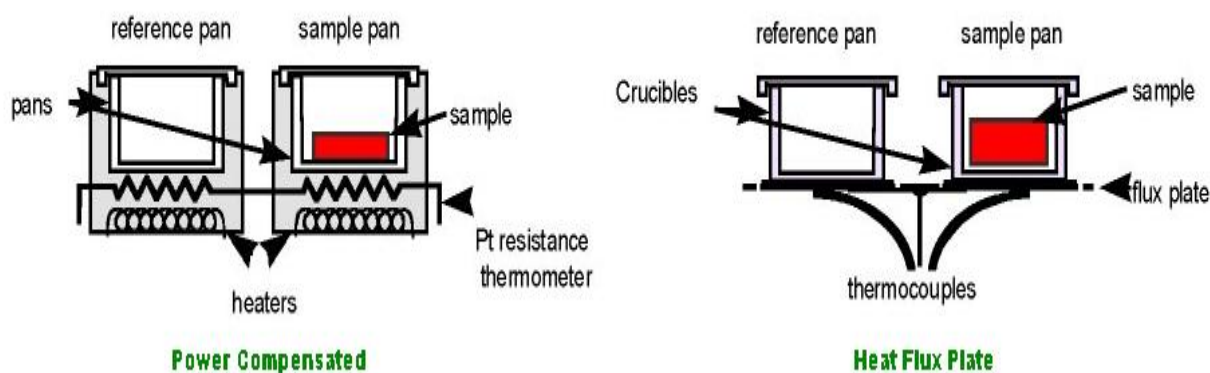


Figure 3.7 Schematic view of power compensated and heat flux plate DSC

The Pyris1 DSC operates on the principle of power compensation, with separate furnaces for the sample and reference cells. It measures change in heat flow as a function of temperature. As the temperature increases and the sample under investigation experiences a thermal event, that sample will either take energy from (e.g. melting) or release energy to (e.g. recrystallisation) the sample cell. When such an event occurs, energy is either supplied to, or taken from the reference cell in order to maintain a constant temperature difference between the two. The actual energy supplied or removed is calculated by the system and the data interpreted in terms of the type of transition that is taking place, endothermic or exothermic. The data are presented as a function of heat flow (mW), which can also be rewritten as energy per unit time (J/s). As the heating rate is increased, there is a greater input of energy per

unit time applied across the sample and reference cells, resulting in an increase in the overall sensitivity of the DSC instrumentation.

Thermogravimetry is a measure of the thermally induced weight loss of a material as a function of the applied temperature. It can be a useful method for quantitative determination of the total volatile content of solid thus it can be used as addition to e.g. Karl Fischer titrations for the determination of moisture. It also represents a powerful adjunct to DSC analysis because combination of these two methods is very useful in the assignment of thermal events. As such it permits the distinction between solvates and the anhydrous form of a given compound. Thermogravimetric analysis is most commonly used to study desolvation processes and compound decomposition because they are accompanied by weight changes. On the other hand, solid-liquid or solid-solid phase transformations are not accompanied by any weight loss of sample mass and would not be registered in TG thermogram (Brittain, 1999).

Thermogravimetry consists of the continual recording of the mass of the sample as it is heated in a furnace. The weighing device used is a microbalance, which permits accurate determination of milligram changes in the sample mass (McCauley et al., 1995).

3.3.4. Solubility

Solubility is defined as the equilibrium concentration of dissolved solid in the solvent medium and is ordinarily a function of temperature and pressure (Brittain, 1999). The solubility depends on the physical form of the solid, the nature of composition of the solvent medium, the temperature and the pressure (Grant et al., 1995). Therefore, e.g. temperature must be recorded for each solubility measurement in addition to the precise nature of the solvent and solid state at equilibrium. Solubility may be expressed in any appropriate units of concentration, such as quantity of solute dissolved divided by quantity of the solvent i.e. g/l mol/l etc.

The solubility of a solid in a liquid cannot be predicted in a wholly satisfactory manner as yet, except possibly for ideal solution, because of the complicating factor which must be taken in account (Martin, 1993).

The solubility of a solid in an ideal solution depends on temperature, melting point of the solid, and molar heat of fusion ΔH_f (heat absorbed when the solid melts). In an ideal solution, the heat of solution is equal to the heat of fusion, which is assumed to be a constant independent of the temperature. Ideal solubility is not affected by the nature of the solvent. The equation 3.6 derived from thermodynamics considerations for an ideal solution of solid in a liquid is:

$$-\log X_2^i = \frac{\Delta H_f}{2.303R} \left(\frac{T_0 - T}{TT_0} \right) \quad \text{Equation 3.6}$$

where:

X_2^i is the ideal solubility of the solute expressed in mole fraction (the superscript i refers to an ideal solution, and subscript 2 designates the mole fraction as that of solute)

T_0 is the melting point of the solid in absolute degrees, and

T is the absolute temperature of solution (Martin, 1993).

At the temperature above the melting point, the solute is in liquid state and in an ideal solution is miscible in all proportions with the solvent. Therefore, when $T > T_0$ the equation 3.6 is not applicable. The equation is also inadequate at temperatures below the melting point where ΔH_f can no longer be used (Martin, 1993).

Equation 3.6 can also be written as follows:

$$\log X_2^i = -\frac{\Delta H_f}{2.303R} \frac{1}{T} + \text{constant} \quad \text{Equation 3.7}$$

Therefore a plot of the logarithm of the solubility expressed in mole fraction, against the reciprocal of the absolute temperature results in a straight line with a slope of $\Delta H_f/2.303R$. By this means, the molar heat of fusion of various drugs may be obtained from their solubility in ideal solution (Martin, 1993).

The aqueous solubility of a drug is an important factor affecting its bioavailability. Solid drugs administered orally for systemic activity must dissolve in the gastro-intestinal fluids prior to their absorption. Thus, the rate of dissolution of drugs in gastrointestinal fluids could influence the rate and extent of their absorption.

USP expresses solubility in terms of milliliters of solvent required to dissolve 1g of solute. For substances whose solubilities are not definitely known, the values are described in pharmaceutical compendia by the use of certain general descriptive terms, table 3.3 (USP31, 2008).

Table 3.3 USP XXXI indicates solubility of different substances in descriptive terms (USP 31 et al., 2008)

Term	Parts of solvent required (ml) for one part of solute (g)
Very soluble	<1
Freely soluble	1-10
Soluble	10-30
Sparingly soluble	30-100
Slightly soluble	100-1'000
Very slightly soluble	1'000-10'000
Practically insoluble or insoluble	>10'000

Different lattice energies of polymorphs or solvates are reasons for the different solubility and subsequently for different dissolution rates and bioavailability of the same compound.

The metastable form should have higher solubility than the stable form, but theoretically a compound can only have one solubility. The real equilibrium solubility happens at infinite size of particles or at a secondary energy minimum. During the solubility test, certain amount of compound is stirred until equilibrium. At that point, a metastable compound has a reproducible number and this number is higher than the solubility of more stable polymorph.

But the molecules in solution are the same and saturated solution of metastable form is just a supersaturated solution of the compound itself. Waiting for a sufficient long time will result in precipitation of the more stable polymorph. Important thing is that solution made from different polymorphs contains the same compound (Carstensen, 2001).

The influence of crystal structure on the solubility of a solid can be explained using a model. For a solid to dissolve, the disruptive force of solvent molecules must overcome the attractive force holding the solid intact, which means that the solvation free energy released upon dissolution must exceed the lattice free energy of the solid for the process to proceed spontaneously. The equilibrium solubility of the solid will be determined by the relative balancing of the attractive and disruptive forces. The balance of these forces is determined by the enthalpy change and the increase in disorder of the system (entropy). Since different crystal structures are characterized by different lattice energies and enthalpies, solubility of different crystal polymorphs must differ as well. It should be emphasized that the solubility differences between polymorphs will be maintained only when a less stable form cannot convert to the most stable form. When such conversion takes place, the equilibrium solubility of all forms will approach a common value, namely that of the most stable form at room temperature (Grant et al., 1995).

The effect of polymorphism becomes critical on solubility since the rate of compound dissolution must be also dictated by the balance of the attractive forces existing at the crystal-solvent interface. A less stable polymorph having a higher lattice free energy will tend to dissolve faster, it will release higher amount of free energy which will increase the solubility and hence the driving force for dissolution. At the same time, each species would liberate the same amount of solvation energy because all dissolved species must be thermodynamically equivalent. The variation of dissolution rate due to different structures of the same drug can lead to the variation of bioavailability for different polymorphs or solvates (Brittain et al., 1999).

Determination of the solubility of solid materials can be obtained using *equilibrium method* where an excess amount of the compound is suspended in the chosen solvent.

During the test, temperature is fixed, samples has to be shaken (agitated), while the concentration of the solute in a saturated solution is determined at equilibrium by suitable analytical procedure. The application of *equilibrium method* to a metastable phase will result in determination of the solubility of the stable phase.

3.3.5. Spectroscopic methods

The utility of solid-state spectroscopy for characterization of polymorphic systems is becoming exceedingly important. Nuclear magnetic resonance (NMR), infrared absorption, and Raman spectroscopy are used to study crystal structures. These methods require that either the nuclei of the pair of substances being examined exist in magnetically inequivalent environments or the vibrational modes are sufficiently different between the structural forms to permit differentiation (Brittain, 1999).

Infrared absorption spectroscopy is type of vibrational spectroscopy where it is possible to observe the absorbance of compound in infrared region of the spectrum (400-4000 cm^{-1}). The characterization of polymorphs is done by using Fourier transformation technology (FTIR method) because it minimizes transmission and beams attenuation problems. Essentially all FTIR spectrometers use a Michelson interferometer. Radiation entering the interferometer is split into two beams by means of a beam splitter. One beam follows a path of fixed distance before being reflected back into the beam splitter, while the second beam travels a variable distance before being recombined with the first beam. The recombination of these two beams yields an interference pattern, and the time dependent constructive and destructive interferences have the effect of forming a cosine signal.

However, sometimes the solid state FTIR spectra of polymorphic systems are found to be only slightly different indicating that the pattern of molecular vibration is not so much affected by differences in crystal structure (Brittain, 1999).

It should be emphasized that the definitive criterion for the existence of polymorphism is via demonstration of a nonequivalent crystal structure, usually by comparison of the x-ray diffraction patterns. Microscopy, thermal analysis methodology, and solid state NMR

are generally considered as sources of supporting information (Brittain, 1989, Brittain, 2002).

3.4. Carbamazepine

Carbamazepine (5H-dibenzazepine-5-carboxamide; CBZ) (figure 3.8) is an iminostilbene derivative with a tricyclic structure. It was discovered in 1953 by chemist Walter Schindler at J.R. Geigy AG in Basel, Switzerland. Schindler synthesized the drug in 1960 and it was marketed in 1962 for treatment of trigeminal neuralgia. Later on it had been discovered that it can be used as an antiepileptic drug. Since 1986 it is available as a generic product. Nowadays CBZ is widely used for treatment of simple and complex partial seizures in epilepsy, trigeminal neuralgia, and bipolar affective disorder.

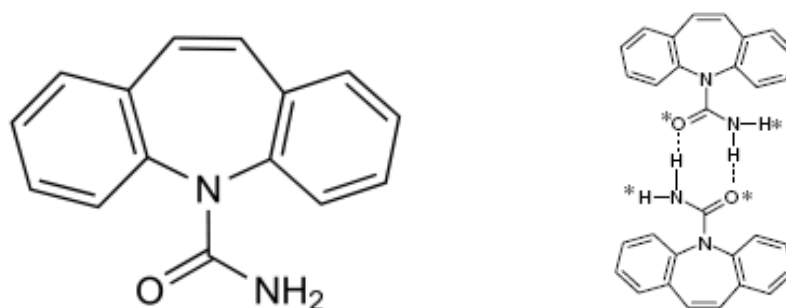


Figure 3.8 Structural formula of CBZ (a) and its dimer (b); *the possible hydrogen bonding sites

CBZ belongs to class II according to the Biopharmaceutical classification system, which means that it has high intestinal permeability and low water solubility. Its absorption is dissolution rate limited (Richter et al., 1978).

There are at least four anhydrous polymorphs of this molecule and dihydrate (structure) as well as other solvates (i.e. monoacetate) (Kobayashi et al., 2000, Krahn et al., 1989, Krahn et al., 1987, Rustichelli et al., 2000). The nomenclature of these polymorphs has varied between papers which later led to misunderstanding of the results. According to Grzesiak et al (Grzesiak et al., 2003) the following polymorphs of CBZ are existing:

- form I (triclinic) thermodynamically stable at temperature $> 130^{\circ}\text{C}$,
- form II (trigonal) metastable form at room temperature,
- form III (P-monoclinic) thermodynamically stable at room temperature;
- form IV (C-monoclinic) metastable form at room temperature.

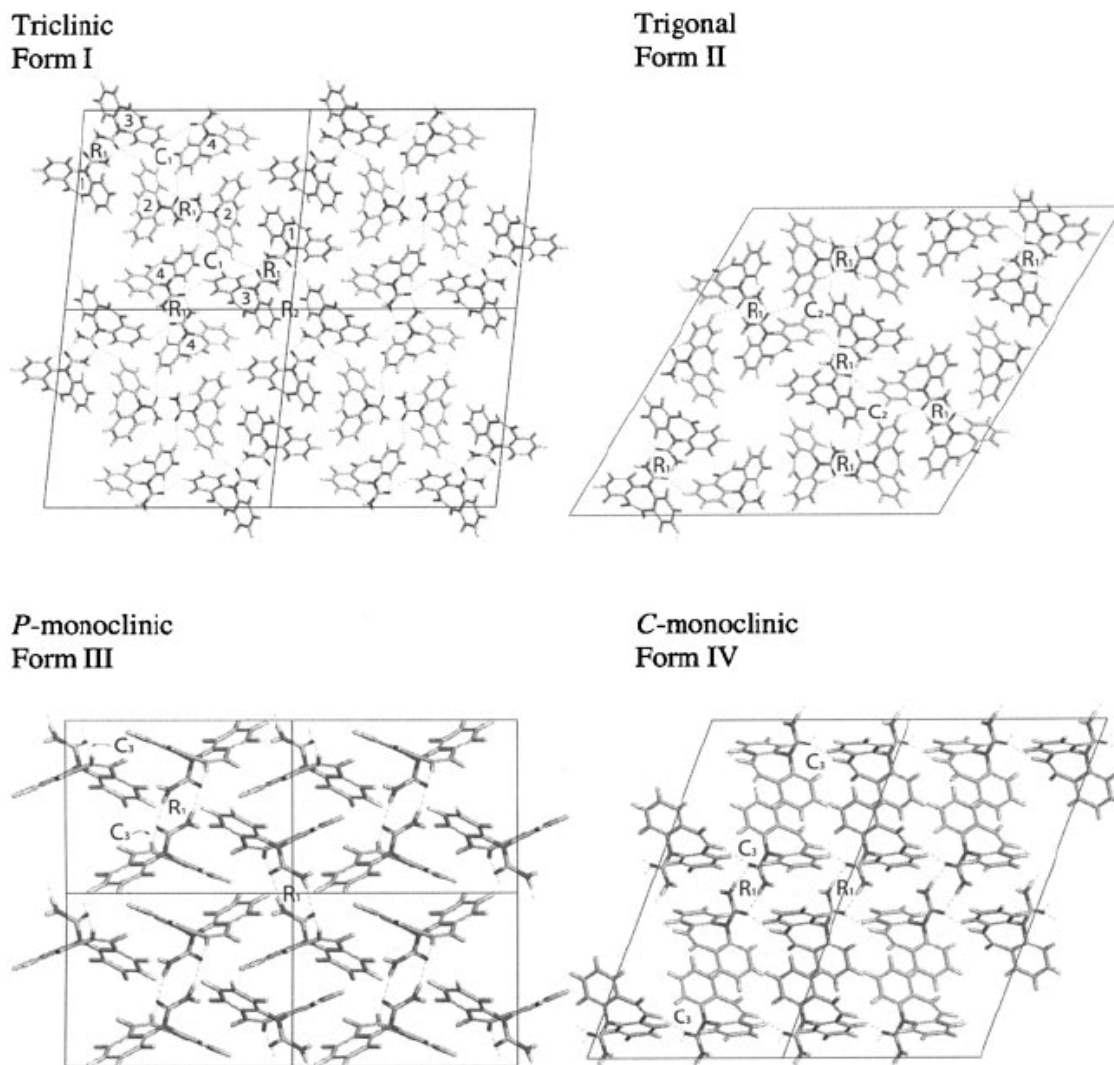


Figure 3.9 Packing diagrams of all four forms of CBZ showing hydrogen-bonding patterns (Grzesiak et al., 2003)

Dihydrate (figure 3.10) at first was defined as orthorhombic, but Harris et al (Harris et al., 2005) defined the crystal structure as monoclinic and therefore is classified as a channel hydrate.

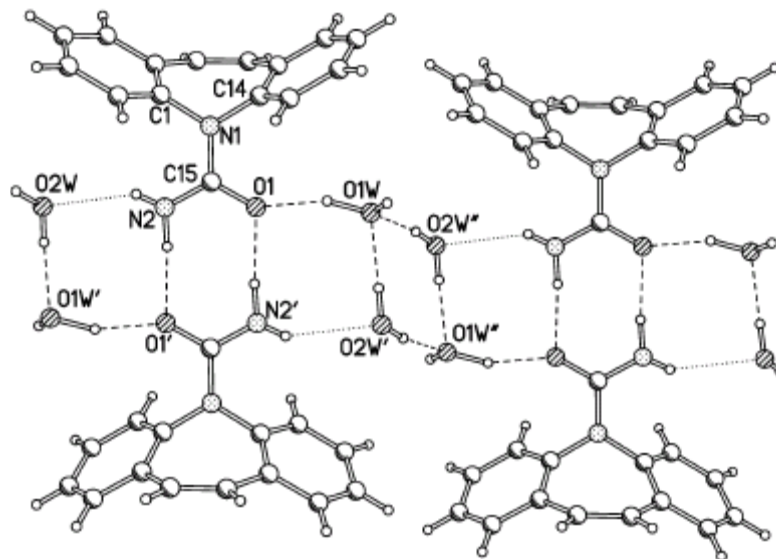


Figure 3.10 Structural formula of carbamazepine dihydrate, a detailed view of CBZ hydrogen-bonded network (Harris et al., 2005)

Among all mentioned polymorphs, form III, thermodynamically the most stable one at room temperature is the only commercially available form and it has been used in formulation of marketed products. The trigonal form is the least stable and therefore most soluble (Murphy et al., 2002)

Dihydrate is the most stable form in the aqueous solution and that is why all other polymorphs convert to the dihydrate form in aqueous solution via solution mediated mechanism though with different kinetics (Rodriguez-Hornedo et al., 2004) The two molecules of water bounded at amino and carboxyl group of CBZ, see figure 3.10, that is theoretically 13.2% of water. Crystals of dihydrate are stable at room temperature and relative humidity above 52% (McMahon et al., 1996).

According to Grzesiak (Grzesiak et al., 2003) DSC results stability of CBZ polymorphs is concluded as follows: form III>form I>form IV>form II, see table 3.4. This is the expected order according to the density rule which states: "If one of a molecular crystal has a lower density than the other, it may be assumed to be less stable at absolute zero".

	Triclinic (Form I)	Trigonal (Form II)	P-Monoclinic (Form III)	C-Monoclinic Form (IV)
Peak 1 (°C)	-	140-160	174.8	187.7
Peak 2 (°C)	193.5	192.1	193.2	191.5
ΔH (kcal/mol)	6.10	5.72	6.41	5.95
$\Delta(\Delta H)$ (kcal/mol)*	0.32	0.69	0	0.46
Density (g/cm ³)	1.31	1.24	1.34	1.27

Table 3.4 Transition temperatures, enthalpy of melting (ΔH) and relative stability of four polymorphs of CBZ and the room temperature density of each form (Grzesiak et al., 2003), * $\Delta(\Delta H) = \Delta H_{\text{form III}} - \Delta H_{\text{other form}}$

Forms I and III constitute an enantiotropic pair whose relative thermodynamic stability changes at 70°C. Below this temperature form III is the most stable form, while above this temperature form I is the more stable one. Form I is also forming an enantiotropic pair with form IV with temperature of transition at 125°C and a monotropic pair with form II (von Raumer, 2004). CBZ can also exist in amorphous state. The glass transition temperature for it was found to start at 56°C, followed by crystallization exotherm at ~85°C (Surana et al., 2003).

Transition conditions for carbamazepine polymorphs are presented in figure 3.11.

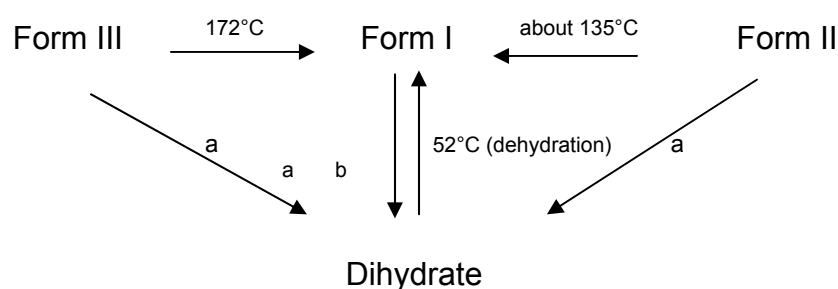


Figure 3.11 Transition conditions for CBZ polymorphs induced by heating and absorbing moisture, a represents 37°C 100%RH 2 weeks, and b represents <52% RH (Kaneniwa et al., 1984)

Because of the different crystal structures, polymorphs of CBZ have different chemical and physical properties, different density, different melting points, solubility, different dissolution rate and therefore different bioavailability.

Different commercial brands of CBZ tablets have a history of bioinequivalence and clinical failure, which may be due to polymorphism (Meyer et al., 1992, Meyer et al., 1998). Solubility, disc intrinsic dissolution and bioavailability of forms III, I and dihydrate were investigated by Kobayashi et al (Kobayashi et al., 2000). They found that form I was the most soluble between all forms, see table 3.5, with the highest disc intrinsic dissolution rate.

Table 3.5 IDR and solubility for forms I, III and dihydrate (Kobayashi et al., 2000)

	Form III	Form I	Dihydrate
IDR ($\mu\text{g}/\text{cm}^2/\text{min}$)	61.8	67.4	41.8
Solubility ($\mu\text{g}/\text{min}$)	460.2 ^a	501.9 ^a	311.1 ^b

^a estimated value, ^b determined value

The changes on dissolution rates of both anhydrous forms were described due to their transformation to dihydrate where transformation rate of form I was higher than transformation of form III. However, bioavailability results have shown that the area under curve (AUC) of examined form is in the order III > I > D. The differences in bioavailability between the forms III and I should be attributed to the more rapid transformation from form I to dihydrate (Kobayashi et al., 2000). The same order in bioavailability was confirmed by Carino et al (Carino et al., 2006).

During the dissolution in aqueous medium, anhydrous CBZ forms are undergoing a transformation to dihydrate CBZ. Kinetics of this transformation is a critical point for the bioavailability cause this phase transformation results in a reduction of dissolution and bioavailability and explains partly erratic dissolution of CBZ tablets stored at different temperatures and relative humidities (Wang et al., 1993). Transformation from anhydrous to dihydrate form may be the reason why some CBZ generic tablets have shown bioinequivalence and clinical failures (Meyer et al., 1992, Meyer et al., 1998).

Ono et al (Ono et al., 2002) determines the intrinsic dissolution rate of CBZ anhydrous forms and dihydrate. The slope of dissolution curve of dihydrate is constant during the test, while those of anhydrous forms vary gradually at the beginning and finally agree with the slope of dihydrate. The initial dissolution rates of anhydrous forms are identical however the kinetics of transformation of each anhydrous form to dihydrate is different thus the time required for changing the slopes differs from each other. This is the reason why the initial dissolution rate of anhydrous forms is faster and by the time when they convert to dihydrate it is becoming slower and finally at the end of the conversion it is in agreement with the dissolution rate of pure dihydrate form.

Kinetics of the CBZA to CBZD transformation in water was investigated by Murphy et al (Murphy et al., 2002) and it shows that transformation process is solution-mediated and the kinetics and the rate-controlling step for the transformation depends on the processing and storage conditions of CBZA. A solution mediated transformation involves three processes: dissolution of metastable form (CBZA); nucleation of stable form (CBZD) and crystal growth. Grinding of CBZA shortens the transformation time and changes the rate-limiting step from crystallization of CBZD form to dissolution of the CBZA. During the grinding step small amount of amorphous CBZ is formed and does not increase the concentration in solution above the solubility of CBZA, but it significantly increases the crystallization rate of CBZD.

According to Tian et al (Tian et al., 2006) raman spectroscopy can also be valuable tool for the investigation of the conversion kinetics of three CBZ polymorphs I, II and III to the dihydrate and that crystal morphology has greater effect than the polymorphic form on the conversion kinetics of CBZA to CBZD in aqueous solution.

The influence of excipients to the transformation of CBZ to CBZ dihydrate was investigated by many authors. Hydroxypropyl methylcellulose HPMC induces amorphism of anhydrous CBZ and inhibits its transformation to the dihydrate form, which can affect CBZA solubility since amorphous crystals dissolve faster than highly crystalline ones (Katzhendler et al., 1998).

Nair et al. demonstrated that solid dispersion of CBZ with polyvinyl pyrrolidone (povidon, Kollidon 30) and polyethylene glycol 4000 (PEG) increase the dissolution of CBZ by different mechanisms. In the povidon dispersion CBZ exists in amorphous form which

allows the higher release of CBZ from the dispersion and in the second case this effect is achieved due to the presence of CBZ as very small crystallites dispersed within the matrix of PEG (Nair et al., 2002).

Influence of the surfactant on CBZ conversion is interesting from the dissolution aspect because sodium lauryl sulfate is used in the USP dissolution medium for the CBZ tablets.

The surfactants, sodium lauryl sulfate (SLS) and sodium taurocholate (STC) can increase the solution-mediated transformation of CBZ. Their effect depends on the type and concentration of surfactants. SLS promotes the surface – mediated nucleation of CBZD on CBZA crystals at the concentration below critical micellar concentration (CMC) and has a little effect on CBZ morphology. Above the CMC, both surfactants SLS and STC promote the transformation by increasing the bulk nucleation of CBZD. STC depending on concentration changes the crystal morphology of CBZD from acicular to prismatic (Rodriguez-Hornedo et al., 2004)

Tian et al (Tian et al., 2006) found that all of the following excipients, hydroxypropyl cellulose (HPC), polyvinyl pyrrolidone (PVP) and carboxymethyl cellulose may retard the conversion of CBZA to CBZD to a certain extent. HPC and PVP show the highest inhibitory effect by the complete inhibition of conversion for 18 hours. In that case crystals of CBZA are dissolving without formation of CBZD nuclei. Carboxymethyl cellulose increases the crystal roughness implying the CBZ dissolution in carboxymethyl cellulose solution without conversion to dihydrate.

Influence of one excipient on the phase transformations of a substance is not always the same and it may depend on the substance itself. Physical stability of hydrates and anhydrates of theophylline and carbamazepine in presence of excipients is investigated by Salameh et al (Salameh et al., 2006). They found out that in general examined excipients (PVP, microcrystalline cellulose and mannitol) can promote dehydration process. For the hydration process (conversion from anhydrous to dihydrate phase) excipient can enhance, retard or have little effect on hydration kinetics and different effect was observed between theophylline and carbamazepine.

Recently Tian et al. (Tian et al., 2007) studied the dissolution of CBZA and CBZD in water and 0,1% w/v solutions of polyethylenglycol (PEG) and HPMC. Anhydrate shows the highest dissolution rate when water is used as dissolution medium. In this case the

increased surface area which is formed by crystallization of CBZD needle-like crystals improves the dissolution rate. As some of the excipients, especially HPMC, can completely stop the transformation to CBZD, the dissolution rate in that case is not enhanced. The enhancement of dissolution is not observed in the dissolution of CBZD compacts and the initial dissolution rate is much lower than for CBZA. For the dissolution of CBZD in excipient solutions, HPMC and PEG increase the wettability of CBZD and improve the dissolution of compound.

Since carbamazepine is prone to phase transformation from one form to another and because the transformation may occur during the preparation of raw material and solid dosage forms it is important to take care of all possible condition which can induce them.

For technological purposes it is important to know that during aqueous granulation of form III partial formation of the dihydrate will occur. As the following process is the drying process, the formed dihydrate may be dehydrated again, but leading to formation of form I. Granules may result with a core of form III and a surface covered by form I, where this part slowly will convert back to form III (Krahn et al., 1989).

Dehydration of CBZ dihydrate results in formation of different forms. The anhydrous form obtained by heating dihydrate was form I. If the dehydration under reduced pressure was used the form was obtained III, while dehydration under nitrogen flow or under low water vapor pressure results in amorphous anhydrate (McMahon et al., 1996). According to Suryanarayanan (Han et al., 1998) dehydration under low water vapor pressure results in an amorphous anhydrate whereas high vapor pressure results in crystalline form I.

CBZ is considered as a drug with a narrow therapeutic index. The therapeutic index or ratio according to definition is ratio between the median lethal dose (LD₅₀) and median effective dose (ED₅₀). According to FDA pharmacologic agents with a therapeutic index < 2 are considered to exhibit a narrow difference between therapeutic and toxic plasma concentrations and therefore are classified as narrow therapeutic index drugs.

3.5. Dissolution

3.5.1. Dissolution process

Dissolution is widely used in vitro test for determination of release rate of drug from a dosage form. It is used for characterization of drugs, quality control of dosage form, to guide development of new formulations and to correlate results with in vivo activity. Dissolution tests are used to confirm compliance with compendial specifications (Ford et al., 2002). Dissolution rate may be defined as the amount of active ingredient in a dosage form dissolved in unit time under standardized conditions of liquid-solid interface, temperature and media composition.

The mathematical expression for this definition is according to Noyes-Whitney (Noyes et al., 1897) given in equation 3.8:

$$dW / dt = kS \cdot (C_{sat} - C_{sol}) \quad \text{Equation 3.8}$$

where:

dW / dt is the dissolution rate ($\text{mgml}^{-1}\text{min}^{-1}$)

k is a dissolution constant

S is the surface area of the solid (cm^2)

C_{sat} is the concentration of a saturated solution (mg/ml)

C_{sol} is the concentration at any given time (mg/ml)

The basic step in drug dissolution is the reaction of the solid with dissolution medium. The dissolution media will pass the solid with a certain velocity. In the diffusion layer concept or film theory it is assumed that the solid is surrounded by a stagnant liquid layer with a certain thickness h . At the surface of solid ($x=0$), the concentration of dissolved solid is equal to its saturation concentration, C_s . Beyond the static diffusion layers, at x greater than h , mixing occurs in the dissolution media so the drug is found to be in a uniform concentration C , figure 3.12. The thickness h of unstable stagnant layer can be influenced by the stirring rate in the dissolution apparatus and it is also influenced in the case of the intrinsic dissolution test.

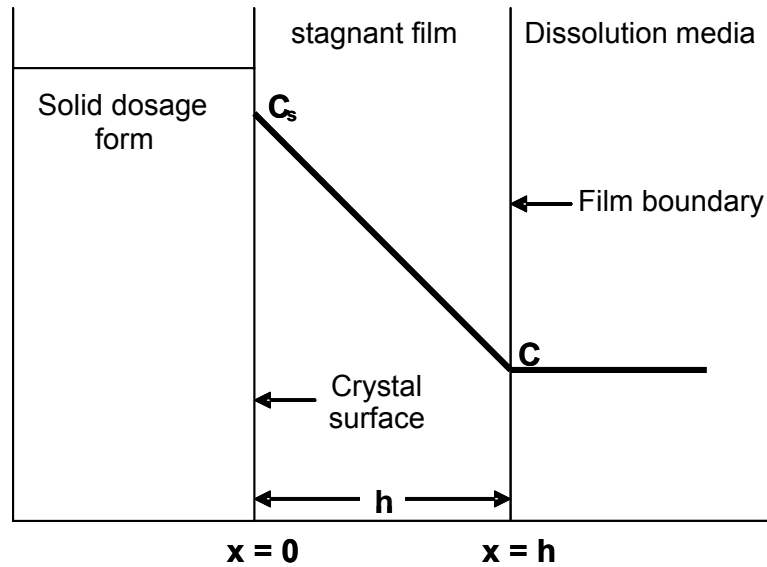


Figure 3.12 Basic principles of the dissolution of drug from solid dosage form

At the solid surface-diffusion layer interface, the drug in the solid is in equilibrium with the drug in the diffusion layer. The gradient, or change in concentration with distance across the diffusion layer, is constant, as shown by the straight downward-sloping line. Using diffusion layer concept, the Nernst (Nernst, 1904) modification to the Noyes-Whitney equation can generally applied to the dissolution of solids:

$$\frac{dC}{dt} = \frac{DS}{Vh}(C_s - C) \quad \text{Equation 3.9}$$

where:

C is the concentration of the solute in time t ($\text{mgml}^{-1}\text{min}^{-1}$),

D is the diffusion coefficient,

S is the surface area (cm^2),

V is the volume of dissolution media (ml)

h is the thickness of the diffusion layer (mm)

C_s is the saturated concentration (mg/ml)

There are a number of experimental factors which can have a direct impact on the dissolution process. The optimum dissolution testing conditions differ with each drug formulation. Different agitation rates, different medium (including different pH), and different dissolution apparatus should be tried to distinguish which dissolution method is optimum for the drug product and discriminating for drug formulation changes. The appropriate dissolution test condition for the drug product is then used to determine acceptable dissolution specifications.

The size and shape of the dissolution vessel may affect the rate and extent of dissolution. For example, the vessel may range in size from several milliliters to several liters. The amount of agitation and the nature of the stirrer affect the dissolution rate. Stirring rates must be controlled, and specifications differ between drug products.

The temperature of the dissolution medium must be controlled and variations in temperature must be avoided. Most dissolution tests are performed at $37 \pm 1^\circ\text{C}$.

The nature of the dissolution medium, the solubility of the drug and the amount of drug in the dosage form will affect the dissolution test. The dissolution medium should not be saturated by the drug. Usually, a volume of medium larger than the amount of solvent needed to completely dissolve the drug is used in such tests. The usual volume of the medium is 500–1000 ml. Drugs that are not very water soluble may require use of a very large capacity vessel (up to 2000 ml) to observe significant dissolution (Ford et al., 2002).

Sink conditions is a term referring to an excess volume of medium that allows the solid drug to continuously dissolve. If the drug solution becomes saturated, no further net drug dissolution will take place. Therefore, sink conditions are one of the main parameters which have to be controlled during the dissolution test, especially for low water soluble drugs. By keeping the volume of solvent large with the respect to saturation point (at least three to ten times larger), sink condition are granted ($C_{sat} \gg C_{sol}$) (Hanson et al., 2004).

3.5.2. Dissolution methodology

The general principle of dissolution test is that the powder or solid dosage form is tested under uniform agitation which is accomplished by either using a stirrer inside the apparatus or rotating the container holding the dosage form. There are four general methods which are currently included in USP XXXI (USP31, 2008):

- basket apparatus (apparatus I)
- paddle apparatus (apparatus II)
- reciprocating cylinder apparatus (apparatus III)
- flow-trough apparatus (apparatus IV)

Here only the first two, both limited volume-type apparatus will be shortly explained. An official description of all dissolution apparatus can be found in above mentioned pharmacopeias with the exact specifications.

3.5.2.1. Rotating basket method

The basket method was first described by Pernarowski as a container with basket, containing the examined dosage form, allowed for fluid change. In 1970 it has been modified in rotating basket apparatus and considered as a first official method in USP (Ford et al., 2002) figure 3.12.

The basket method represents an attempt to constrain the position of the dosage form in order to provide the maximum probability of a constant solid-liquid interface. The agitation of the liquid is caused just by the movement of the basket itself. But when, a rapid drug release occurs, the drug may not be continuously distributed in dissolution media as fast as it should be.

3.5.2.2. Paddle method

This method known as apparatus II was original developed by Poole 1969 where a paddle of specific dimensions replaces the basket as a source of agitation. Paddle method (figure 3.13) overcomes some disadvantages of the rotating basket method, but it requires careful precision in the geometry of the paddle and flask because any minor change in paddle orientation may cause variations in dissolution.

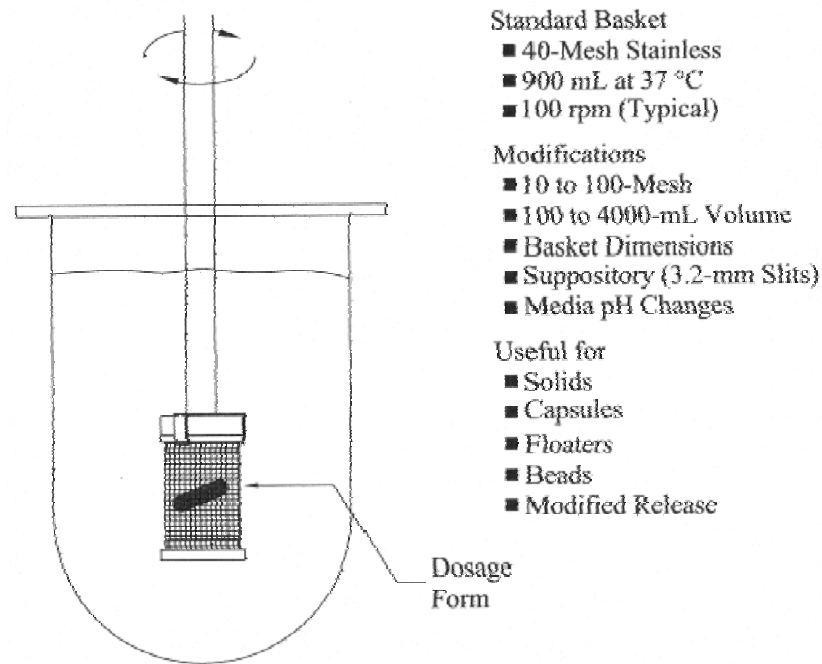


Figure 3.12 Basket method

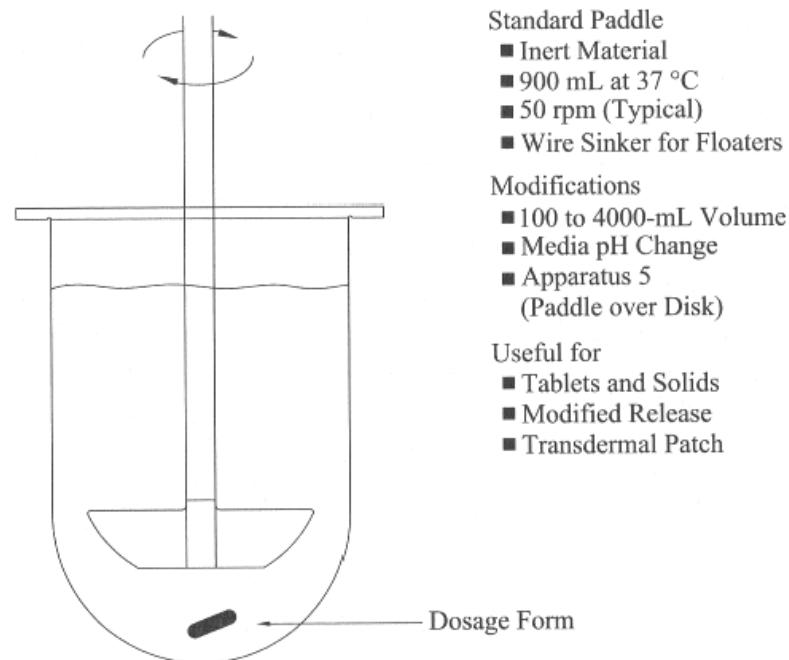


Figure 3.13 Paddle method

During the dissolution tests solution-mediated transformation are important because the rate of transformation determines the concentration of drug in solution, with faster conversion rates leading to lower levels of drug dissolved.

Solution mediated transformation involves three main steps: dissolution of metastable solid phase, nucleation and growth of stable solid phase (Ford et al., 2002)

It is known that anhydrous CBZ converts to dihydrate in aqueous solution mediated mechanism. The reason for a solution-mediated transformation to the dihydrate crystal form is that solubility in water of anhydrous CBZ form is at least three times higher at the room temperature than of CBZ D (Murphy et al., 2002)

Because of CBZ poor solubility, USP dissolution method for CBZ tablets requires use of surfactant, 1% sodium lauryl sulfate (Rodriguez-Hornedo et al., 2004).

3.5.3. Intrinsic dissolution

Intrinsic dissolution, or measurement of the rates of solution, is a very powerful method for the evaluation of solubility differences between polymorphs or solvates. It is a method which gives valuable information about physicochemical behavior of a pure drug substance in dissolution medium by removing many of the variables you would find in normal dissolution (effect of change of surface area, effect of excipients, etc).

There are two types of intrinsic dissolution methods. One is to simply pour powder into the dissolution medium and to monitor the concentration of dissolved solute as a function of the time. Data obtained by this method should be corrected by the factors relating to surface area or particle size distribution. In the second approach, the powder is compacted in a tableting die. Only one face of the disc is exposed to the dissolution medium and rotated at the constant speed e.g. of 100rpm (Yu et al., 2004).

The advantage of the constant surface area method is that its dissolution profiles are linear with time and more easily comparable. Additional information about relative surface areas or particle size distributions of two materials is not required, since these differences were eliminated when the analyzed disc was prepared (Grant et al., 1995).

Under constant hydrodynamic conditions, the intrinsic dissolution rate is usually proportional to the solubility of the dissolving solid. Consequently, in a polymorphic system, the most stable form will ordinarily exhibit the slowest dissolution rate.

Intrinsic dissolution rate investigation becomes more complicated when one or more of the studied polymorphs interconvert to another during the measurement (Brittain et al., 1999).

If sink conditions are given, the concentration of the drug C (mg/ml) at the time t (min) can be expressed by equation 3.10 (Nogami et al., 1966):

$$C = \frac{S}{V} k C_s t \quad \text{Equation 3.10}$$

where:

S is the surface area of the tablet (cm^2),

V is volume of test solution (ml),

k is intrinsic dissolution rate constant

C_s represents solubility (mg/ml).

Subsequently the intrinsic dissolution rate (IDR) or dissolution rate from unit surface area than can be calculated by the following equation 3.11 (Kobayashi et al., 2000, Sethia et al., 2004):

$$IDR = \frac{C}{t} \cdot \frac{V}{S} = k \cdot C_s \quad \text{Equation 3.11}$$

Intrinsic dissolution rate is expressed in terms of $\text{mg}/\text{cm}^2/\text{min}$. IDR above $1.0\text{mg}/\text{cm}^2/\text{min}$ suggest negligible problems with dissolution rate limiting absorption, but rates below $0.1\text{mg}/\text{cm}^2/\text{min}$ indicate likelihood with dissolution rate limited absorption (Hanson et al., 2004).

3.6. Preparation of tablets

A powder can physically be described as a special type of disperse system consisting of discrete, solid particles which are surrounded by or dispersed in air. However, the particles are normally in contact with each other. The interparticulate attractions at the

point of contact are relatively weak and the powder is thus characterized by exhibiting a low mechanical strength. The transformation of powder into a compact is the result of a reduction in the porosity of the powder system, and thus particle surface will be brought into close proximity to each other. As a consequence, the number and strength of interparticulate attractions will increase with a subsequent increased coherency of the powder system. The result of the compaction procedure is a solid specimen of a certain porosity, normally in the range of 5 to 35% for pharmaceutical compact (Alderborn, 1996).

Compressibility may be defined as the ability of the material to undergo a reduction in volume as a result of applied pressure. Compressibility indicates the ease with which powder bed undergoes volume reduction under pressure and is represented by a plot showing the reduction of tablet porosity with increasing of pressure. The lower the porosity at a given compaction pressure, the better the compressibility and the greater the interparticulate bonding.

Compactibility is the ability of a material to produce tablets with sufficient strength under the effect of densification. The tensile strength of a tablet decrease exponentially with increasing porosity. Compactibility shows the tensile strength of tablets normalized by tablet porosity (Leuenberger, 1982).

Tablets are the most commonly used dosage form for pharmaceutical preparations. They are prepared by applying a pressure to a powder bed, which compacts the powder into a coherent compact (powder compaction), the tablet. When external mechanical forces are applied to a powder mass several following processes may occur:

- particle rearrangement
- elastic deformation of particles
- plastic deformation of particles
- fragmentation of particles
- formation of interparticulate bonds

During the compression process particles are initially rearranged and they are forming closer packing structure. As the load increases, rearrangement becomes more difficult and packing characteristics of the particles or a high interparticulate friction between

particles will prevent any further interparticulate movement. The further compaction involves some types of particle deformations. If on removal of the applied load, deformation is spontaneously reversible than this type of deformation is *elastic*. This is true for any material. On the other hand, *plastic or brittle fracture* deformation is irreversible and in that case an elastic limit (yield point) is reached and loads above it result in not reversible deformation on removal of applied force.

Plastic deformation mechanism dominates in materials in which shear strength is less than the tensile or breaking strength. When the shear strength is greater, particles may be fractured (*fragmentation*) into smaller fragments, which will decrease the compact volume by rearrangement. If the applied pressure is increased the smaller particles can again be deformed. A single particle may pass through some of these processes several times during the compaction cycle. This is brittle fracture and most likely occurs with hard, brittle particles.

When the particle surface area brought together into close vicinity they may form interparticulate attraction or bonds. Some deformation processes like plastic deformation are time dependent and occur at various rates during the compaction sequence. This means that if a plastically deforming solid is loaded too rapidly for this process to take place, the solid may exhibit brittle fracture. Contrary, if the dwell time under the compressive load is prolonged, than plastic deformation may continue leading to more consolidation (Marshall, 1986).

Information on the compression and compaction properties of the pure drug is extremely useful. The tabletted material should be plastic and capable of permanent deformation, but it should also exhibit a degree of brittleness (fragmentation).

Pharmaceutical materials normally consolidate by more than one of these mechanisms, depending on the applied pressure range and therefore it is a need to have adequate characterization techniques.

The factors accounting for the strength of the tablets can be classified as primary and secondary. The primary factors are bonding mechanism and the surface area over which they act. Secondary factors include particle shape, surface texture and particle size distribution.

The general bonding mechanisms responsible for compaction are classified according to Rumpf (Rumpf, 1958) in five types:

- bonding due to movable liquids (surface tension and capillary pressure)
- non-freely-movable binder bridges (adhesion and cohesion forces)
- solid bridges
- attractions between solid particles (intermolecular forces)
- shape-related bonding (mechanical interlocking)

The dominating bond types adhering particles together in compaction of dry powder can be limited to three types: intermolecular bonding, mechanical interlocking and solid bridges.

Intermolecular forces are all the forces that act between surfaces separated by some distance (Van der Waals forces, electrostatic forces and hydrogen bonding) (Nystrom et al., 1995) and they are considered to be the most important for the mechanical strength in the tablet. Mechanical interlocking is dependent on the shape and the surface of the particles and their deformation during the compaction process. The material/solid bridge appears just in special cases like partial melting or dissolution in adsorbed water.

Particles dimensions and their shape before compaction are other very important factors for the tablet strength. It is generally assumed that a change in particle size not only affects the external surface area of particles but also their. Furthermore, it is suggested that reducing of original particle size will increase the compact strength. However, deviations from this pattern are commonly reported for the highly fragmenting materials, in which case the tablet strength is independent of particle size.

The shape of crystals is a complex characteristic but that it is difficult to assess its importance in relationship to powder properties. Concerning the influence of the shape of the particles before compaction on the compact strength, it seems that only in case when material fragments to a limited degree during the compaction phase a change toward more irregular particles increases the compact strength (Alderborn, 1996)

3.6.1. Compaction simulator

Compaction simulators are sophisticated tools that enable the reproduction of different compaction parameters of any industrial machine (as compaction speed, compaction force, etc.). Published works encourage to use compaction simulators as research tools for robust formulations (Marshall, 1986, Muller et al., 1994)

The Presster™ is a single station, linear compaction simulator, which can simulate any rotary tablet press by mimicking the mechanics of these machines (Picker, 2003). Built around a linear carriage that moves a set of punches and a die between two compression rolls, it can mimic press geometry by matching the compression wheels. It can also match press speed using a variable speed motor drive; match tablet weight and thickness by adjusting depth of fill and the distance between the rolls; and match tooling by installing standard or any special tooling (Levin, 2002).

Presster™ is instrumented with:

- Linear Variable Differential Transformers (LVDT) for upper and lower punch displacement measurement.
- Strain gauges for force measurement during compaction and precompression.
- Strain gauges for die wall expansion measurement with instrumented die.
- Strain gauges for ejection force.
- Strain gauges for tablet take-off force.

The following set up can be installed before compaction:

- Selection of an industrial machine model in a list
- Filling position of the lower punch before compression
- Minimal gap between the punches during precompression and compaction by variation of the rolls positions
- compaction speed
- Ejection angle

4. Aims of the study

The polymorphs and hydrate of carbamazepine have been shown to exhibit different dissolution rates, bioavailability and different commercial brands of carbamazepine tablets have a history of bioinequivalence and clinical failure, which may be assigned polymorphism.

It is well known that raw materials obtained from different producers, although containing, as declared, the same polymorphic form, can show different properties during the dissolution caused by possible variation in the synthesis or influenced by presence of impurities or mixture of polymorphic forms.

Carbamazepine - the selected model drug which has a problem with the uniformity of dissolution of final product is one example that illustrates the necessity to identify and characterize polymorphic modifications as precise as possible.

We hypothesize that the variation in dissolution may be avoided by establishing an adequate strategy to maintain product quality by defining and monitoring the variability of critical parameters of the bulk drug and by using specific excipients in the formulation which will control the CBZ anhydrate to dihydrate conversion and thereby stabilize the variation in dissolution behavior of the final CBZ product.

Thus, the aims of the study include the following issues:

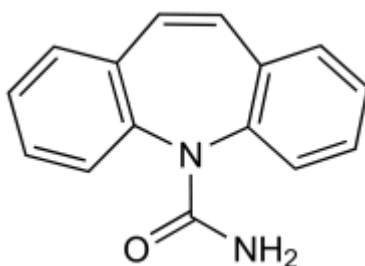
- Investigation of the variability of commercially available CBZ on the intrinsic dissolution behavior in order to recommend a strategy to maintain product quality by monitoring the variability of critical parameters of the bulk drug
- To suggest a method to delete the prehistory of the active material
- Investigation of the influence of selected excipients on the IDR of CBZ

5. Materials and methods

5.1. Materials

Carbamazepine

Structural formula:



Empirical formula: C₁₅H₁₂N₂O

Molecular weight: 263.27g/mol

Appearance: white or almost white crystalline powder

Melting point: 189 - 193°C

Dissociation constant (pKa): 7.0

Partition coefficient log P (octanol/water): 2.45

The following samples of carbamazepine were used for the investigation:

- CBZ USP standard purchased from Sigma Aldrich, Lot 093K1544.
- Carbamazepine anhydrous: the samples were provided from three different Bosnalijek's suppliers and for the reasons of confidentiality will be signed as CBZ A, CBZ B and CBZ P. Each of the producers donated three batches of carbamazepine (A1, A2, A3, B1, B2, B3, P1, P2 and P3) and thus batch to batch variability was investigated as well. There was no special specification for the drug substance from our side e.g. for particle size distribution, therefore all delivered samples were of commercial grade.
- Carbamazepine dihydrates (CBZ D) prepared by crystallization from all 10 available CBZ anhydrous samples (see 5.2.2.1. for method of preparation)

Following excipients were used:

- Lactose monohydrate Fast Flo[®] (Foremost Pharma, USA). This is spray dried lactose monohydrate with certain percentage (up to 5%) of amorphous lactose.

Fast Flo[®] lactose has improved flow and compression properties in comparison with lactose α -monohydrate and it is mainly used in direct compression.

- Ludipress[®], purchased from BASF, Germany. Ludipress[®] contains 93 \pm 2% of spray dried lactose α -monohydrate, 3.5 \pm 0.5% of Kollidon[®]30 (polyvinyl pyrrolidone) as a binder with superior binding powers and 3.5 \pm 0.5% of a Kollidon[®]CL (crosspovidone) as a disintegrant which ensure that the tablet disintegrates and releases active ingredients rapidly in contact with water. Its main characteristics are controlled particle size, high bulk density, low degree of hygroscopicity, good flowability, and the possibility of producing tablets with good hardness and low friability independent of machine speed.

For tablet preparation for intrinsic dissolution the following wax was used:

- Paraffin wax, white pellets, solidification point 50-52°C, Fluka, Chemie AG, Switzerland.

All other chemicals and reagents purchased from commercial sources were of analytical grade.

5.2. Methods

5.2.1. Characterization of CBZ anhydrous

5.2.1.1. High performance liquid chromatography (HPLC)

HPLC was used for identification (assay) of carbamazepine and impurity test. Carbamazepines A, B, P were assayed by using HPLC System (Shimadzu, Japan), equipped with a photon diode area detector. A reversed-phase column Luna 100a CN 250mm x 4.0mm, 10 μ m was used. A mobile phase consisting of water, methanol and tetrahydrofuran (850:120:30) with the addition of formic acid and triethylamin was prepared. UV-detection at 230nm was made. Flow rate was 2ml/min and injection volume 20 μ l. Sample solutions were prepared by dissolving a certain amount of carbamazepine in methanol. Each measurement was repeated two times.

Assay was calculated according to the following formula:

$$\% = \frac{P_p \cdot m_{st}}{P_{st} \cdot m_p} \cdot f \cdot 100 \quad \text{Equation 5.1}$$

where:

P_p and P_{st} – area under peak of sample and standard respectively

m_p and m_{st} – weight of sample and standard (mg)

f – factor to eliminate the humidity in standard ($f = 100 / (100 - \text{loss on drying})$)

5.2.1.2. Fourier transform infrared spectroscopy (FTIR)

FTIR spectroscopy was accomplished with a microscope Olympus BX/51-52 (Olympus, Japan) modified with an infrared microspectrometer IlluminatIR® (Smith Detection, USA), and equipped with an ATR objective (attenuated total reflectance objective). Only small amount of crystals was placed onto the microscopical slide and analyzed at room temperature. Setting parameters were: resolution 4cm^{-1} , data region $4000 - 700\text{ cm}^{-1}$, aperture $100\mu\text{m}$, energy 27000, detector type MCT (mercury-cadmium-telluride) and numbers of runs per spectrum 32.

5.2.1.3. Determination of residual moisture content

Loss on drying measurements were carried out according to European Pharmacopoeia Ph.Eur.5., using an infrared balance Type LP 16M (Mettler Toledo, Switzerland). Samples of approximately 1g were heated up for 2 hours at temperature of 105°C .

5.2.1.4. Scanning electron microscopy (SEM)

The morphology of the bulk materials and the lower surface of CBZ compacts before and after intrinsic dissolution were determined by scanning electron microscopy. SEM images were taken using an ESEM XL 30 FEG (Philips, The Netherland). The samples were mounted with carbon adhesive on aluminum holder, sputtered with gold and photographed at a voltage of 10kV. In the case of compacts, Ag was used as additional conductor.

5.2.1.5. Particle size analysis (PSA)

The average particle size and particle size distribution were determined by laser diffraction technique with a Malvern Mastersizer 2000 (Malvern Instruments, United Kingdom) using dry unit Scirocco 2000 (Malvern Instruments, United Kingdom). The following instrument settings have been done: measurement time 10s, measurement snaps 10000, vibration feeding rate 45%, and dispersive air pressure 0,1bar. In order to have a representative sampling and good reproducibility of results, before applying powders in measurement unit, sample was shaken for 10 seconds. The measurement was carried out six times and five consecutive values with the smallest variation were taken in account. An obscuration value between 1 and 10% was achieved in all measurements. Particle size and particle size distribution were calculated on Malvern software.

5.2.1.6. True density

The true density was measured with a helium pycnometer AccuPyc 1330 (Micrometrics, USA) with nominal cell volume of 10ml. As the true density is expressed as a quotient of mass and volume, the samples were weighted on balance AX204 (Mettler Toledo, Switzerland) and placed in the cell. The volume was determined by purging each sample 10 times with helium. The first five runs were considered as an equilibrating procedure and the average of the last five measurements was taken as the value for true density.

5.2.1.7. Bulk and tap density

The bulk and tap density were determined using an appropriate apparatus Type STAV 2003 (Engelsmann AG, Germany). 100g sample was placed into a graduated cylinder. The volumes at the beginning (bulk volume V_0) and after tapping 1250 times (tap volume V_{1250}) were noted. The bulk density (ρ_b) was calculated as a ratio of mass and initial volume V_0 , while the tapped density (ρ_t) was calculated as a ratio of mass and tapped volume V_{1250} . The Hausner ratio (HF) and the Carr's index CI were determined according to following equations:

$$HF = \frac{\rho_t}{\rho_b} \quad \text{Equation 5.2}$$

$$CI = \frac{(\rho_t - \rho_b)}{\rho_t} \cdot 100 \quad \text{Equation 5.3}$$

where:

HF - Hausner ratio ρ_b – bulk density (g/cm³)
 CI - Carr's index (%) ρ_t – tapped density (g/cm³)

Hausner ratio values less than 1.25 indicate good flow, whereas values greater than 1.25 indicate poor flow. For values between 1.25 and 1.5, added glidant normally would improve flowability.

Carr's index can be interpreted as in table 5.1:

Table 5.1 Interpretation of Carr's index

Carr's index (%)	Type of flow
5-15	Excellent
12-16	Good
18-21	Fair to passable
23-35	Poor
33-38	Very poor
>40	Extremely poor

5.2.1.8. X-ray powder diffraction

X-ray powder diffraction profiles of powders were taken at room temperature with a Diffractometer D5000 (Siemens, Germany). Powder samples were placed in special sample holders, and the surface was excess off powder was removed to be totally flat. The operating conditions were as following: Ni filtered Cu-K α radiation ($\lambda=1.5406\text{\AA}$), voltage 40kV, current 30mA; step 0.02° step time 1.2s, angular scanning speed 1° 2 θ /min and angular range between 2° and 40° 2 θ scale.

5.2.1.9. Thermal analysis

5.2.1.9.1. Differential scanning calorimetry (DSC)

DSC measurements were performed using a Differential Scanning Calorimeter, Pyris 1, (Perkin Elmer, USA). CBZ samples of 4-6mg were weighed into 30 μ l perforated aluminum pans and scanned from 40 to 220°C at the heating rate of 10 and 40°C/min and at the flow rate of nitrogen gas of 20ml/min. The Pyris 1 instrument was calibrated with indium and zinc prior to analysis. Baseline runs were performed by scanning empty perforated Al pans in the temperature range between 40 and 250°C in order to test the thermal behavior of the measuring system itself and the degree and influence of unavoidable asymmetries. DSC measurements were performed in triplicate.

5.2.1.9.2. Thermogravimetric analysis (TGA)

Thermogravimetric analyses were conducted on the Pyris TGA 6 (Perkin Elmer, USA). Samples of 8-10mg were weighed into sample pan and scanned from 40 to 220°C at the heating rate 10°C/min with nitrogen gas flow rate 100ml/min. Loss of mass was registered on instruments microbalance. TGA measurements were conducted in triplicate.

5.2.1.9.3. Hot stage microscopy (HSM)

Physical changes in the samples during heating were monitored by hot stage microscopy. Lynkam THMS 600 (Lynkam, United Kingdom) was used as a hostage unit. A small amount of each sample was placed on a glass slide and scanned at the same heating rate and the same temperature range as for DSC measurements, (see 5.2.1.9.1). The changes in the samples were observed via an optical microscope Olympus BX51 (Olympus, Japan) with 10x magnification.

5.2.1.10. Solubility

Equilibrium solubility was determined by adding an excess amount of sample into 100ml of distilled water. The samples were placed in a shaker, set at 100rpm, and tempered by water bath (Heto, Denmark) at 37 \pm 1°C for 72hours (Murphy et al., 2002). Samples of

2ml milliliter were withdrawn at the following time intervals: 5, 10, 15, 20, 25, 30, 45, 60, 90min, 2, 4, 8, 12, 24, 36, 48 and 72h. Then, they were filtered and analyzed by UV/VIS spectrophotometer (Beckman, USA) at $\lambda=285\text{nm}$. Solubility measurements were performed in triplicate.

5.2.1.11. Porosity

The porosity of CBZ compacts was measured using a mercury porosimeter PoreSizer 9320 (Micrometrics, USA). Three tablets were used for each analysis. The sample cell was filled with mercury in an evacuated state. The low pressure run was performed manually in the pressure range from 5 – 20psia (i.e. 35-150kPa) and the high pressure run was automatically done in the pressure range from 20psia – 30kpsia (i.e. 150-207MPa) with an equilibrium time of 10s after each pressure.

The porosity of compacts was also calculated using the following equation:

$$\varepsilon = \left(1 - \frac{m}{V_t \cdot \rho_t} \right) \cdot 100 \quad \text{Equation 5.4}$$

where:

ε – porosity of tablet (%)

m – weight of tablet (g)

V_t – volume of the tablet (cm^3)

ρ – true density of powder (g/cm^3)

The thickness of the tablet for calculation was measured with a thickness gauge 532 G (Compac, Switzerland). The tablet volume was calculated geometrically from the diameter and thickness.

5.2.1.12. Intrinsic dissolution rate

The intrinsic dissolution rate was measured by the rotating disk method. A compact of 11mm diameter was prepared by compacting 400mg of sample using Zwick 1478 material tester (Zwick, Germany) with flat faced round punches. CBZ samples were

compacted to a constant porosity of $12\pm 0.3\%$. Compaction, decompression and ejection speed were kept constant, 10mm/min, 25mm/min and 10mm/min respectively. The punch and die were constantly lubricated before each compaction process with magnesium stearate powder. The excess of lubricant was removed with compressed air. Five compacts were prepared for each examined samples and they were stored at the constant conditions at room temperature and a relative humidity 42% (using the saturated solution of K_2CO_3).

Prior to dissolution test, compacts were embedded in paraffin wax which was melted at the temperature of $70-80^\circ\text{C}$. Only the lower punch side with a surface of 0.95cm^2 was left to the outside to be in direct contact with dissolution medium.

Disc intrinsic dissolution was performed at 100rpm in 400ml of distilled water, as dissolution medium, at $37\pm 1^\circ\text{C}$ for 120min. Additionally, in order to get a homogeneous dissolution media, a magnet stirrer was placed at the bottom of each vessel (see figure 5.1).

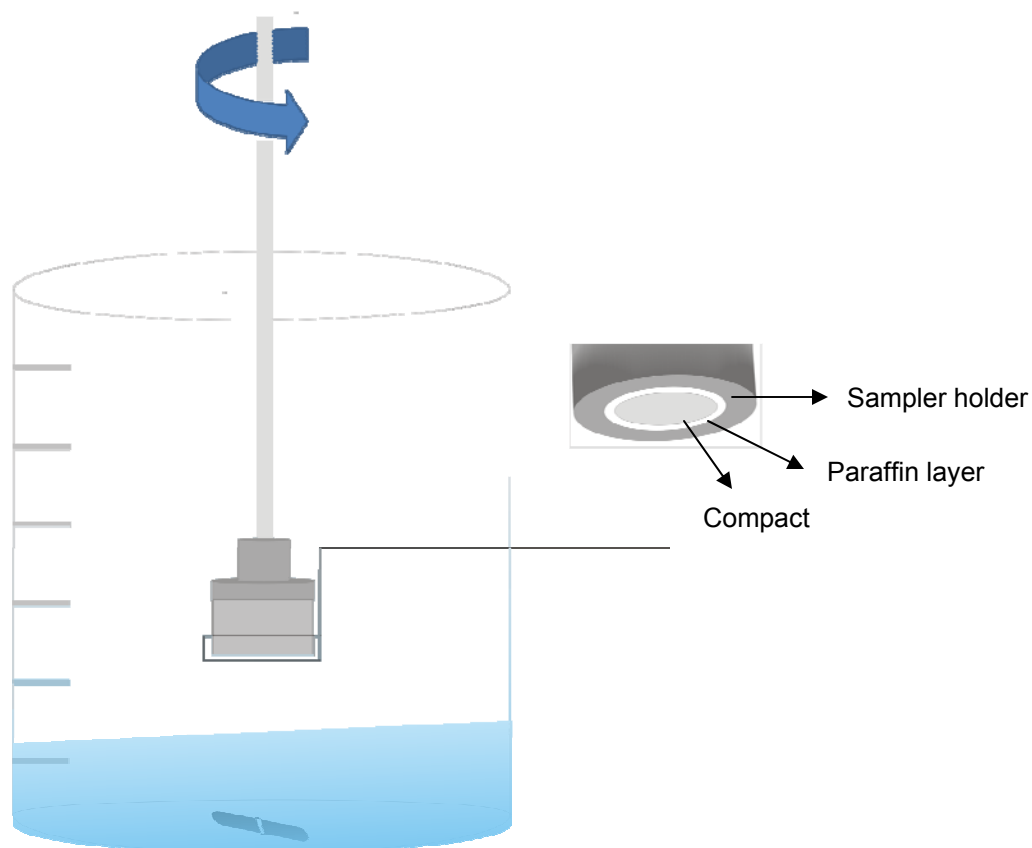


Figure 5.1 Disc intrinsic dissolution apparatus

Aliquots of 5ml were withdrawn every minute during the first 20min, then every 5min during the first hour, and afterward every 10min during the second hour. Dissolution media was replaced after every sampling. Concentration of CBZ in solution was measured by UV spectrophotometer DU 530 (Beckman, USA) at wavelength of 285nm. The sink conditions were maintained during the whole dissolution experiment, which means that the total concentration of investigated drug dissolved in dissolution medium was not higher than 10% of its saturated concentration.

5.2.2. CBZ dihydrate

5.2.2.1. Preparation of dihydrate

CBZ dihydrates (CBZ D) were prepared by crystallization of all 10 available CBZ anhydrous forms by suspending samples in distilled water and stirring with a magnetic stirrer for 24h at room temperature. The precipitated crystals were filtrated on filter and dried at room temperature. Dihydrates were stored at room temperature and a relative humidity of 55-60% to maintain hydrate conditions (McMahon et al., 1996).

5.2.2.2. Characterization of CBZ dihydrate

Carbamazepine dihydrates were characterized using the same methods as for CBZ anhydrous: x-ray diffraction (see 5.2.1.8.), thermal behavior by DSC (see 5.2.1.9.1.), morphology (see 5.2.1.4), loss on drying (see 5.2.1.3.), solubility (see 5.2.1.10.) and disc intrinsic dissolution (see 5.2.1.11.).

5.2.3. Carbamazepine binary mixtures

5.2.3.1. Preparation of binary mixtures

Carbamazepine CBZ A3, CBZ B3, CBZ P3 and CBZ D were selected to be investigated in binary mixtures with Fast Flo[®] lactose as an excipient. Mixtures were prepared in ratios presented in table 5.2. Mixtures were mixed in a blender Turbula T2C (W. Bachofen, Switzerland) for 10 minutes prior to compaction.

Table 5.2 Binary mixtures of CBZ A, B, P and D and Fast Flo[®] lactose

Mixture	Carbamazepine (%)	Fast Flo lactose (%)
Mixture 1	90	10
Mixture 2	80	20
Mixture 3	70	30
Mixture 4	60	40
Mixture 5	50	50
Mixture 6	40	60
Mixture 7	30	70
Mixture 8	20	80
Mixture 9	10	90

5.2.3.2. Tableting of binary mixtures

Tablets with constant porosity were prepared by using Zwick material tester (for compaction parameters see 4.2.1.12.). The porosity of $12\pm 0.5\%$ was kept constant in order to compare the obtained data with data of pure CBZ compacts.

Prepared compacts were stored for two weeks at room temperature at two different storage conditions in desiccators under saturated salts solutions (at 55-60%RH using sodium bromide and at 85-90%RH using potassium chloride).

5.2.3.3. Disintegration of binary mixtures

The disintegration time of binary mixtures was measured with disintegration apparatus Sotax DT3, (Sotax AG, Switzerland). The disintegration medium used was distilled water, at the temperature of $37\pm 1^\circ\text{C}$. The tablets were considered disintegrated when no residue of the units remained in the basket. For each binary mixture and formulation, six tablets were tested and the time taken to complete the disintegration was recorded.

5.2.3.4. Intrinsic dissolution of binary mixtures

Intrinsic dissolution test was performed as for CBZ pure compacts (see 5.2.1.11.).

5.2.4. Carbamazepine formulations

5.2.4.1. Preparation of CBZ formulations

Five different formulations have been prepared consisting of CBZ (USP standard, CBZ A3, CBZ B3, CBZ P3 and CBZ D), Ludipress[®] and magnesium stearate. Formulations were mixed in blender Turbula T2C (W. Bachofen, Switzerland) for 5min.

5.2.4.2. Tableting of CBZ formulations

Tablets of 350mg for each formulation were produced using Presster[™] compaction simulator (MCC, USA) with flat faced round punches of 10mm diameter. The tablet press simulated was Korsch PH336, with desired press speed of 10800 TPH (tablet per hour) and resulting dwell time of 32.0 ± 1.9 ms. The porosity of the tablet was kept constant ($12.7 \pm 0.2\%$), simulating the porosity of marketed CBZ tablets, and in respect to that the gap value was adapted in the range from 2.75 to 2.90mm.

5.2.4.3. Tablet strength

The tablet strength was measured using the tablet tester Dr.Schleuniger (Pharmatron, Switzerland). Six tablets were used for each measurement and average value was calculated.

5.2.4.4. Disintegration of CBZ formulations

Disintegration test was performed as for binary mixture tablets (see 5.2.3.3.)

5.2.4.5. Dissolution

The dissolution test for the five CBZ formulations (CBZ, Ludipress[®] and magnesium stearate) was performed according to USP XXXI for dissolution of Carbamazepine immediate release tablets, dissolution apparatus II (USP31, 2008). The dissolution apparatus used was VK7025 (Varian, USA). Dissolution media was 900ml of distilled water containing 1% of sodium lauryl sulfate at $37 \pm 1^\circ\text{C}$, with a rotation speed of 75rpm during 60min. Samples of 5ml were withdrawn every five minutes during the dissolution, and replaced by the same amount of dissolution media. Concentration of CBZ in solution was measured by UV spectrophotometer (Perkin Elmer, USA) at wavelength of 288nm. The weight of each tablet was used in the calculation of dissolved percentage of the drug.

6. Results and discussion

6.1. Carbamazepine anhydrous

6.1.1. Identification of carbamazepine raw material

The available carbamazepine samples were submitted to several analytical tests to check their identity and quality. The standard specification for carbamazepine and the limits of allowed values are listed in appendix 9.1. The examined commercial CBZ samples were in accordance with the specification for all above mentioned parameters. No impurities were found in any of investigated samples, see table 6.1.

Table 6.1 Results of analysis of raw material

Sample	A ₁	A ₂	A ₃	B ₁	B ₂	B ₃	P ₁	P ₂	P ₃
Appearance	√	√	√	√	√	√	√	√	√
Solubility(g/100ml)									
water	0,01068	0,01216	0,01136	0,01079	0,01087	0,01307	0,01234	0,01152	0,01214
ethanol	1,00179	1,00721	1,00635	1,00442	1,00592	1,02082	1,01754	1,00746	1,00687
methylene Cl	10,3542	10,3626	10,1755	10,5397	10,3232	10,5394	10,1087	10,2573	10,2001
acetone	1,01143	1,00427	1,00508	1,02445	1,04531	1,03519	1,03605	1,00568	1,03371
Melting point	190,9	191,1	190,7	190,7	190,8	190,8	191,5	191,4	191,5
Acidity/alkalinity	√	√	√	√	√	√	√	√	√
Impurities(%)	0	0	0	0	0	0	0	0	0
Chloride	√	√	√	√	√	√	√	√	√
Heavy metals	√	√	√	√	√	√	√	√	√
Loss on drying (%)	0,03	0,11	0,01	0,03	0,03	0,09	0,01	0,01	0,02
Sulphated ash (%)	0,06	0,06	0,07	0,02	0,02	0,02	0,08	0,07	0,08

In order to meet the requirement described by Eur.Ph.5. and USPXXXI (USP31, 2008) for the assay test of carbamazepine, the raw material has to contain not less than

98.0% and not more than 102.0% of $C_{15}H_{12}N_2O$, calculated on the dried basis. The results of CBZ assay obtained by HPLC method are presented in table 6.2. All analyzed raw materials complied with the main pharmacopoeias.

Table 6.2 Carbamazepine assay results

Assay (%) \pm SD n=2	CBZ A	CBZ B	CBZ P
batch 1	99,35 \pm 1,05	100,64 \pm 0,20	99,25 \pm 0,50
batch 2	100,51 \pm 1,84	99,55 \pm 0,82	99,89 \pm 0,66
batch 3	99,25 \pm 0,09	100,11 \pm 1,10	99,50 \pm 0,88

6.1.2. FTIR

The band characteristics for CBZ are in the range of 3490-3460 cm^{-1} where NH valence vibration occurs, then in the range of 1700-1680 cm^{-1} where $-CO-R$ vibration is pronounced, and in the range around 1600 cm^{-1} absorption bands are happening due to $-C=C-$ and $-C=O$ vibration, and $-N-H$ deformation. These are also the main regions for identifying and distinguishing between different polymorphs of CBZ by IR spectrum. Generally, there is a shift of band position to higher wave numbers starting from polymorphic form III to form I respectively. In particular the bands at 3464, 1676 and 1383 of form III, are shifted to the bands 3473, 1673 and 1393 in the case of form II and to 3484, 1684 and 1397 for form I (Rustichelli et al., 2000). Intensity of the peaks and peaks at any additional band are valuable information for the polymorphic characterization. In the case of polymorphic form III the peak at 1471 is less intense than the peak at 1245, while for polymorphic form I these two peaks have the same intensity.

The results for different modifications obtained by Krahn, Rustchelli and Griezak (Grzesiak et al., 2003, Krahn et al., 1987, Rustichelli et al., 2000) are summarized in table 6.3, and are used as references for polymorphic characterization in this study. The FTIR spectra of anhydrous carbamazepine samples are shown in figure 6.1.

According to the literature data (see table 6.3.), these spectra corresponded to the spectra of polymorphic form III showing the characteristic absorptions at 3463-3462, 1673-1672, 1604, 1593-1592, 1379-1378, 1269, 1244 and 851 cm^{-1} . CBZ USP standard

was also analyzed by FTIR microspectroscopy, and found to be polymorphic form III. The FTIR spectrum of CBZ USP are presented in appendix 9.2. There was no variation in the FTIR results of the commercial samples in comparison to the FTIR spectrum of CBZ USP standard.

Table 6.3 Summary of typical bands for carbamazepine IR spectrum (Grzesiak et al., 2003, Krahn et al., 1987, Rustichelli et al., 2000)

Range(cm ⁻¹)	3500-3450	1700-1689	1600	830-770	Additional bands
Krahn:					
Form I	3489	1695	2 bands	811,800,783	
Form II	3473	1688	1 band	815,783,770	1275,1135,960
Form III	3468	1680	2 bands	810,775	
Rustichelli:					
Form I	3484	1684		954, 853	1397,1270,1251
Form II	3473	1673		954, 853 (weak)	1393,1271,1249
Form III	3464	1676	1605,1593	850 (weak)	1383,1271,1245
Griezak:					
Form I	3485	1688	1602,1593	773	1396,1271,1251
Form II	3485	1690	1603,1593	803,772	1395,1270,1251
Form III	3466	1677	1605,1595	767	1386,1270,1246
Form IV	3474	1674	1603,1591	773,765	1394,1271,1249

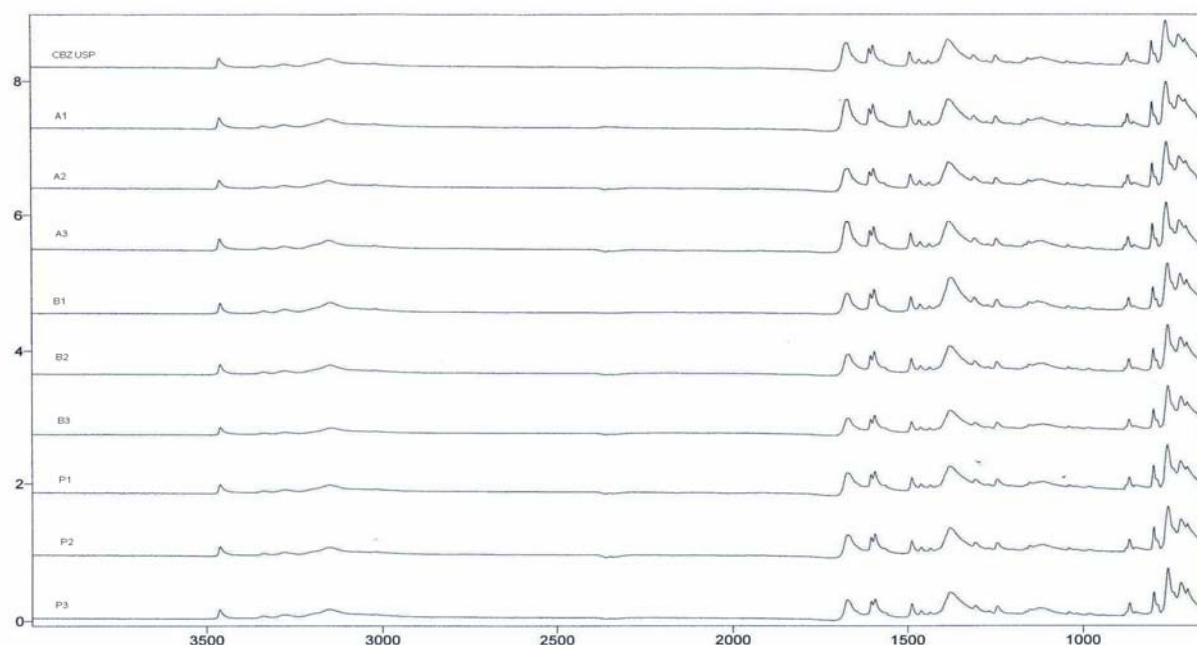


Figure 6.1 FTIR spectrum of CBZ samples

6.1.3. Synthetic pathways

Crystallization is widely used in pharmaceutical and chemical industries for purification of the final crystal form or for particle size control. In crystallization process it is sometimes necessary to use mixture of solvents in order to reduce the solubility of solute or to change the dependence of the solubility on temperature, to increase the yield of cooling crystallization. However, the concentration of the second solvent used in that process can affect polymorphism, pseudopolymorphism and morphology of the crystalline product. Consequently, production of the pharmaceutical solid products has to be optimized in terms of final solid form, crystal habit and size distribution, final yield and batch to batch reproducibility (Qu et al., 2006). Crystal properties such as polymorphism, habit, and particle size also can be changed by using different crystallization techniques. The nature and the extent of these changes depend on the crystallization conditions such as presence of impurities, and cooling rate (Nokhodochi et al., 2004). Crystal shape and crystal disruption formed during or after crystallization process are important for the process-ability of raw materials and therefore, for the efficacy and performance of the final solid dosage form.

The influence of solvent on polymorphic form can be explained on CBZ. The monoclinic form (form III) is predominantly obtained when CBZ is crystallized from various solvents with high dielectric constant like *sec*-butyl alcohol, *i*-propyl alcohol, *n*-propyl alcohol, ethanol and methanol. The pure monoclinic form is obtained when a slow cooling rate during the crystallization process is maintained. The trigonal form (form I) is obtained upon crystallization from solvents with low dielectric constants like carbon tetrachloride, tetrahydrofuran, and cyclohexane, irrespective of cooling rate (Lowe et al., 1986).

Several reports are concerned about changing the crystal habit or polymorphism in the presence of impurities during the crystallization of CBZ (Bolourtchian et al., 2001, Luthala, 1992, Nokhodochi et al., 2004, Rodriguez-Hornedo et al., 2004). Also the presence of small amounts of an effective additive in the crystallization medium can dramatically change the crystal size and shape of CBZ (Luthala, 1992).

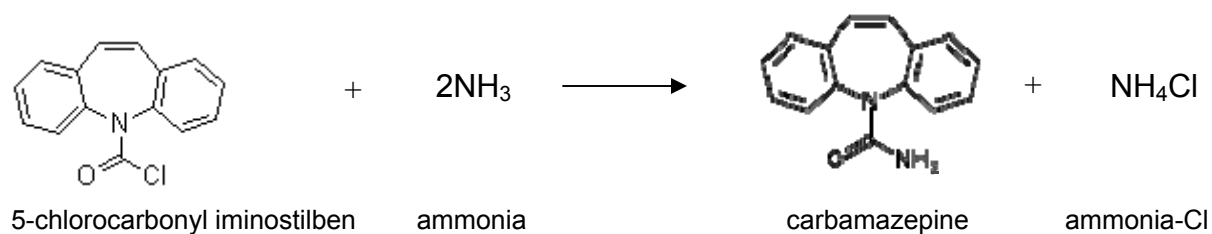
The changes in morphology of CBZ crystals which are happening during crystallization process could be due to variations in face dimensions or appearance or disappearance of some faces. In other words, under certain crystallization condition one part of the

crystal may be induced to grow faster (or slower) than other parts. This is why using the same method with different additives can change the pattern of crystal growth from block-shaped to polyhedral crystals (Nokhodochi et al., 2004).

The synthetic pathway of carbamazepine is presented in table 6.4, as it was declared by the respective producers in the open part of the carbamazepine's Drug Master Files (DMF). CBZ is manufactured in two stages:

- First step is the synthesis of CBZ from 5-chlorocarbonyl iminostilben and ammonia as starting materials, for CBZ A and CBZ B ammonia gas is used, while in the case of CBZ P ammonia was in liquid state;
- Second stage is recrystallization process of a drug from a solvent, which is usually used for the purification of drugs during the final stage of manufacturing (see figure 6.2).

1st stage



2nd stage



Figure 6.2 Two stage of the manufacturing of carbamazepine

Table 6.4 Comparison of synthetic pathways of

	CBZ A	CBZ B	CBZ P
1 st stage	<ol style="list-style-type: none"> 1. methanol; stirring 10-15min 2. cooling at 5 – 10°C 3. heating at 20°C 3h 4. distillation of methanol at 60-65°C 5. slurring in water 6. centrifugation at 50 ± 2°C for 1h 7. drying at 70 – 80°C 	<ol style="list-style-type: none"> 1. toluen; ethanol 2. centrifugation 3. spin drying for 1h 	<ol style="list-style-type: none"> 1. toluene; heating 75-80°C 1h 2. cooling to 20 – 25°C crude 3. filtration 4. washing with water 5. centrifugation
2 nd stage	<ol style="list-style-type: none"> 1. dissolving in acetone/water mixture 2. heating at 55 - 60°C 3. active carbon 4. charcoalization; clarification 5. cooling /chilling to 0 – 2°C 3h 6. centrifugation and spin drying 7. washing with water 8. drying under 600-650 mmHg; 65-70°C 9. sifting 	<ol style="list-style-type: none"> 1. ethanol 2. filtration (sparkler filter) 3. chilling 4. centrifugation 5. drying in fluidized bed until less than 0.5% moisture 6. pulverizing 7. sieving 	<ol style="list-style-type: none"> 1. methanol 60% solution in water 2. heating to ~ 65°C (boiling) 3. active carbon 4. filtration 5. cooling with glycol to 10°C 6. centrifugation 7. washing with 50% solution of methanol 8. drying 9. grinding

All producers have used different processes during the manufacturing of carbamazepine raw material. The crystallization process took different time periods and in some cases grinding was used as final step, for which is known that it can produce some amorphousness of CBZ (Murphy et al., 2002). The producers used different solvents in the recrystallisation process of CBZ, such as methanol/acetone in case of CBZ A, toluene/ethanol in case of CBZ B and toluene/methanol in case of CBZ P. All of these factors could cause variations in the examined samples.

The content of residual organic solvent may be an interesting parameter to be investigated because organic solvent may remain and be present in carbamazepine. In contact with water organic residuals can help or promote the conversion of polymorphic forms. However, analysis of solvent residual was not performed in this study.

6.1.4. Morphology

The commercial carbamazepine samples were declared by producer to be polymorphic form III (monoclinic) with a prismatic shape. CBZ USP is chemically pure standard with very small particles of prismatic shape, while CBZ USP D - dihydrate made from USP standard exhibited the needle-like formation typical for CBZ dihydrate. The scanning electron micrograph pictures of USP standard and CBZ USP dihydrate are presented in figures 6.3 and 6.4, respectively.

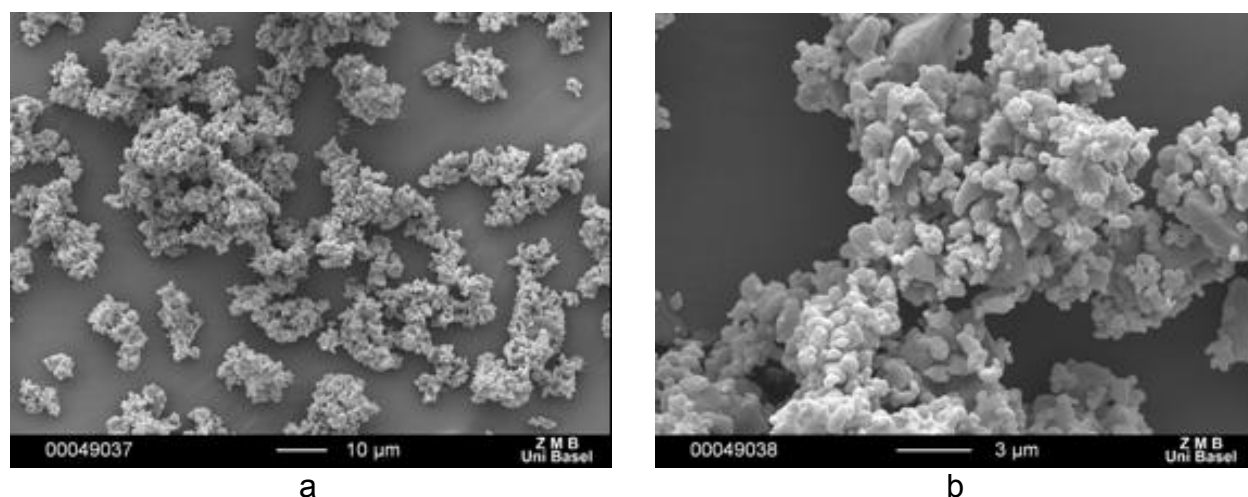


Figure 6.3 Scanning electron micrographs of CBZ USP a (100x) and b (1000x)

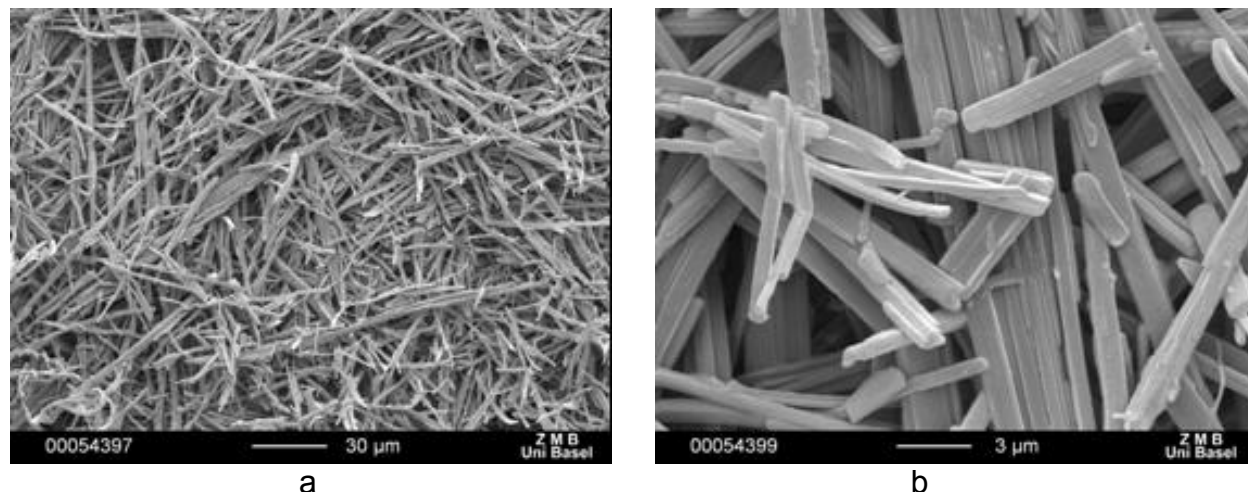


Figure 6.4 Scanning electron micrographs of CBZ USP dihydrate a (1000x) and b (5000xmagnification)

Those of carbamazepines CBZ A, B and P are presented in figures 6.5, and it is seen that they exhibited different morphology of the particles.

Although all commercial anhydrous CBZ appeared to be prismatic, particle shape varied among them. CBZ A had crystals with more elongated and tabular shape, while CBZ B and CBZ P crystals looked like polyhedrons or prisms, and had different sizes of particles. Since solvent type and crystallization conditions have a significant effect on carbamazepine crystal modification (Bolourtchian et al., 2001), the variations in the morphology of the commercial samples were probably caused by the type of solvent used in the second stage of CBZ manufacturing i.e. acetone for CBZ A, and alcohols for CBZ B and CBZ P.

Figure 6.6 shows some of the anomalies found only in crystals of CBZ P. In the case of CBZ P, the last step during the production of raw material was grinding. Grinding, as mechanical stress, can promote a formation of amorphous carbamazepine (Murphy et al., 2002) or may cause a disruption in the crystal lattice.

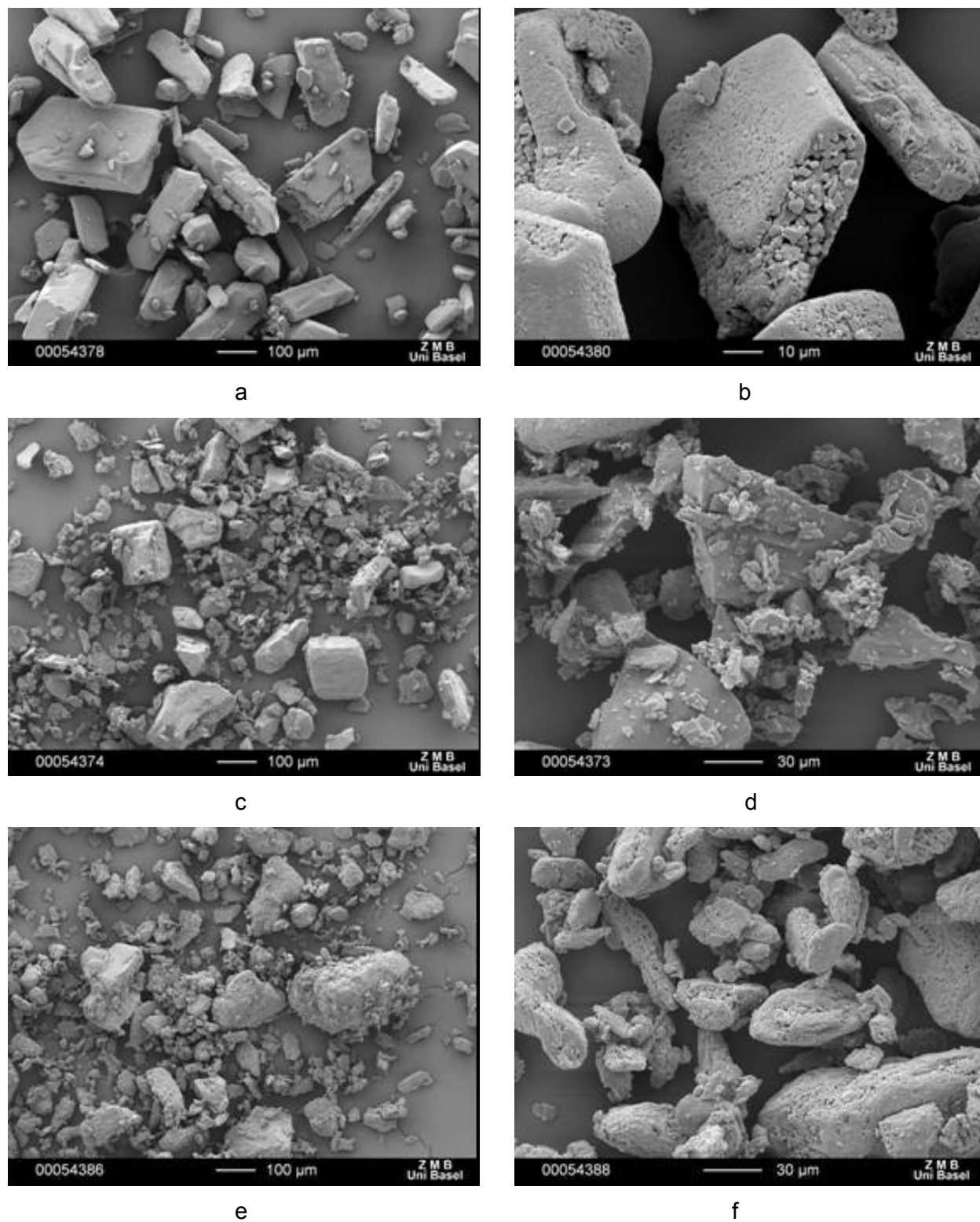


Figure 6.5 Scanning electron images of CBZ A (a 100X, b 1000X), CBZ B (c 100X, d 1000X), and CBZ P (e 100X, f 1000X)

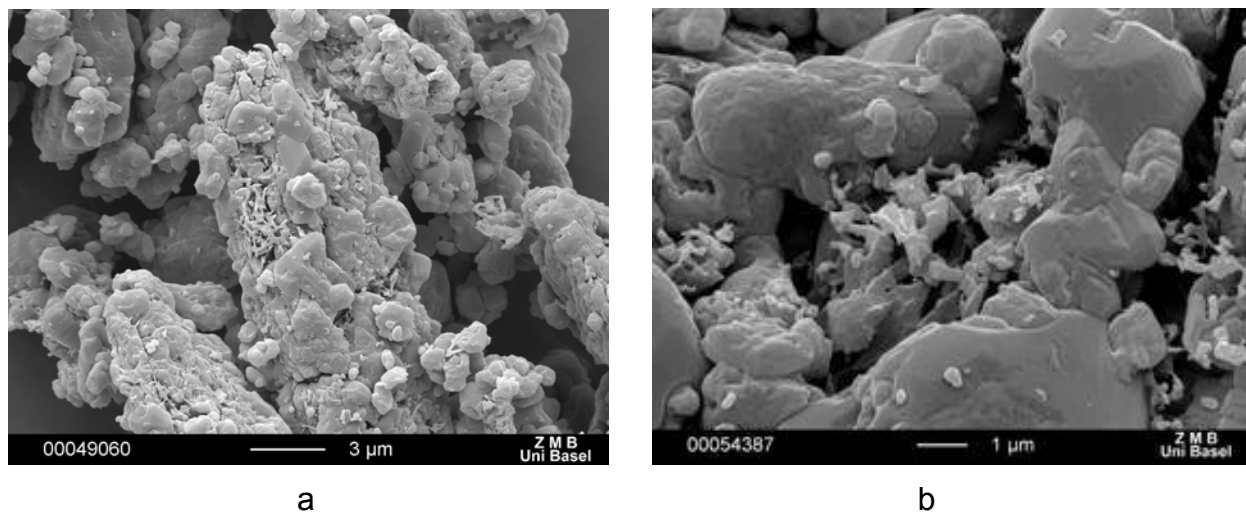


Figure 6.6 Scanning electron images of CBZ P, (a magnification 1000x, b 5000X)

6.1.5. Particle size and particle size distribution

Particle size and particle size distribution are important parameters of the compound because they are directly influencing dissolution rate, absorption rate, bioavailability and stability of the drug, especially for poorly soluble compounds where the absorption process is rate-limited by the dissolution rate.

Particle size distribution was determined by laser diffraction. Two types of methods are used in laser diffraction particle size measuring: wet and dry method. Wet dispersion is the most widespread method for obtaining reproducible results. Usually, a medium in which the analyzed compound is not soluble, is used to provide a dispersion of the particles to be measured. Some of the advantages of this method are: dispersion of particles can be readily achieved for diverse particle systems due to wide range of available dispersants; dispersion stability can be optimized which is not the case of the dry method; good for sticky and strongly agglomerated powders; reproducibility of results is high and friability of materials is not important because the wet method is less aggressive compared to the dry analysis (Malvern, 2000).

In the dry method, particles are dispersed by air pressure with a dry powder feeder which has a similar design to that of an air jet mill. During the measurement, particles are subjected to high acceleration, with the applied shear being related to the dispersant pressure setting. This together with particle-particle and particle-wall collision helps to disperse agglomerates. The most important thing for a good dry measurement is to

apply a high enough pressure to cause particle dispersion. Nevertheless, for friable materials care must be taken because the use of high dispersion pressure may result in the fracture or attrition of the material and milling of the product. To determine the most suitable pressure for dispersion and to avoid eventual milling, several measurements of particle size as a function of pressure must be taken. Comparing the results obtained by the dry method with the results obtained by the wet method of the well-dispersed material can help choose the correct pressure (Malvern, 2000).

For particle size analysis (PSA) of carbamazepine the dry method was developed because the compound itself is slightly soluble in the common dispersant used for wet methods (like alcohol, acetone etc). Although CBZ is practically insoluble in water, water as a medium for dispersion of particles could not be used because carbamazepine has the tendency of hydration, which affects also its particle size and particle shape (transformation from prismatic to needle-like shape). This was confirmed in preliminary experiments using light microscopy to compare the dry crystals (see figures 6.7) with those dispersed in water (see figure 6.8).

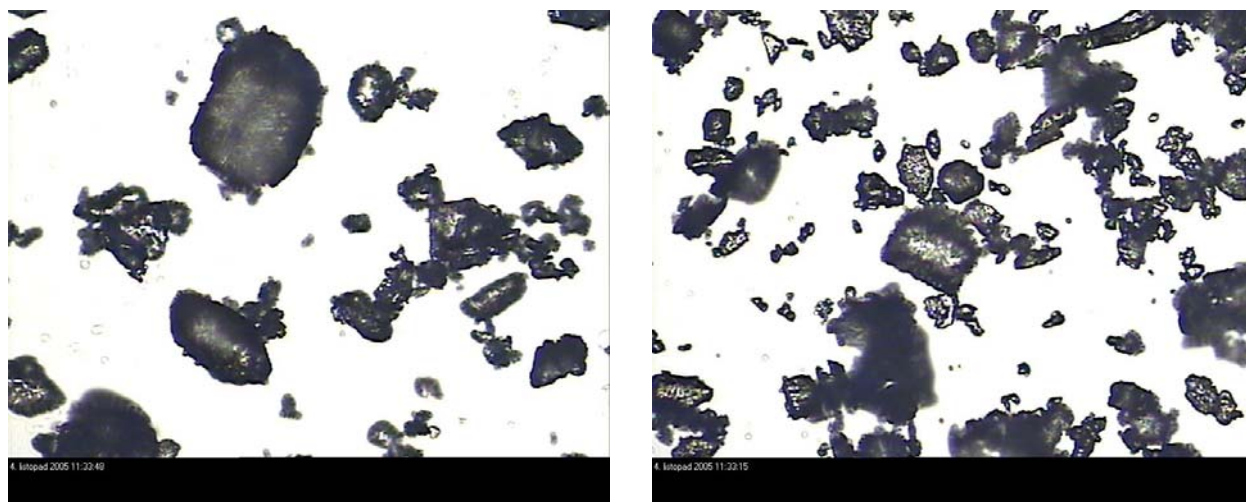


Figure 6.7 Light microscopy pictures of dry particles of CBZP

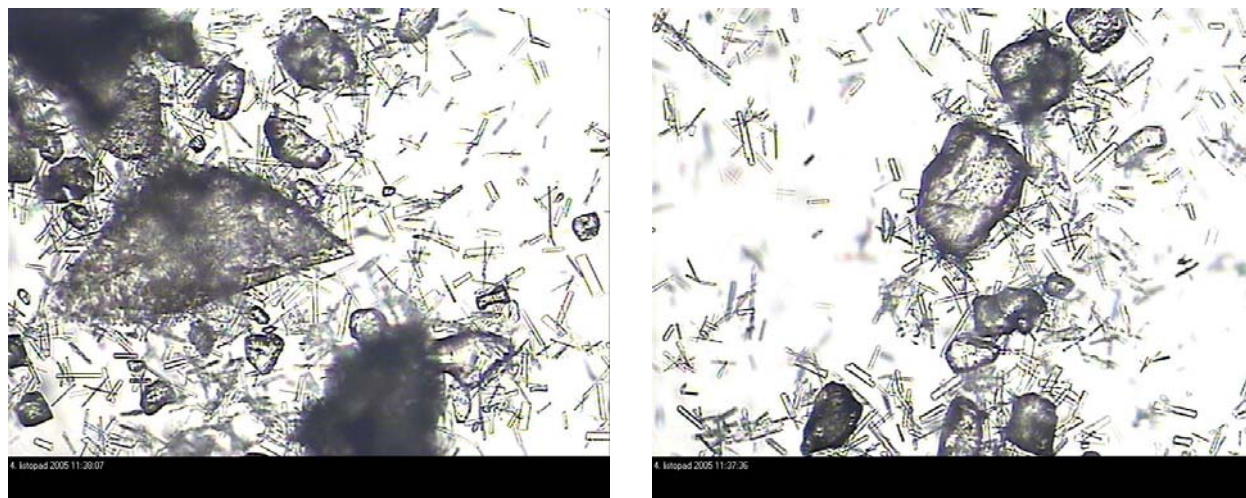


Figure 6.8 Light microscopy pictures of CBZP samples taken from Hydro unit after a temptation to develop a wet method for PSA using water as a dispersant (formation of dihydrate)

Therefore, a wet method using toluene as dispersant was used with the aim of verifying the results obtained by dry method. Visualization of the particles dispersed in toluene was done by light microscopy and the results are presented in the following figure 6.9. No morphological change in the CBZ particles dispersed in toluene was observed, which means that toluene is good dispersant for PSA of CBZ. The results obtained by the dry method were consistent with the results obtained in toluene. Comparison of these two methods is presented in figure 6.10. Due to toxicity of toluene, and for safety, and practical reasons, the dry method was used for the subsequent characterization of CBZ in the present work.



Figure 6.9 CBZP dispersed in toluene, the sample after wet PSA measurements

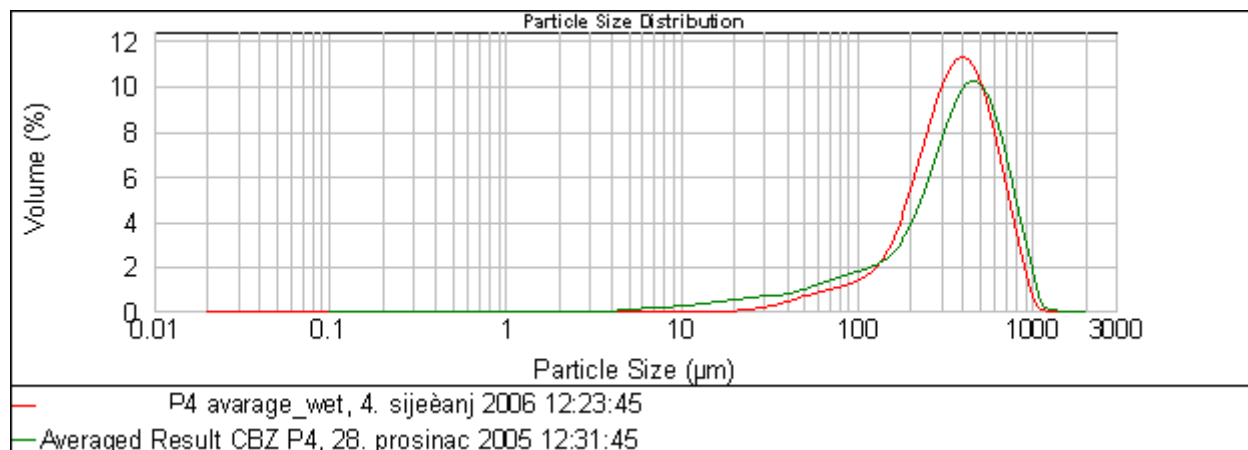


Figure 6.10 Wet vs. dry method.

In order to optimize the pressure used for deagglomeration of the samples in the dry method, pressures in the range from 0.1 until 1bar were applied. The results are shown in appendices 9.3-9.5.

In case of CBZ A increasing the pressure led to particle breaking, see appendix 9.6, which was confirmed by analyzing the particles under the light microscope.

For CBZ B and CBZ P the enhancement of pressure had almost no influence on the results. In order to compare the samples under the same conditions, the pressure of 0,1bar was selected for further experiments.

Furthermore, the stability of the dispersion and the repeatability of the results during the measurement were controlled using the trend graph of the Malvern software. This is illustrated in appendix 9.7, showing five consecutive measurements which gave the same size distribution.

After development of appropriate method, CBZ particle sizes were measured and the results are presented in the table 6.5.

CBZ starting materials from different sources had different particle size. CBZ B samples had the smallest particles among all investigated samples, but standard deviation within batches was the lowest.

Table 6.5 Particle size distribution for anhydrous CBZ

Sample (n=5)	d(0,1) μm	D(0,5) μm	d(0,9) μm
CBZ A1	103.67 \pm 3.08	307.52 \pm 7.93	741.83 \pm 17.18
CBZ A2	105.89 \pm 2.33	327.86 \pm 8.19	821.88 \pm 27.23
CBZ A3	93.33 \pm 4.06	299.43 \pm 11.22	722.13 \pm 23.03
CBZ B1	36.29 \pm 0.45	174.20 \pm 0.46	362.79 \pm 2.54
CBZ B2	44.79 \pm 0.91	191.37 \pm 1.64	384.65 \pm 3.65
CBZ B3	43.76 \pm 1.16	196.69 \pm 2.30	396.22 \pm 4.30
CBZ P1	95.93 \pm 6.26	377.53 \pm 20.44	778.71 \pm 29.75
CBZ P2	65.20 \pm 2.28	295.83 \pm 10.40	668.31 \pm 11.51
CBZ P3	79.48 \pm 3.18	375.24 \pm 10.60	720.19 \pm 13.26

6.1.6. True density, Bulk and Tapped densities

Flowability is one of the principal characteristic of a powder as it plays an essential role in many processes (mixing, filling tableting machine during compaction process, etc.) Bulk density is a simple test developed to evaluate the flowability of a powder by comparing the poured (fluff) density and tapped density of a powder and the rate at which it is packed down. This measurement characterizes the ability of powders for rearrangement under gravity and vibrations. If a powder rearrange easily, it has good flowability.

Table 6.6 True, bulk and tapped density, Hausner ratio and Carr index of anhydrous CBZ samples

Sample (n=3)	True density (g/cm^3)	Bulk density (g/cm^3)	Tapped density (g/cm^3)	Hausner factor	Carr index (%)
CBZ A1	1.346 \pm 0,002	0.563 \pm 0.00	0.654 \pm 0.01	1.16 \pm 0.01	13.91 \pm 0.61
CBZ A2	1.316 \pm 0,002	0.562 \pm 0.01	0.661 \pm 0.01	1.18 \pm 0.02	14.98 \pm 1.16
CBZ A3	1.347 \pm 0,001	0.557 \pm 0.00	0.656 \pm 0.00	1.18 \pm 0.02	15.18 \pm 1.13
CBZ B1	1.338 \pm 0,001	0.541 \pm 0.01	0.693 \pm 0.01	1.28 \pm 0.02	21.94 \pm 0.42
CBZ B2	1.338 \pm 0,001	0.578 \pm 0.02	0.714 \pm 0.00	1.24 \pm 0.03	19.11 \pm 2.12
CBZ B3	1.339 \pm 0,002	0.581 \pm 0.01	0.866 \pm 0.03	1.49 \pm 0.04	32.87 \pm 1.94
CBZ P1	1.340 \pm 0,001	0.669 \pm 0.01	0.792 \pm 0.02	1.18 \pm 0.03	15.57 \pm 1.97
CBZ P2	1.340 \pm 0,001	0.681 \pm 0.02	0.826 \pm 0.01	1.21 \pm 0.02	17.55 \pm 1.02
CBZ P3	1.339 \pm 0,000	0.662 \pm 0.01	0.812 \pm 0.01	1.23 \pm 0.02	18.50 \pm 1.20

Data for true density, bulk and tapped density, Hausner ratio and Carr index respectively are shown in table 6.6. True densities for all CBZ are corresponding to literature data (form III) (Grzesiak et al., 2003). Differences in bulk and tapped density may be noted among CBZ from different producers. Flowability expressed in terms of Hausener ratio for CBZA was good, while CBZB and CBZP have shown higher values and therefore poorer flow properties. According to Carr's index, CBZA had good flow properties, CBZP good to fair, while CBZB exhibit poor flow properties.

6.1.7. X-ray powder diffraction (XRPD)

As every crystalline solid phase has a unique XRPD pattern, this technique is very powerful for identification of crystalline solid states. It is the most reliable method to distinguish the four polymorphic forms of CBZ and its dihydrate. Characteristic peaks for different forms are presented in the table 6.7 (Grzesiak et al., 2003, Krahn et al., 1987, Rustichelli et al., 2000).

Table 6.7 Literature data of XRPD characteristic peaks for CBZ polymorphs (Grzesiak et al., 2003, Krahn et al., 1987, Rustichelli et al., 2000)

2θ	Form I	Form II	Form III	Form IV
Rustichelli: (*II=IV)	6.1, 9.4, 12.25, 19.8, 19.9, 22.8	17.8, 21.2, 33.0*	14.9, 15.2, 15.8, 27.2, 27.5, 32.0	
Griezak:	7.92, 9.37, 12.28, 19.94	8.68, 13.26, 18.56, 24.54	15.36, 19.56, 25.00, 27.47	14.11, 17.89, 21.79, 33.11
Krahn	14.9, 15.2, 15.8, 27.2, 27.5, 32.0	16.5, 18	15, 16, 25	

The anhydrous CBZ samples showed patterns corresponding to polymorphic form III reported in the literature (Grzesiak et al., 2003, Krahn et al., 1987), see figure 6.11.

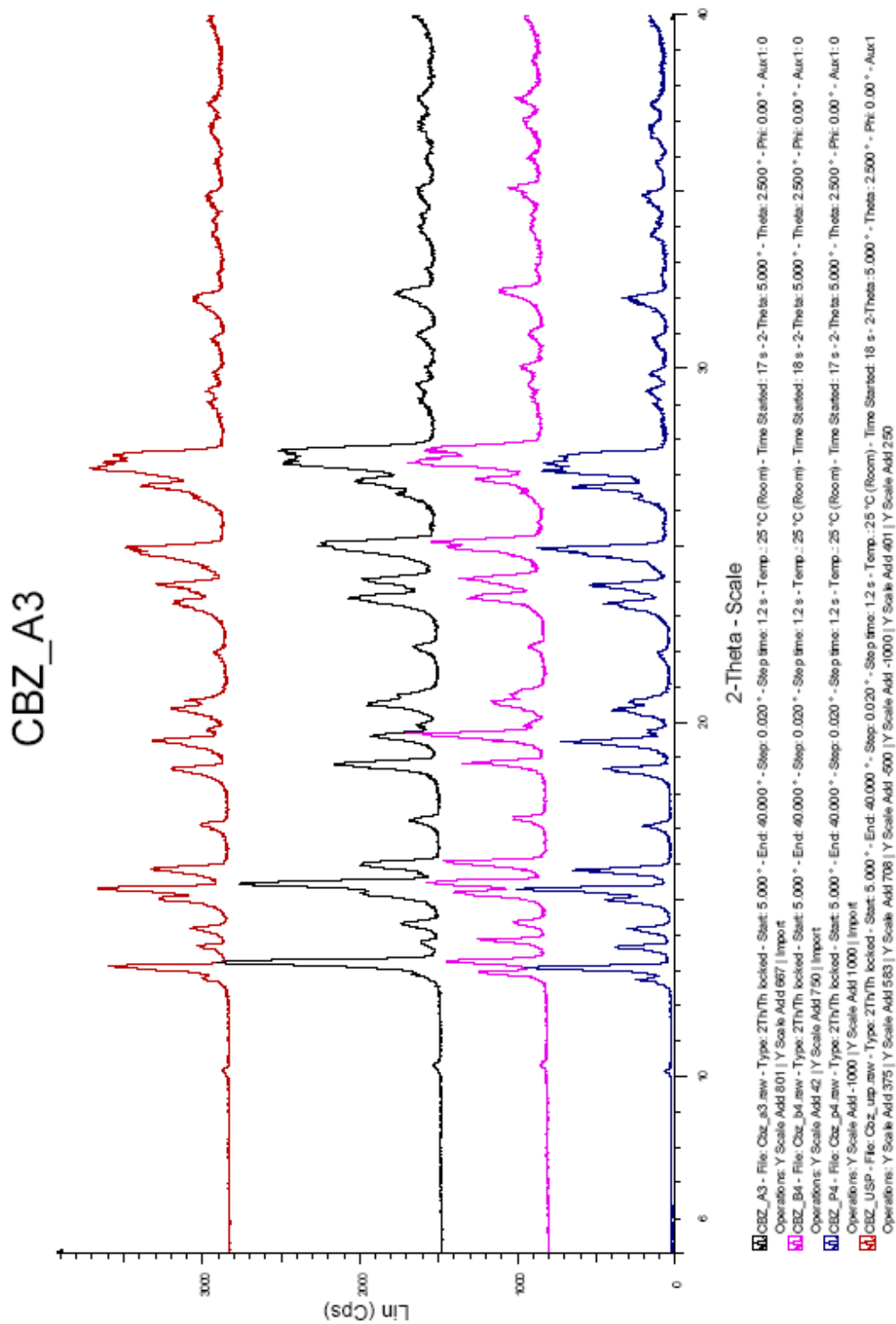


Figure 6.11 X-ray diffractograms of CBZ USP, CBZ A, B and P samples

The absence of characteristic peaks of form I and II in the range between 5 and 10° of 2θ excluded the possibility of having these two forms present in the commercial samples. Patterns of form IV reported by Griezak and Rustichelli (Grzesiak et al., 2003, Rustichelli et al., 2000) were not detected, which lead to the conclusion that there is no mixture of polymorphs present in the commercial samples or at least not in the detectable quantities. However, the relative height (intensity) of some peaks (e.g. peaks around 13-17° of 2θ) varied between different samples. This discrepancy may be attributed to the differences in crystal sizes and habits. Differences in the peak intensity may also be caused by the crystal lattice disruption formed during the manufacture of CBZ samples, especially in the case when milling or grinding step was performed.

The diffractograms of three consecutive batches of each of commercial samples A, B and P showed good batch to batch repeatability (appendix 9.7-9.9), thus all samples have shown the constant quality of raw materials.

6.1.8. Thermal analysis

6.1.8.1. Differential scanning calorimetry (DSC)

DSC was used to characterize the thermal behavior of carbamazepine. When CBZ is heated at standard heating rate of 10°C/min, it exhibits multiple thermal events: the melting endotherm of form III is accompanied by a concurrent exotherm due to recrystallisation to form I and subsequent melting of this newly formed polymorph. The enthalpy calculation of the melting endotherm for species that undergo recrystallisation during heating is difficult since the concurrent endothermic melt and exothermic recrystallisation events cannot be separated. One method to avoid this problem is to use faster heating rates which will lead to inhibition of recrystallization of the lower melting point. This may be done because many transitions being kinetic events are a function of both time and temperature. This is why in this study heating rates of 10 and 40°C/min were used for characterization of CBZ.

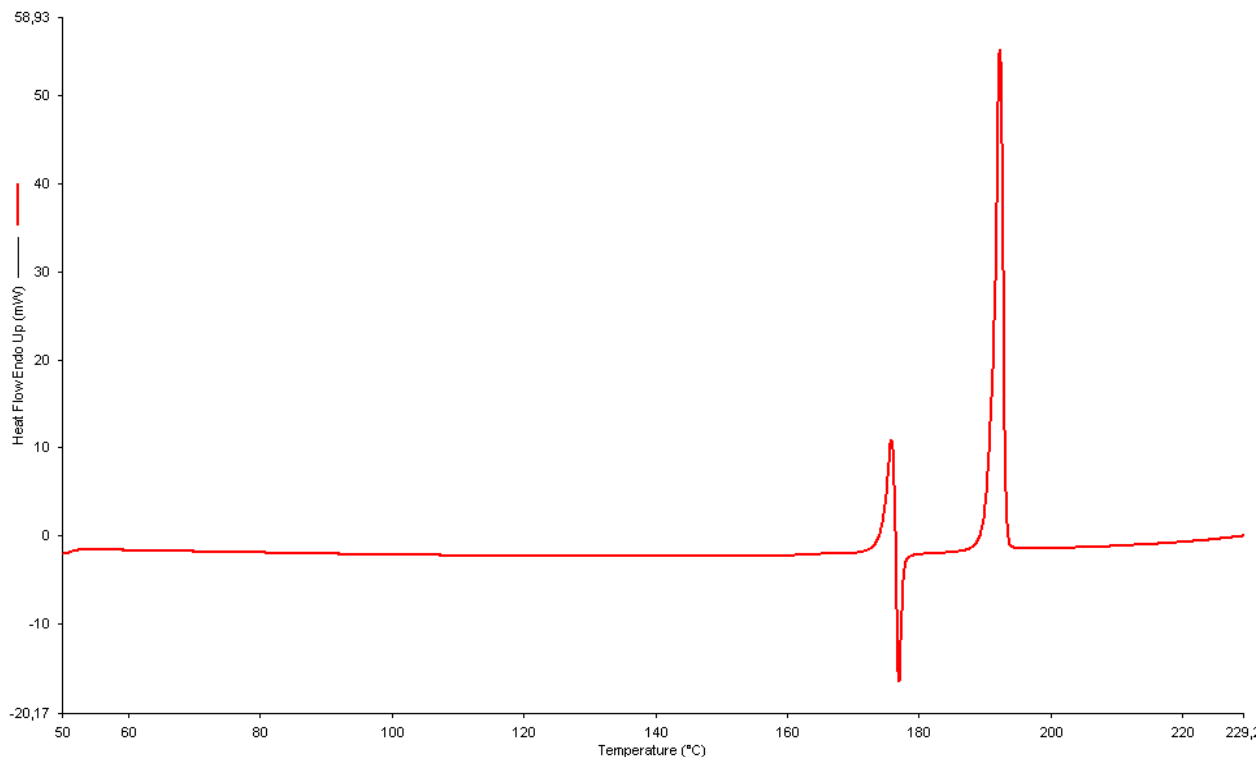


Figure 6.12 DSC thermogram of CBZ USP standard at heating rate 10°C/min

The DSC thermogram of CBZ USP obtained at 10°C/min showed characteristic behavior of CBZ form III: melting of form III at 176.6°C, followed by exothermic crystallization of form I (solid - solid transformation of form III to form I) and then a sharp melting endotherm of form I at 191.9°C with enthalpy of $\Delta H=107.3\text{J/g.}$, see figure 6.12. These results agreed with literature data (Grzesiak et al., 2003, Krahn et al., 1987, Rustichelli et al., 2000).

Analyzing three available consecutive batches from one source of each commercial sample, it was found that they were not showing any differences in the thermal behavior, thus no batch to batch variation was found.

Although all analyzed samples were shown to exhibit the same polymorphic form, differences in the thermal behavior and deviation from the CBZ USP standard were observed among them. CBZ A and CBZ B exhibited melting endotherms similar as CBZ USP with transition peaks at 178.8°C and 176.3°C respectively, the melting of form I at 194.9°C and 192.9°C respectively and the melting enthalpies $\Delta H=106.4\text{J/g}$ and $\Delta H=107.3\text{J/g}$ respectively. These results confirmed that samples A and B are

polymorphic form III of CBZ. However, the sample CBZ P exhibited thermal characteristic atypical of CBZ USP standard (see table 6.8 *). In the DSC thermograms of all CBZ P samples an additional endothermic peak can be seen at 164.6°C with enthalpy of $\Delta H=11.3\text{J/g}$. This was followed by a melting/recrystallisation event at 184.6°C, and subsequently by the melting endotherm of form I at 192.9°C with an enthalpy of $\Delta H=109.0\text{J/g}$, see table 6.8 and figure 6.13.

Table 6.8 Transition temperatures, melting enthalpy of CBZ USP, A, B and P at 10°C/min, *atypical event

Sample (n=3)	Solid-solid transformation Form III → Form I ± SD(°C)	Melting point of Form I ± SD (°C)	Enthalpy ± SD (J/g)
CBZ USP	176.57 ± 0.12	191.88 ± 0.23	107.32 ± 1.13
CBZ A	178.16 ± 1.37	194.98 ± 1.46	106.47 ± 2.52
CBZ B	176.37 ± 0.21	192.95 ± 0.36	107.32 ± 2.13
CBZ P	184.63 ± 0.23*	192.98 ± 0.30	109.01 ± 2.16

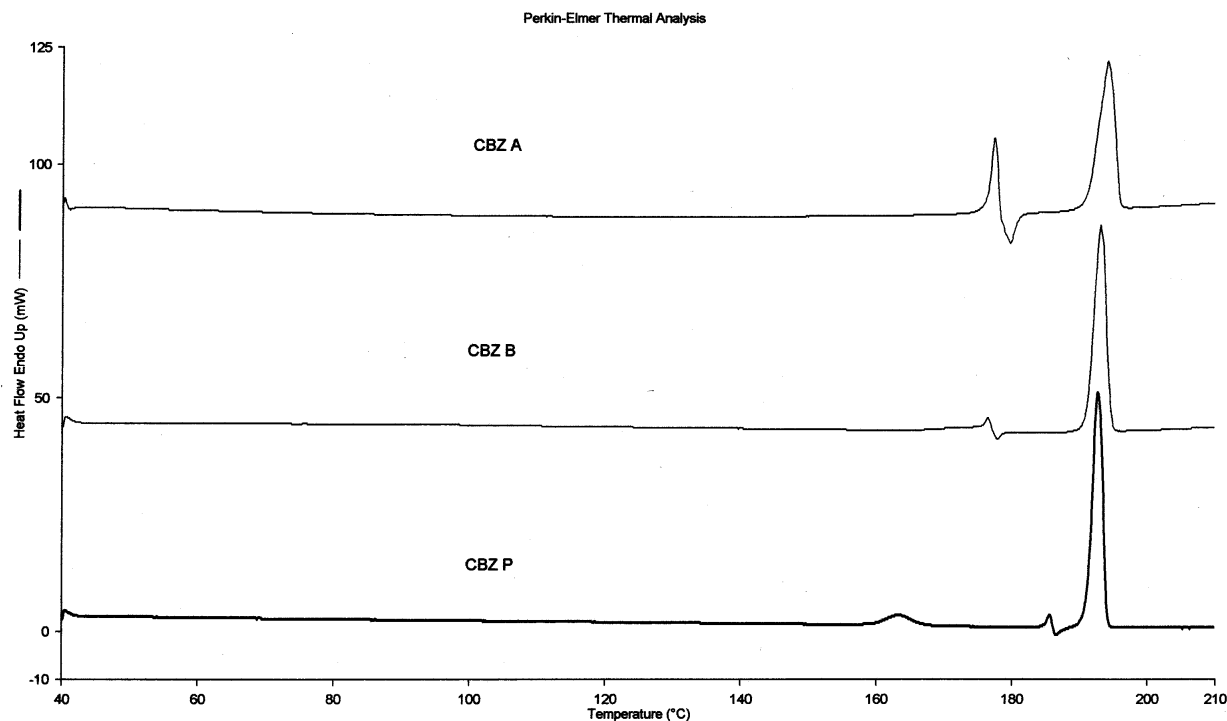


Figure 6.13 DSC thermograms of CBZ A, B and P at heating rate of 10°C/min

The enthalpy of solid-solid transformation (form III to form I) was difficult to calculate because there is no clear change-over from endothermic reaction of melting of form III to exothermic reaction of recrystallisation of form I. In other words, it was difficult to distinguish where the first reaction stops and the second one starts. Analyzing the thermograms of examined samples it could be seen that solid-solid transition varied among CBZ A, B and P. The enthalpy of fusion of form III was approximately calculated and presented in the following table 6.9.

Table 6.9 Enthalpy of melting of CBZ USP, A, B and P at 10°C/min

Sample (n=3)	Enthalpy± SD (J/g)
CBZ USP	12.33 ± 1.32
CBZ A	43.27 ± 9.40
CBZ B	5.12 ± 0.38
CBZ P	6.23 ± 4.25

Previously it was mentioned that transitions e.g. melting or recrystallisation represent kinetic events and they are a function of both time and temperature. When a compound is heated at a higher heating rate, all transitions will be shifted to a higher temperature because there is less time for the transition to take place. To study the effect of heating rate, DSC measurements were conducted additionally at 40°C/min (Rustichelli et al., 2000).

Difference in the thermal behavior was observed with the increase of heating rate which resulted in the partial inhibition of recrystallisation of the lower melting point polymorph (form III). The enthalpy of endothermic transition of melting of form I decreased, while the enthalpy of melting of form III increased. The behavior of CBZ USP standard under heating rate of 40°C/min is presented in following figure 6.14. The melting of form III happened at 177.8°C, with higher value for enthalpy of fusion of 22.1J/g than in the case of heating rate of 10°C/min, followed by exothermic crystallization of form I and then a sharp melting endotherm of form I at 194.9°C with enthalpy of fusion $\Delta H=91.3\text{J/g}$, which was lower than the corresponding value obtained with heating rate of 10°C/min.

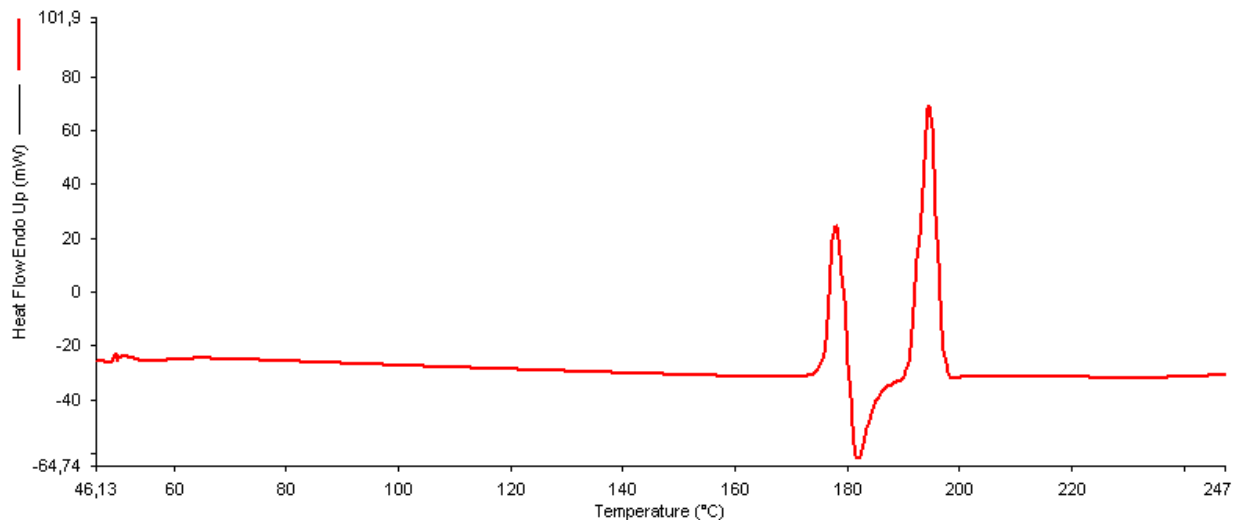


Figure 6.14 DSC thermogram of CBZ USP standard at heating rate 40°C/min

The thermograms of samples CBZ A, B and P showed some differences as well. The melting of form III and form I were, as expected, shifted to higher temperatures. CBZ A samples exhibited the highest enthalpy for III to I transition and the lowest enthalpy of fusion of form I. The enthalpy of III to I transition for CBZ B increased, but enthalpy of melting of form I was almost the same as with the heating rate of 10°C/min. Thus, changing of heating rate had no influence on melting of form I in case of CBZ B.

The additional peak observed in the thermograms of CBZ P at heating rate of 10°C/min, was shifted from 164.4 at the 177.1°C and had the higher enthalpy (13.9J/g). The melting event was shifted to 187.6°C and had lowest enthalpy of fusion among all CBZ samples. The results of thermal behavior at 40°C/min are presented in table 6.10, and figure 6.15.

Table 6.10 Transition temperatures, melting enthalpy of CBZ USP, A, B and P at 40°C/min, *atyp.event

Sample (n=3)	Solid-solid transformation Form III → Form I ± SD(°C)	Melting point of Form I ± SD (°C)	Enthalpy of fusion Form I ± SD (J/g)
CBZ USP	177.75 ± 0.35	194.95 ± 0.19	91.26 ± 2.35
CBZ A	179.62 ± 0.38	195.31 ± 0.18	68.34 ± 2.94
CBZ B	179.23 ± 0.14	195.59 ± 0.16	110.83 ± 2.48
CBZ P	187.60 ± 0.49*	195.64 ± 0.37	97.59 ± 8.42

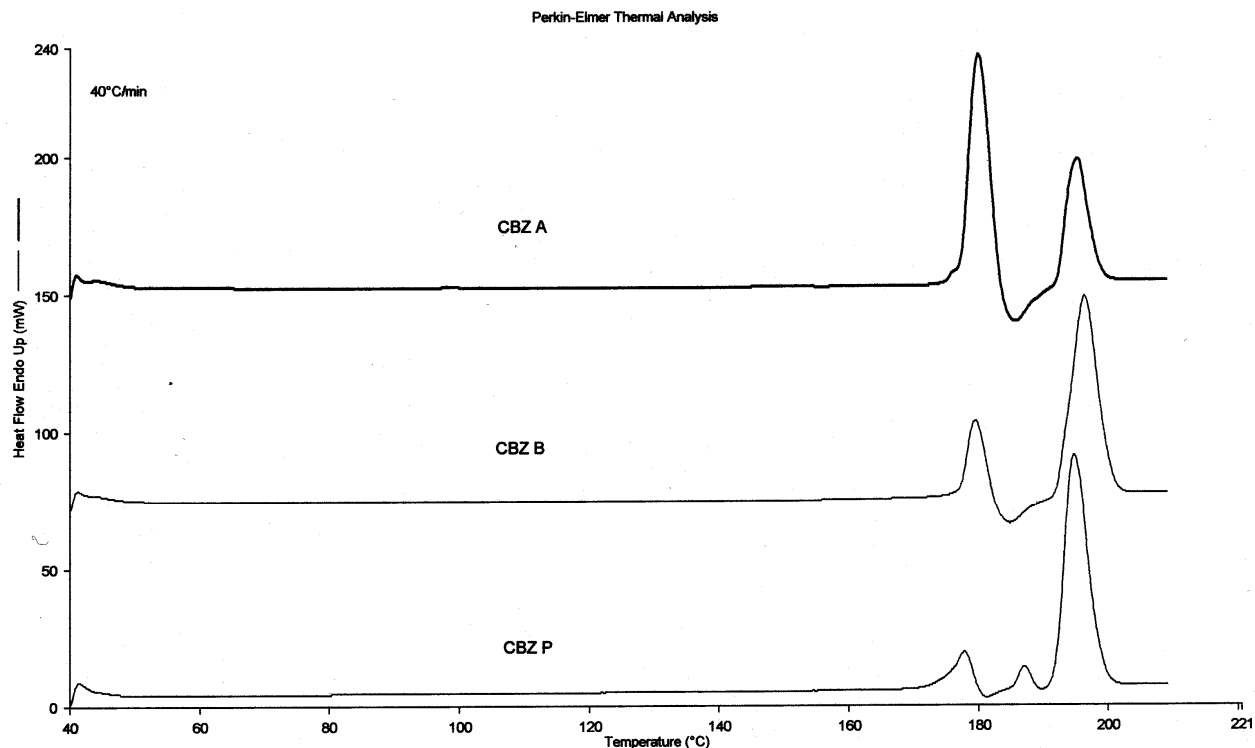


Figure 6.15 DSC thermograms of CBZ A, B and P at heating rate of 40°C/min

Enthalpies of melting of form III at heating rate 40°C/min were calculated and the results are presented in table 6.11. Comparing the enthalpies obtained at the two applied heating rates, it can be seen that there was an increase of enthalpy with increase in heating rate. Additionally, the variations in obtained values among samples were found to be significant. For example enthalpy of fusion of form III at 40°C/min for CBZ USP was double than at lower heating rate; for CBZ A was increased almost three times and obtained value corresponded to enthalpy of form I recorded at the 10°C/min; for CBZ B increased (from 5.12 J/g to 47.38 J/g), while in case of CBZ P there was only slight differences between two enthalpies.

Although the examined samples corresponded to polymorphic form III of CBZ, differences in thermal behavior were observed according to the DSC data. At both heating rates used in this study, the samples of CBZ A and to large extent the samples of CBZ B exhibited similar behavior as the CBZ USP standard. On the other hand, the behavior of the samples of CBZ P at both 10 and 40°C/min differed from that of the USP standard.

Table 6.11 Comparison of enthalpies of melting of form III obtained by different heating rates for CBZ USP, A, B and P at 10 and 40°C/min

Sample (n=3)	Enthalpy± SD (J/g) at 10°C/min	Enthalpy± SD (J/g) at 40°C/min
CBZ USP	12.33 ± 1.32	22.14 ± 2.72
CBZ A	43.27 ± 9.40	109.38 ± 3.30
CBZ B	5.12 ± 0.38	47.38 ± 2.41
CBZ P	6.23 ± 4.25	7.27 ± 2.49

To explain the atypical thermal events seen on the DSC thermograms of CBZ P the following mechanisms are considered.

One explanation for the additional endothermic peak in the case of all CBZ P samples is sublimation of CBZ which is an endothermic reaction that occurs around 150°C. But since all measurements were done with the same type of pan (open pan), it is not clear why it was not registered with the other samples. On the other hand, sublimation (which can be observed with the hot stage microscope) results in a loss of compound and it would be possible to record it by TGA (HSM and TGA studies were therefore conducted and results are discussed in sections 6.1.8.2 and 6.1.8.3 respectively).

The possibility of presence of small amount of form II can be considered as well because the form II exhibits the thermal reaction between 140 and 160°C as reported by Khran (Krahn et al., 1987). However, according to Griezak, Umeda and Kaneniwa (Grzesiak et al., 2003, Kaneniwa et al., 1984, Umeda et al., 1984) solid-solid transition in the case of monotropic pair of polymorphs is exothermal.

Other possibilities are to have a small solvent inclusion (entrapped solvent) in the crystal pores, which may play a role in the crystal stability or to have presence of amorphous material, created by grinding during the manufacture of the raw material. Amorphous CBZ would exhibit crystallization around 80°C (glass transition and than crystallization), and this could be detected by TGA (TGA tests were therefore conducted and the results are discussed in section 6.1.8.2).

6.1.8.2. Hot stage microscopy (HSM)

The DSC results of anhydrous forms were confirmed by the visual images obtained with HSM operated at the same heating rate as the one used for DSC. The examination by optical microscope revealed, in agreement with previous results from XRPD and PSA tests, the presence of prismatic particles of CBZ in all analyzed samples and the difference in particle size. The prisms appeared brightly colored under polarized light.

During the heating of CBZ USP at 10°C/min heating rate, the melting of the form III could be observed around 176°C followed by formation of the needle-like particles of form I which then melted around 192°C. Obtained data were in agreement with literature data (Rustichelli et al., 2000).

The anhydrous samples CBZ A exhibited analog behavior as CZB USP standard. With increase in the temperature, at 176-178°C melting of form III particles began, and around 179°C some needles started to spread out from the edges of the prisms. The transformation into needles was completed at 182°C. Subsequently, these crystals melted in the 189–192°C range, according to the endothermal event previously registered by DSC. A very similar situation was observed analyzing the sample CBZ B. During heating, the smallest particles disappeared, turning into needles at temperatures higher than 175°C. Finally, the fusion of the crystals occurred at 193–195°C. CBZ P samples on the other hand showed discrepancies from all the other samples. At temperature of 149°C there were slight changes in the intensity of the color of the samples. Starting from 160°C, the formation of needle-shaped crystals could be observed, followed by intense needle formation at 184-188°C and their melting between 192 and 194°C (see figures 6.16 and 6.17).

CBZ is known to undergo sublimation in the temperature range of 145-155°C which was noticed in all samples as formation of small crystals at the upper lid of THSM unit.

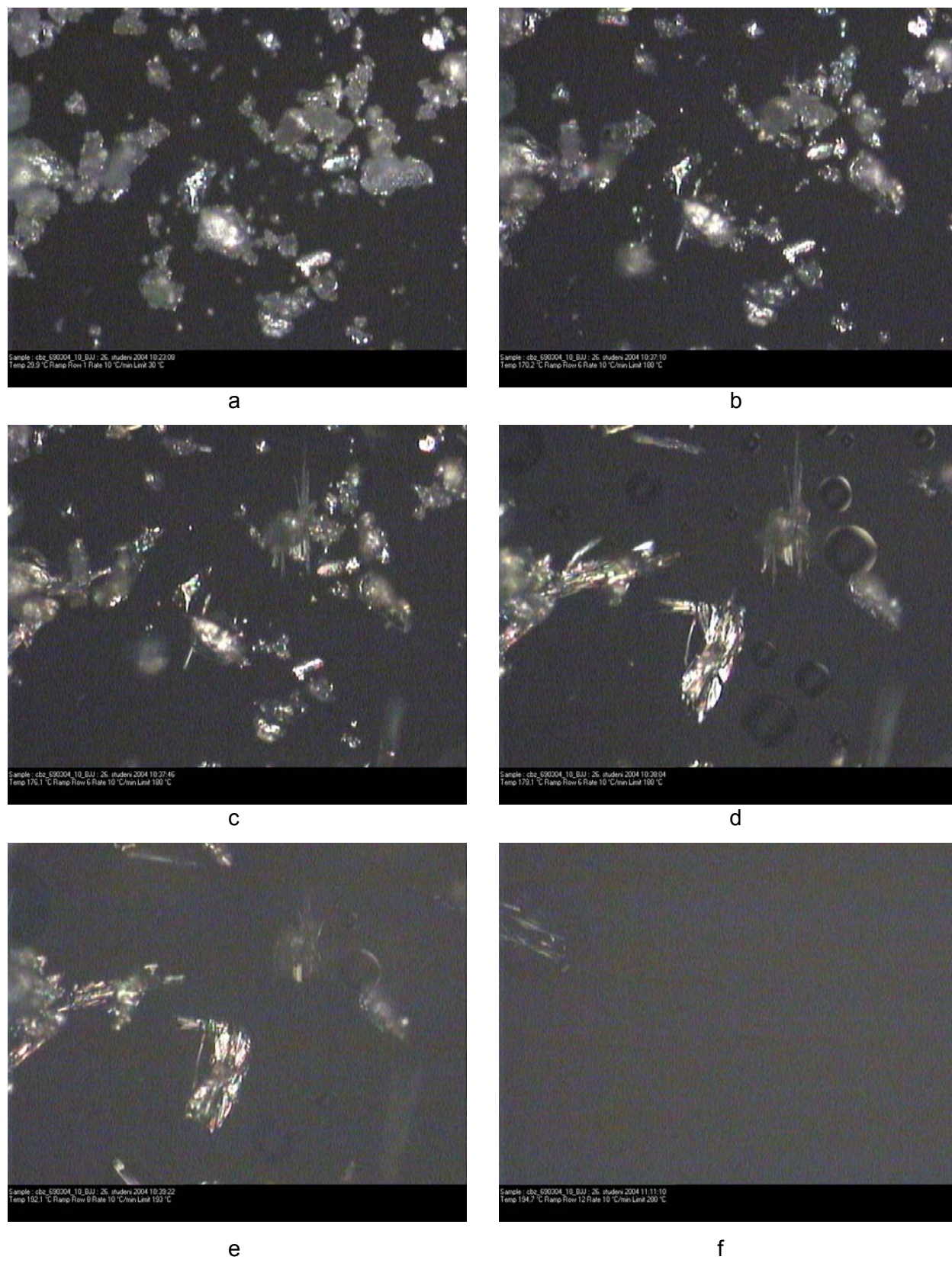


Figure 6.16 HSM of CBZ P sample: a)29.9°C; b) 170.2°C; c) 176.1°C ; d) 179.1°C e) 192.1°C f) 194.7°C

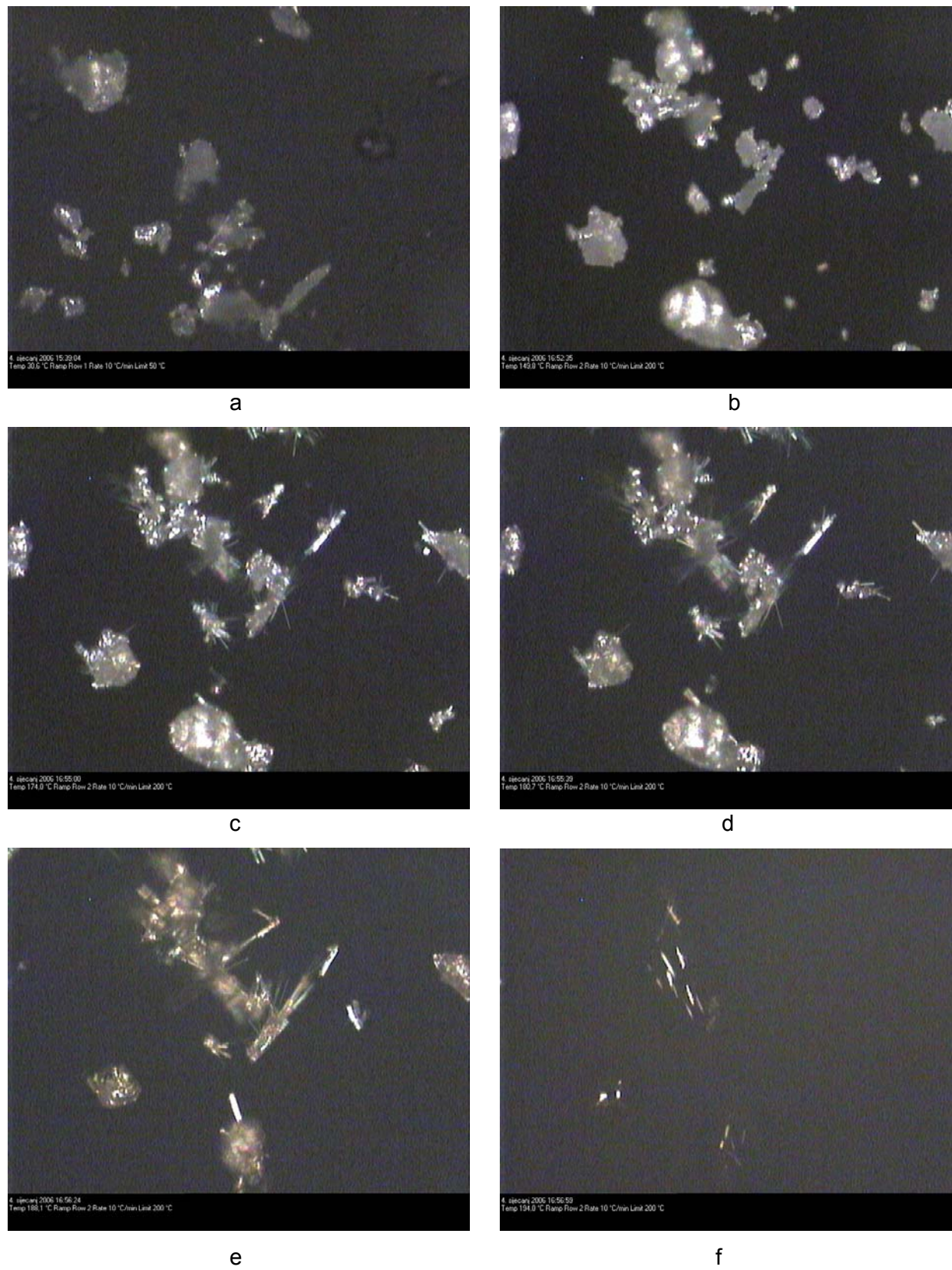


Figure 6.17 HSM of CBZ P sample: a)30.6°C; b) 149.8°C; c) 174.0°C ; d) 180.7°C e) 188.1°C f) 194.0°C

6.1.8.3. Thermogravimetric analysis (TGA)

Thermogravimetry is a powerful tool for determination of desolvation processes or decomposition. TGA in this study was used in combination with DSC measurements for better understanding of thermal behavior of the carbamazepine samples. TG analyses were done to check if any possible solvent inclusion or impurity is present in the anhydrous CBZ samples, and to determine a glass transition in case of presence of amorphous material. In other words, if the additional peak found in the CBZ P samples, was due to a solvent inclusion, or sublimation, the partial degradation should be expressed as loss of weight on the TGA profile at the exact temperature range of the endothermic reaction seen on the DSC thermogram.

All anhydrous samples were investigated by TGA and the results are presented in table 6.12. The loss in weight, representing all the changes in weight caused by evaporation of water or other volatile impurities, was registered by the instrument as Delta Y value and it was calculated by instrument's software. No sharp drop of TGA curve, characteristic for desolvation or decomposition, was recorded. In the case of all examined samples ΔY was in the range between 0.169 and 0.214%. In comparison to the TGA findings, the water content in the CBZ samples determined by the loss on drying tests was slightly lower, i.e. between 0.1 until 0.14%. This small variation in the values can be explained as volatile impurities. The results of TGA for CBZ P3 are presented figure 6.18.

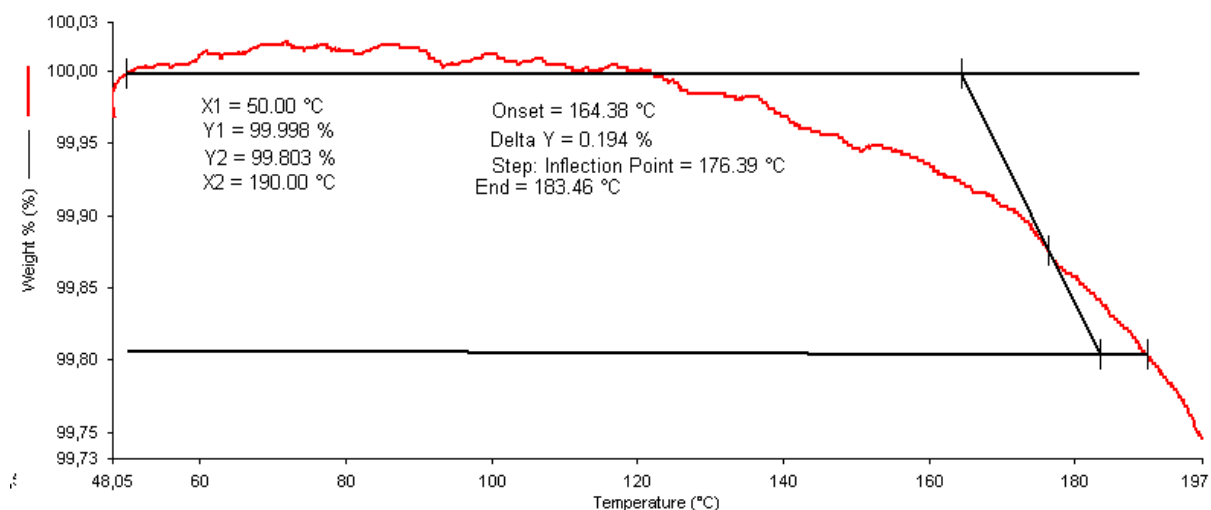


Figure 6.18 TGA results of CBZ P sample (with calculations)

Table 6.12 TGA results of CBZ A, B and P

Sample (n=3)	Onset temperature (°C)	Inflection point temperature (°C)	End temperature (°C)	Weight difference ΔY (%)
CBZ A	171.37 ± 10.57	187.22 ± 1.64	189.21 ± 0.41	0.214 ± 0.177
CBZ B	173.96 ± 2.86	184.60 ± 0.42	187.97 ± 0.48	0.169 ± 0.081
CBZ P	168.14 ± 9.39	180.22 ± 0.87	185.16 ± 1.98	0.197 ± 0.131

It can be concluded, that no substantial weight loss or glass transitions were evident from the TGA data. Therefore, the atypical DSC thermograms of CBZ P can be a result of partial melting of the CBZ crystals at lower temperature, i.e. around 160 °C. Stressed and aged CBZ crystals have been reported to exhibit endothermic event at lower temperatures, than the ones characteristic of form III (Krahn et al., 1989). Higher density of crystal defects and mechanical stress caused by grinding could have caused the atypical melting of CBZ P. The formation of needle-like crystals (corresponding to a metastable polymorph form of CBZ) was observed in the melt by HSM but no exothermic effect was seen by DSC (this can be due to the dispersion of the small crystals in the melt and to the high rate of heating). As the temperature rises the newly formed crystals melt together with the remaining form III crystals pushing the melting event to higher temperature than that of the melting of pure form III. The form I then crystallizes from the melt and finally melts at the temperature characteristic for form I. And because the observed phenomena take place at elevated temperature, they could not be detected by XRPD which is conducted at room temperature. However, the performance of the commercial product under normal room conditions (i.e. its solubility and dissolution behavior) will be affected by variability in the primary material caused by the variations of the processes used for its manufacture.

6.1.9. Solubility

The solubility of metastable form is very difficult to determine in anhydrate/hydrate systems, since transformation happens quickly in most of the cases. It has been reported by Brittain (Brittain et al., 1999) that the unexpected high metastable solubility could be caused by greater density of crystal defects rather than by polymorphism.

However according to Qu et al (Qu et al., 2006) the effect of crystal defects on solubility seems to be small since the concentration of dissolved anhydrous crystals of CBZ in their case reaches a certain value and then remains constant at that value for quite a long time (in their case around 100min). Solubility measurement of metastable form can be estimated from the maximum in the dissolution rate curve. The accuracy of the determination depends on the rate of transformation versus the rate of dissolution (Jozwiakowski, 2000).

Solubility test according to Murphy (Murphy et al., 2002) was carried out by shake agitation method until the equilibrium concentration was achieved. Since carbamazepine anhydrous is known to undergo a phase transformation in aqueous solutions, after 72 h, only CBZ dihydrate form was present in solution. The solubility curve of anhydrous forms showed the typical shape for solubility measurement of metastable form, and it is presented on figure 6.19.

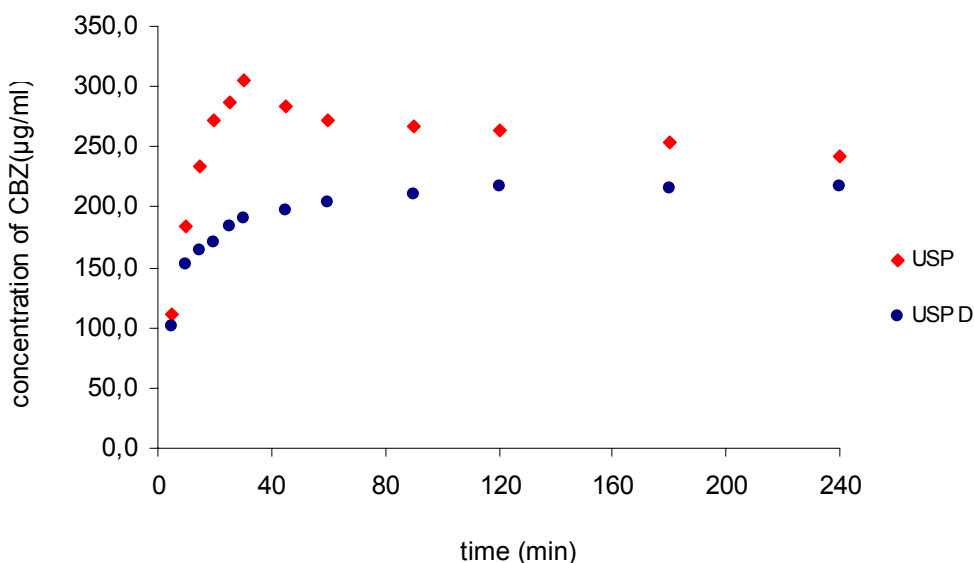


Figure 6.19 The solubility curves of CBZ USP anhydrous and dihydrate forms

During solubility measurement of anhydrous CBZ, samples were withdrawn in predefined time intervals (as referred in 5.2.1.10) to determine if there is discrepancy among the commercial CBZ samples in the kinetics of solubility in water, see figure 6.20. The solubility values measured after 72h are presented in the table 6.13. It can be

seen from the figure 6.20 that the maximum dissolved concentration was achieved at different time points for different CBZ samples. The maximum solubilities are also presented in the table 6.13.

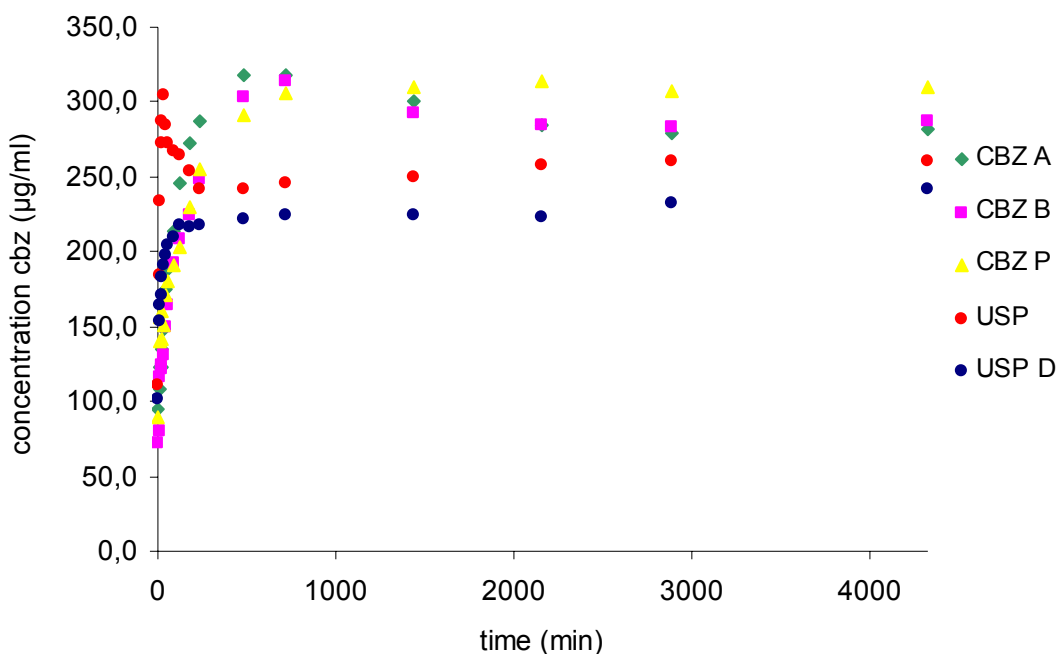


Figure 6.20 Solubility charts for CBZ samples A, B, P and USP

Table 6.13 Solubility parameters after 72h and estimated values for maximum CBZ dissolved

Sample (*n=3; n=9)	Solubility \pm SD ($\mu\text{g/ml}$) after 72h	Max. measured solubility \pm SD ($\mu\text{g/ml}$)
CBZ USP*	262.8 \pm 2.1	304.0 \pm 7.6 (after 30min)
CBZ USP D*	237.3 \pm 2.2	
CBZ A	282.0 \pm 4.1	318.4 \pm 7.8 (after 12h)
CBZ B	310.5 \pm 3.9	314.0 \pm 3.3 (after 36h)
CBZ P	286.4 \pm 11.2	314.2 \pm 9.6 (after 12h)

The shortest time for reaching the maximum quantity of dissolved anhydrous carbamazepine was found to be 30 minutes for CBZ USP standard, caused by very small particle size (see figure 6.3). Samples CBZ A and CBZ P reached the maximum

quantity dissolved after 12h, while in the CBZ B samples which showed the highest amount of dissolved material, the maximum dissolved was reached only after 36h.

Calculations of solubility of anhydrous CBZ were made as well using the results obtained by DIDR tests, whereby only the initial part of the curve was used for the calculations. The estimated solubilities had higher values than the measured ones, because during the equilibrium method after 72 hours CBZ was almost completely converted to dihydrate form which has lower solubility (see 6.1.10).

ANOVA tests were performed to evaluate batch to batch variation (variation within the same sources of CBZ) and variation between the different samples. Results within one group of samples did not show significant batch to batch variation. However, comparing the solubility results between CBZ A, B, P and USP, differences were found. CBZ P samples exhibited the highest variation from CBZ USP, but that discrepancy was statistically significant (confidence interval $\alpha=0.05$, $p<0.1$).

6.1.10. Disc intrinsic dissolution

Because of the poor compactibility of anhydrous CBZ (Villafuerte-Robles, 1982), preliminary tests were conducted to determine the compression force needed for the preparation of reproducible compacts for the intrinsic dissolution measurements. For this purpose, compacts were prepared at different pressure levels from 4kN to 20kN. With force in the range from 4 to 6kN and from 18 to 20kN, the obtained compacts were too weak, with low crushing strength (less than 10N). Using compaction force in the range from 14 to 20kN resulted in compact lamination of the compact. Only compaction force in the range from 8 to 12kN was acceptable for producing compacts which despite of low hardness of 34 - 40N, were robust enough to be submitted to intrinsic dissolution test. After selection of the compaction pressure range, the porosity of obtained compact was measured by mercury porosimeter and then calculated as well (as referred in method 5.2.1.11.).

The ideal case for investigating intrinsic dissolution of some material is to start with 0% porosity compact (which is practically not achievable) and perfectly flat surface. In such

cases the influence of particle size and surface area on the intrinsic dissolution will be minimized.

The CBZ samples used in this study varied in their particle size, particle shape and bulk density. As it was impossible to obtain compacts with less than 12% porosity, the further investigations were carried out with constant porosity compacts ($12\pm 0.3\%$) by varying only the compaction force in the range between 8 and 12kN (for CBZ A samples the compaction force was 10kN, and for CBZ B and CBZ P samples the compaction force was 8kN).

The aim was also to compare commercial samples with the chemically pure standard of carbamazepine sample, CBZ USP however all efforts to compact CBZ USP were unsuccessful, because lamination occurred with all compaction forces in the range of 4 to 16kN. With lower force ($< 4\text{kN}$), the compacts were not robust enough to handle for the subsequent preparation for intrinsic dissolution. The effort to recompress the laminated compact (simulation of dry granulation or slugging method) also failed. This poor tablettability is due to very small particles size of the USP CBZ sample.

In the USP XXXI monograph for Carbamazepine 200mg immediate release tablet the recommended dissolution medium is 1% solution of sodium lauryl sulphate (SLS) (USP31, 2008). Rodriguez-Hornedo reported that surfactants (especially SLS) affect the solution mediated transformation of CBZ by increasing the anhydrous to dihydrate conversion (Rodriguez-Hornedo et al., 2004). The aim of this study was to investigate the intrinsic dissolution behavior of commercially available carbamazepine samples without influencing the anhydrous to dihydrate conversion. Therefore distilled water was chosen as the dissolution medium.

And because the intrinsic dissolution rate of carbamazepine is independent of pH of the medium as reported by Yu (Yu et al., 2004), water alone is the most appropriate medium for the IDR tests.

The slope of the intrinsic dissolution curve is usually linear, but that it is not the case of carbamazepine because anhydrous CBZ was shown to undergo a phase transition into the dihydrate form during the test (Kobayashi et al., 2000, Murphy et al., 2002, Ono et

al., 2002). This phase transition is indicated by the change of slope in the profile, thus the intrinsic dissolution profile of CBZ can be split in two distinct parts:

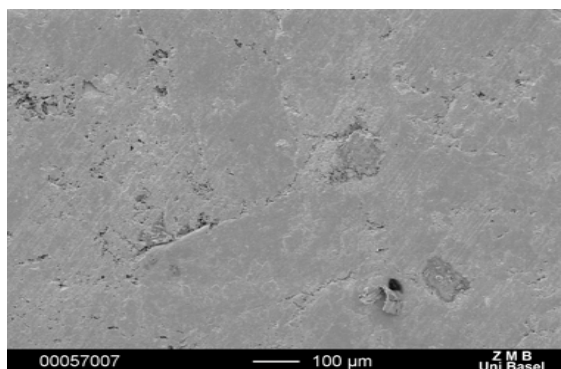
- the initial segment which describes dissolution of anhydrous form and
- the final segment which represents the dissolution of dihydrate form.

This means that during the intrinsic dissolution, the crystallization of CBZ dihydrate occurs at the surface of tablets resulting in a decrease of intrinsic dissolution rate of CBZ anhydrous.

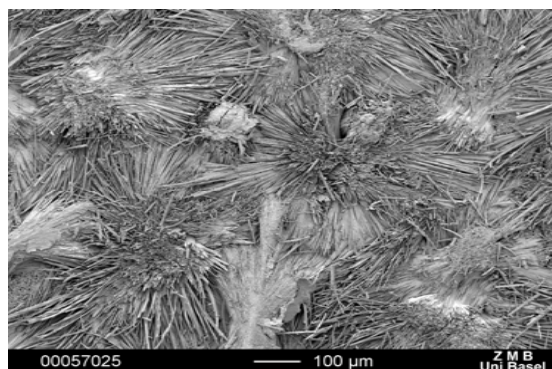
The disc intrinsic dissolution profiles of the CBZ anhydrous materials showed the above mentioned typical behavior. Nevertheless some “jumps” on the dissolution curve were observed following the transition period. That could be explained by the fact that in some regions of compacts the transition was not completed, and the “jumps” were probably created when some newly exposed regions of anhydrous CBZ began to dissolve.

By performing disc intrinsic dissolution test, it should be possible to exclude the influence of particle size on the dissolution. However, preliminary tests showed that tablettability of the CBZ samples (and thus appearance of the surface of the compacts) were affected by the difference in particle size and morphology. In order to minimize the problem during compaction, the CBZ A, B and P samples were sieved into fraction with the same particle sizes. The fraction of particle size from 250 to 355 μm was selected for the further experiments, because it was most representative of all samples.

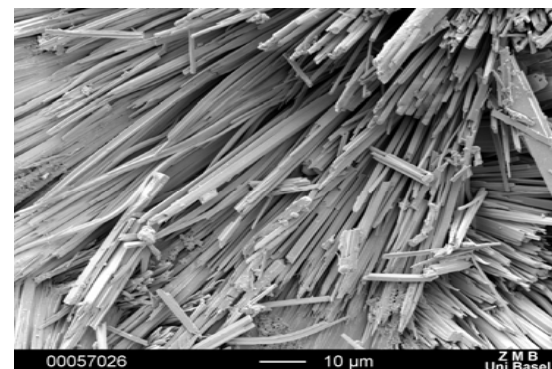
The surfaces of CBZ compacts were analyzed before and after intrinsic dissolution testing by SEM and are presented in figures 6.21. It can be observed that the compacts prepared from CBZ A had flatter surfaces, than those of samples B and P, where the latter were rougher, with gaps which could eventually increase the starting area of compacts. Some discrepancies were found also by analyzing the pictures of the compacts after the intrinsic dissolution. These variations resulted from the conversion to dihydrate form which varied among samples i.e. the change in the dissolution slope occurred at different time periods. For some samples (i.e. CBZ P) the transition was not fully completed even after 120 min.



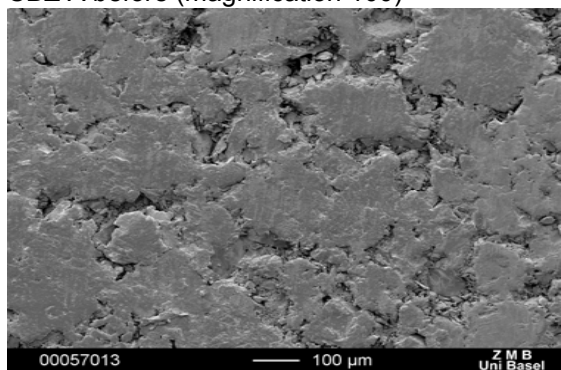
CBZ A before (magnification 100)



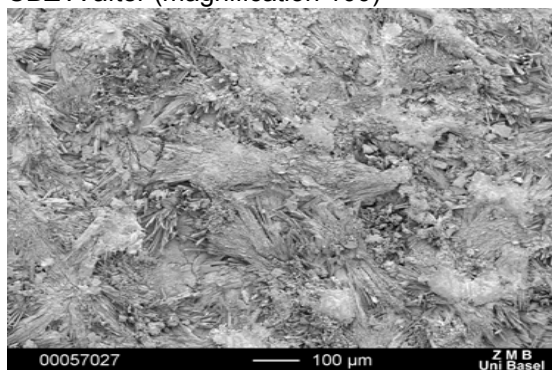
CBZ A after (magnification 100)



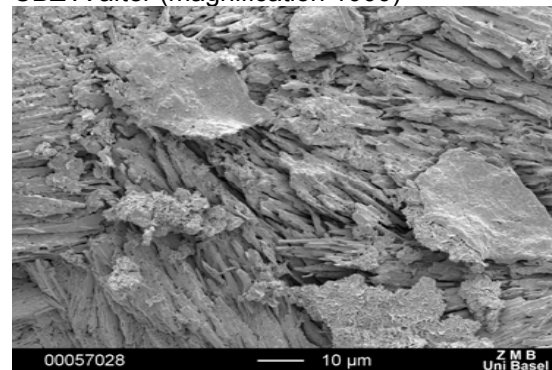
CBZ A after (magnification 1000)



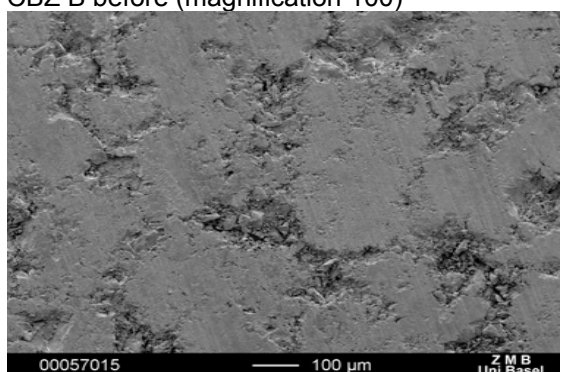
CBZ B before (magnification 100)



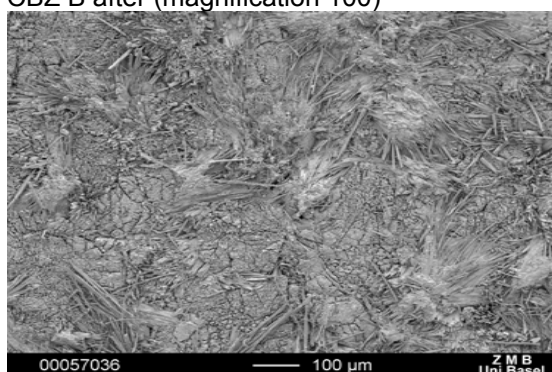
CBZ B after (magnification 100)



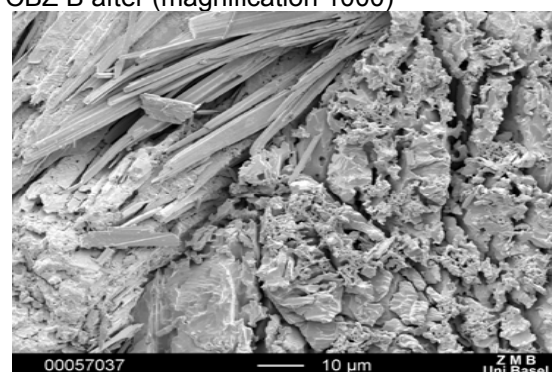
CBZ B after (magnification 1000)



CBZ P before (magnification 100)



CBZ P after (magnification 100)



CBZ P after (magnification 1000)

Figure 6.21 Surface of compacts before and after disc intrinsic dissolution

Therefore, based on the observation of the SEM pictures, the conversion of anhydrous to dihydrate form of CBZ A was completed after 120 minutes of dissolution (as confirmed by needle-like formations which were covering the surface of the compacts). In the case of CBZ P, after 120 minutes of dissolution, besides the needle-like formations, some prismatic particles were present as well.

The dissolution profiles of each group of CBZ anhydrous samples during the initial 20 minutes and during 120 minutes are shown in the figures 6.22 and 6.23 respectively. The time interval of 20 minutes was selected because the transition from anhydrous to dihydrate CBZ normally would take place within the first 20 minutes of intrinsic dissolution. Therefore, it is important to determine the variations in the intrinsic dissolution behavior of the commercial CBZ samples during that particular time interval.

One of the major difficulties in formulating CBZ immediate release tablets was that the formulations did not meet the narrow requirements for CBZ recommended by USP, where the amount of carbamazepine dissolved from the dosage unit must conform with the Acceptance Table 2 (see section 6.5) (USP31, 2008). Moreover, the amount of dissolved CBZ was often outside the levels L_1 and L_2 given in the Acceptance Table 2, and this was accompanied by high variation between six analyzed tablets.

The intrinsic dissolution results of anhydrous CBZ B and P samples showed higher variations within the tablets of one sample than those of CBZ A (compare the error bars in the figures 6.22.-24). In other words the erratic dissolution found in the CBZ pure compacts confirmed that the variations in dissolution results of formulated CBZ tablets are most likely caused by the properties of CBZ raw material itself.

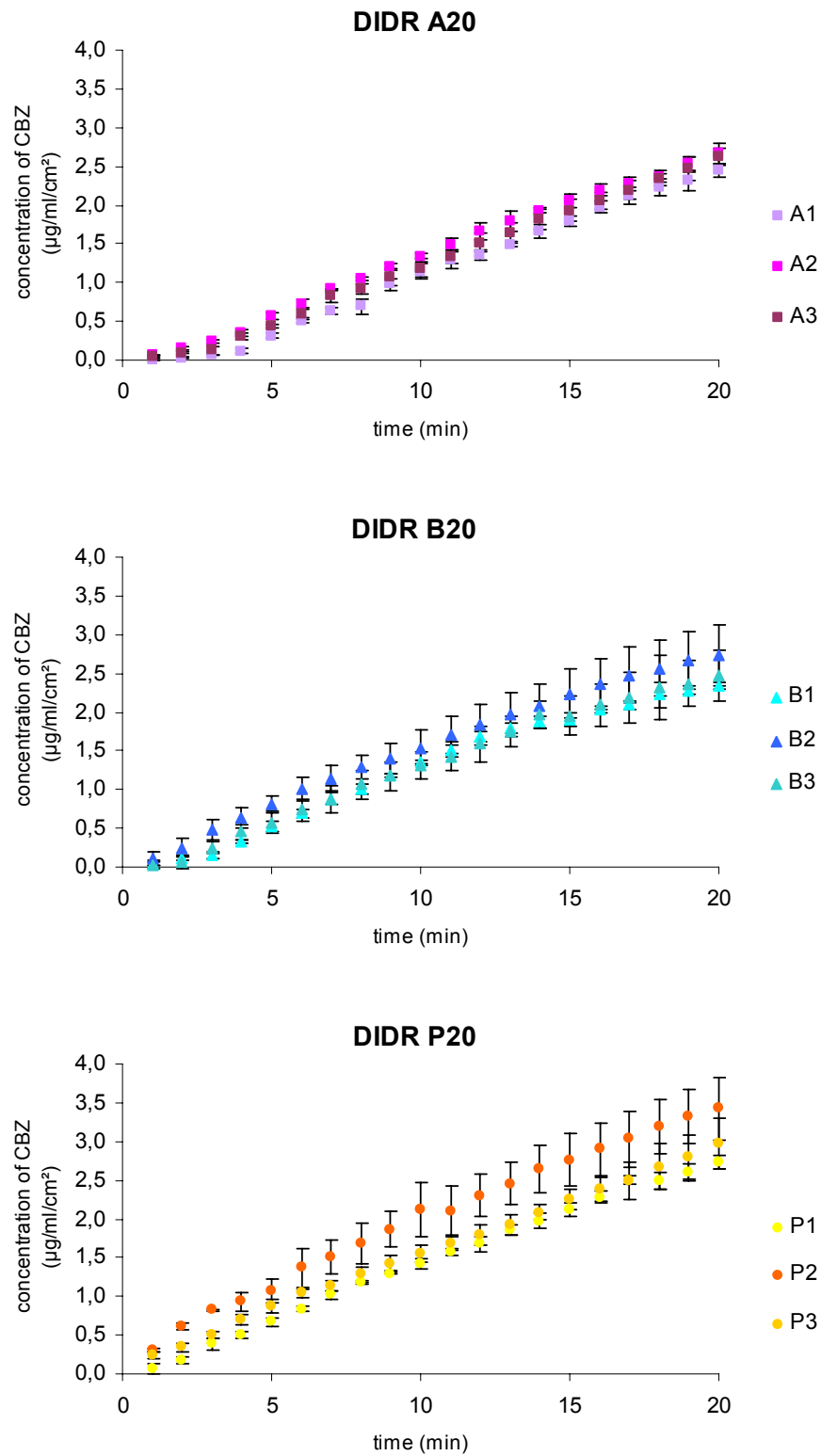


Figure 6.22 Intrinsic dissolution profiles of CBZ A, B and P for first 20 minutes

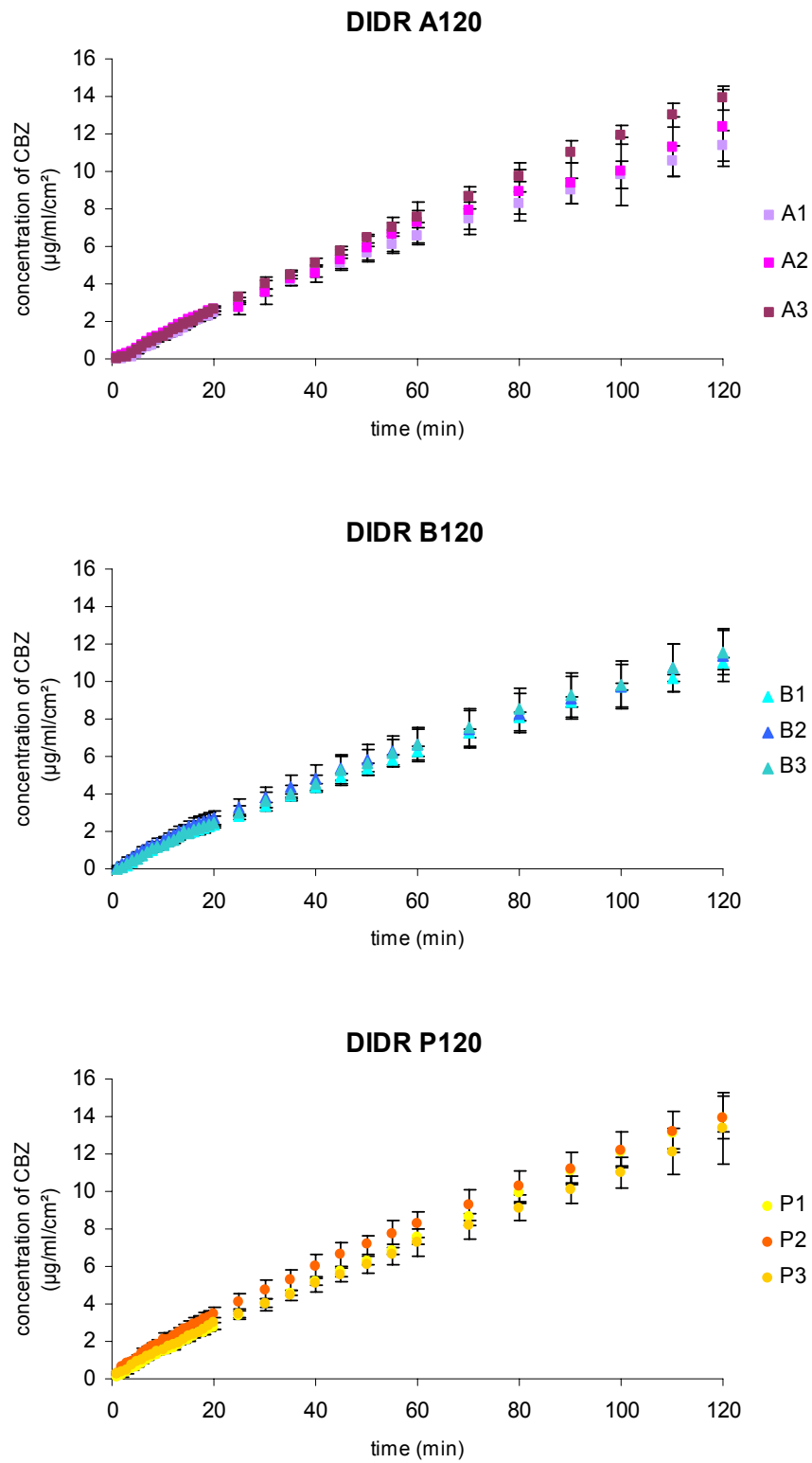


Figure 6.23 Intrinsic dissolution profiles of CBZ A, B and P for 120 minutes

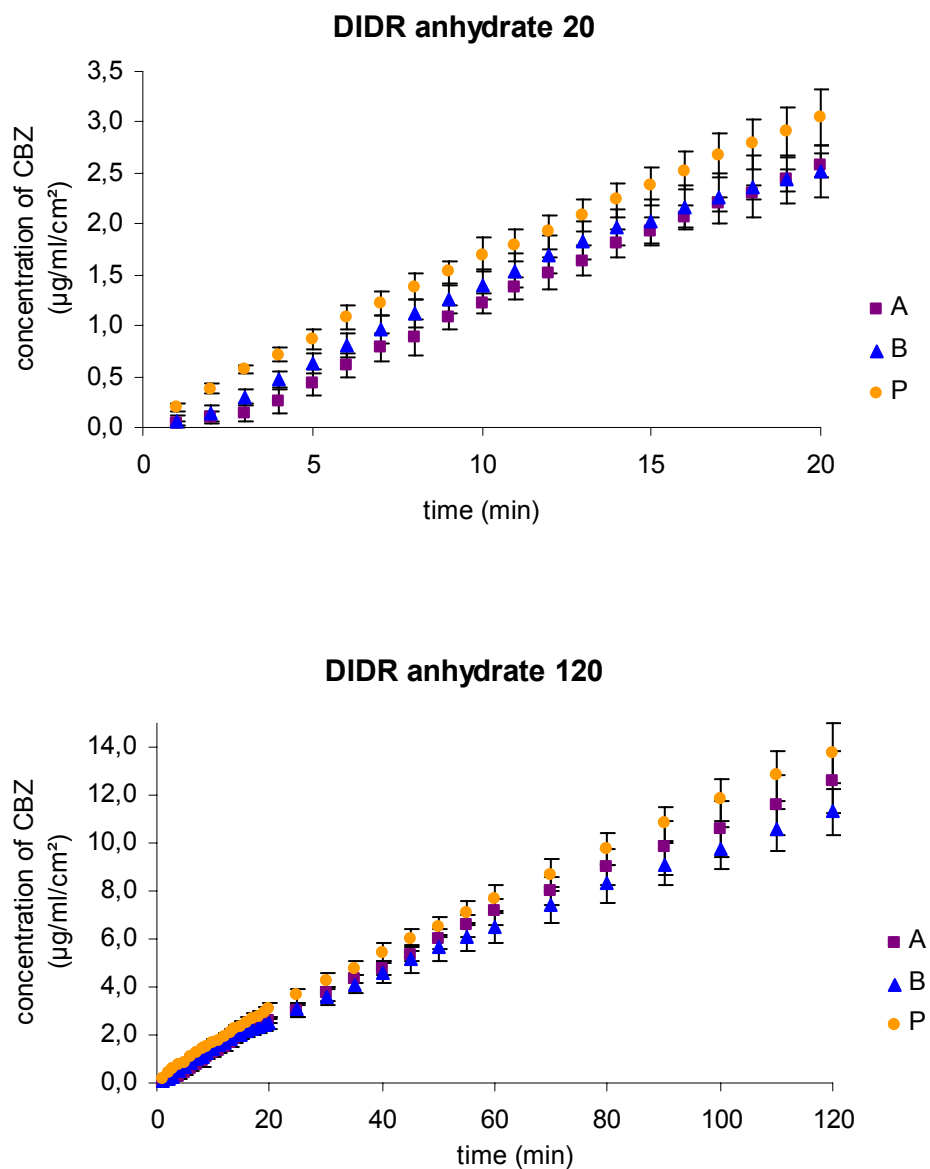


Figure 6.24 Intrinsic dissolution profiles of CBZ A, B and P with standard deviations.

One-way ANOVA was used to test if the differences in the intrinsic dissolution profiles and/or in the conversion kinetics within each CBZ of same producers were statistically significant. According to the results obtained, no significant difference was found in the intrinsic dissolution behavior among the batches of samples A and batches of samples B, while in the CBZ P batches, the difference was statistically significant (for confidence interval $\alpha=0.05$, $p<0.1$).

One-way ANOVA test was also used for the comparison between the CBZ A, CBZ B and CBZ P samples. It was shown that the intrinsic dissolution behavior for the initial 20 minutes was different, but the differences were not statistically significant when the intrinsic dissolution profiles of CBZ A, B and P were compared over the period of 120 minutes. This leads to the conclusion that most probably the main differences between CBZ A, B and P are expressed in the initial part of dissolution, i.e. where anhydrous-dihydrate conversion occurs.

The variations can be attributed to various manufacturing processes most likely resulting from different solvent systems used and different drying and/or grinding regimes applied in the final stage of the manufacture (see table 6.4) all of which have influenced the final shape and size of the CBZ crystals. Moreover, crystal defects and ruptures could also lead to differences in the conversion kinetics of CBZ anhydrous to CBZ dihydrate.

It was mentioned previously that intrinsic dissolution rate can become complicated when one or more of the studied polymorphs interconvert to another polymorph during the time of the measurement. If one of the polymorphic forms is hydrate, the dissolution rate of the anhydrous phase normally exceeds that of any corresponding hydrate phase.

This phenomenon is observed for carbamazepine which undergoes phase transformation during dissolution and intrinsic dissolution. Unlike the linear intrinsic dissolution profiles of many substances, CBZ exhibited inflection in the curve, resulting in two distinct slopes: the initial slope, which describes dissolution of anhydrous phase and the final slope, which represents the dissolution of dihydrate phase. The inflection point between these two segments of the intrinsic dissolution curve is defined as the transition point of the two phases.

Segmentation of the DIDR curves of the different samples into initial and final segments was obtained by splitting the data in such a way that the linear regression lines for each segment resulted in the best correlation coefficient. Systat software (Systat Software Inc, USA) was used to obtain the best fit linear segments of each DIDR plot. The slopes of each segment and the intercept of the final segment for each sample were obtained from statistical analysis using nonlinear model with Systat software. The segmented graphs of the different batches of each sample and their average are presented respectively in the figures 6.25-6.27.

In the figure 6.28 graphs showing the transition points of all CBZ samples are summarized and the difference in the dihydrate part of the slope are observed.

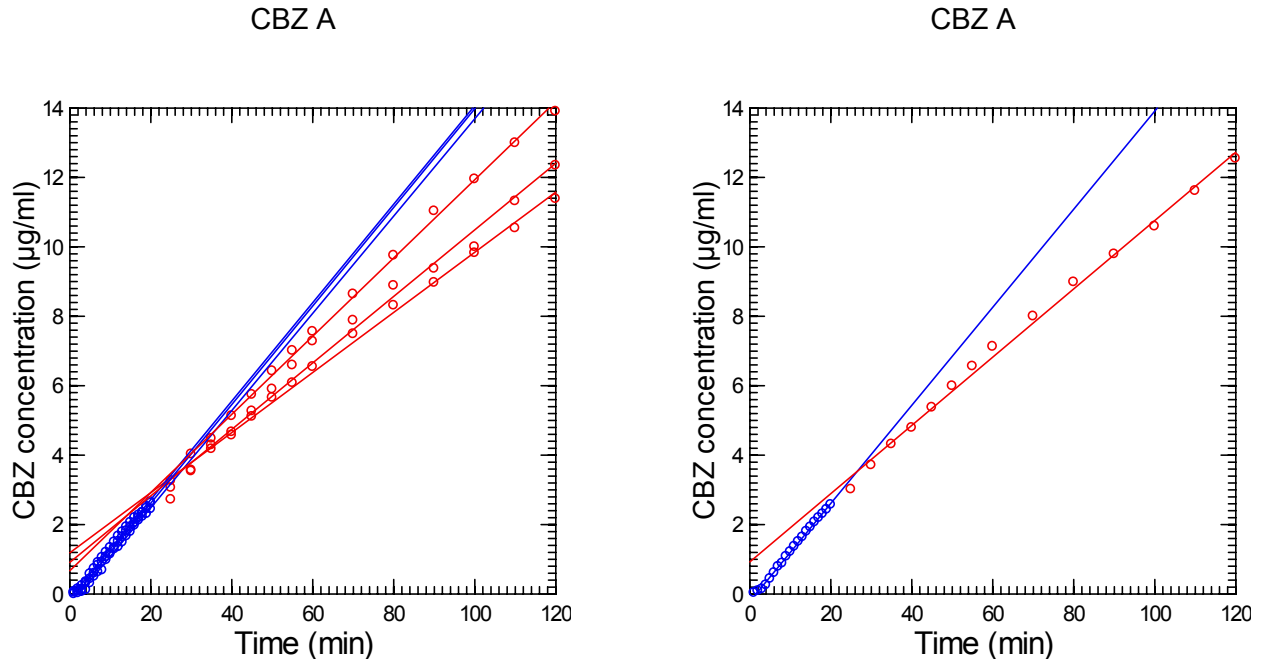


Figure 6.25 Intrinsic dissolution profiles of all batches CBZ A and average for CBZ A divided in initial part (blue) and final part (red)

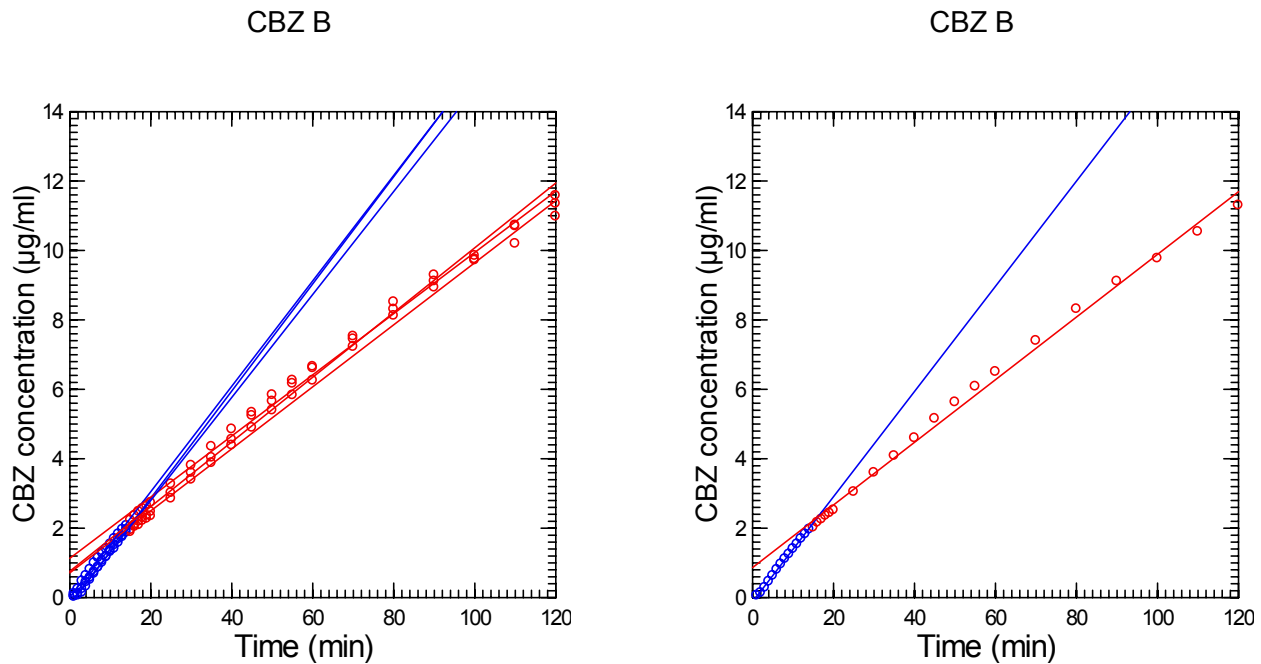


Figure 6.26 Intrinsic dissolution profiles of all batches CBZ B and average for CBZ B divided in initial part (blue) and final part (red)

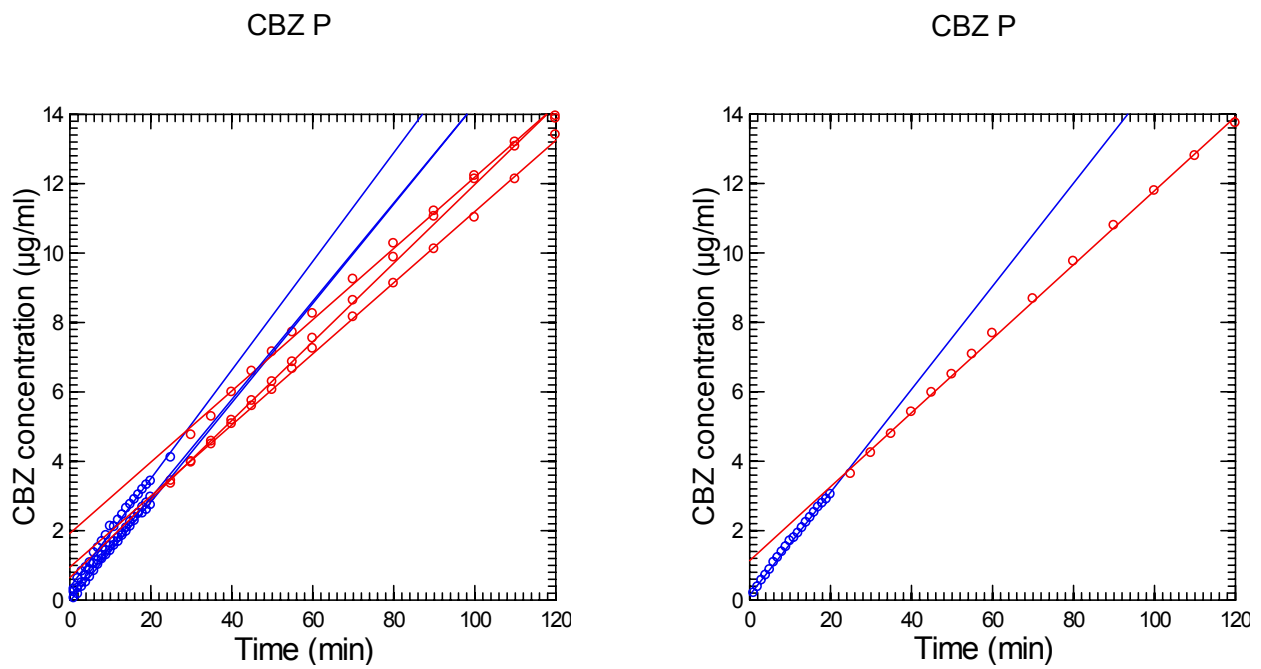


Figure 6.27 Intrinsic dissolution profiles of all batches CBZ P and average for CBZ P divided in initial part (blue) and final part (red)

CBZ

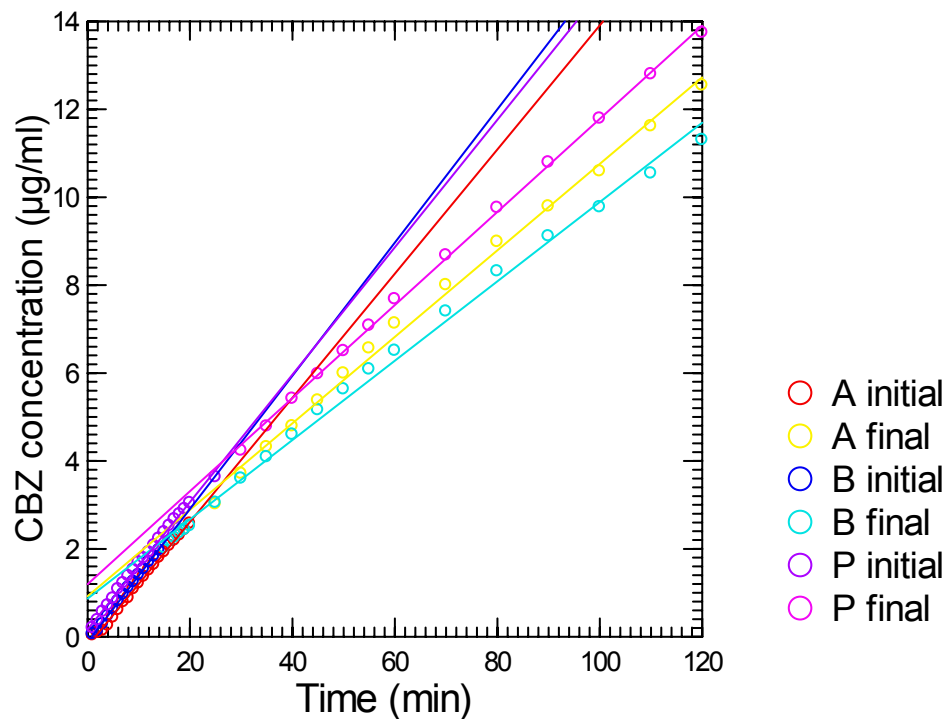


Figure 6.28 Transition points of CBZ A, B and P

It can be seen that the times required for conversion of anhydrous CBZ to dihydrate differed in each group of carbamazepines. They were around 20min, around 15min and between 20 and 25 min for CBZ A, CBZ B and CBZ P respectively. According to literature data, the transformation occurs after 5 to 10 min of intrinsic dissolution test (Kobayashi et al., 2000, Ono et al., 2002). The discrepancies found in the present work can be explained by the different raw material used.

It can be seen in figures 6.25, 6.26 and 6.27, that the initial part of the dissolution curve did not show batch to batch variation for CBZ A and B, while for CBZ P (figure 6.27) deviation was observed.

One-way ANOVA confirmed that the batch to batch variations in CBZ P samples were not statistically significant. The differences seen in the slope of the final segment of the intrinsic dissolution curves, i.e. the slope after the detected transition point can be explained by the differences in the crystallization process of CBZ dihydrates. During the intrinsic dissolution test nucleuses of dihydrate are formed on the surface of the compact which act as initiators for the dihydrate crystallization process. The kinetics of the crystallization process depends on the size of the nucleuses and this can have direct influence on the final slope of DIDR profile.

The segmented plots were analyzed employing the method of Nogami et al (Nogami et al., 1969) and Ono et al (Ono et al., 2002) to calculate the dissolution parameters using the following equations:

$$\frac{dC}{dt} = k_t C_{SH} \quad \text{Equation 6.1}$$

$$\left(\frac{dC}{dt} \right)_{t=0} = k_t C_{SA} \quad \text{Equation 6.2}$$

$$b = \frac{k_t (C_{SA} - C_{SH})}{k_r} \quad \text{Equation 6.3}$$

where:

C represents the concentration of carbamazepine in bulk solution ($\mu\text{g/ml}$)

t is the time (min)

k_t and is the rate constant of the transport process (min)

k_r is the rate constant of the phase transformation process (min)

C_{SH} is the saturated concentration of dihydrate ($\mu\text{g/ml}$)

C_{SA} is the saturated concentration of anhydrous form ($\mu\text{g/ml}$)

b represents the intercept obtained by the extrapolation of the linear portion of the dissolution curve of the anhydrous form.

The parameters k_t , k_r and C_{SA} were calculated from the above equations. k_t or the rate constant of the transport process was calculated from the slope of the dihydrate curve (equation 6.2) using the solubility value for the respective dihydrate C_{SH} obtained from equilibrium solubility testing (see later 6.2.4 and 6.2.5). C_{SA} was calculated from equation 6.1 using the estimate of the slope of the initial segment and the k_t value calculated from equation 6.2. The intercept of the final segment was calculated using the equation 6.3. The results are presented in table 6.14. Table 6.15 shows the average values obtained of all tested CBZ samples. Values for the final slope in anhydrous part were lower than the initial slope (because of phase transformation). However, these values are markedly higher than those of pure dihydrates. The reason may be that even after 2 hours of disc intrinsic dissolution test, there were some parts of compact remaining in anhydrous form which increased the intrinsic dissolution rates. It is interesting to note that CBZ B, which gave the highest amount of drug released in 20 minutes, had a final slope relatively close to the slope of dihydrate, suggesting the most complete transformation from anhydrous to dihydrate.

The turning point on the DIDR curves (transition point), where the slope changes from dissolution of anhydrous CBZ to dissolution of dihydrate, varied from sample to sample: CBZ A ~20 min; CBZ B ~15 min; CBZ P 20~25 min. In addition to that, variations were found in the value for the constant of phase transformation process (k_r) were found (see table 6.14).

Table 6.14 Calculated results from intrinsic dissolution test

Sample (n=5)	Initial slope ($\mu\text{g/ml min}$)	Final slope ($\mu\text{g/ml min}$)	Intercept ($\mu\text{g/ml}$)	k_t (per min)	k_r (per min)	Solubility estimated ($\mu\text{g/ml}$)	Solubility measured ($\mu\text{g/ml}$)
A2	$0,140 \pm 0,003$	$0,087 \pm 0,002$	$1,187 \pm 0,112$		$0,0495 \pm 0,002$	$483,2 \pm 10,4$	$277,4 \pm 7,10$
A3	$0,142 \pm 0,002$	$0,096 \pm 0,003$	$0,915 \pm 0,217$		$0,0651 \pm 0,014$	$493,9 \pm 6,90$	$284,9 \pm 7,20$
A4	$0,142 \pm 0,002$	$0,113 \pm 0,001$	$0,674 \pm 0,097$		$0,0904 \pm 0,010$	$495,9 \pm 7,00$	$283,7 \pm 11,2$
B3	$0,154 \pm 0,004$	$0,089 \pm 0,001$	$0,715 \pm 0,085$		$0,1022 \pm 0,010$	$521,8 \pm 13,5$	$308,9 \pm 11,9$
B4	$0,152 \pm 0,003$	$0,088 \pm 0,001$	$1,135 \pm 0,083$		$0,0635 \pm 0,002$	$524,5 \pm 10,4$	$314,9 \pm 5,60$
B5	$0,148 \pm 0,002$	$0,093 \pm 0,002$	$0,760 \pm 0,091$		$0,0839 \pm 0,008$	$478,0 \pm 6,40$	$307,7 \pm 7,00$
P2	$0,142 \pm 0,002$	$0,113 \pm 0,001$	$0,646 \pm 0,108$		$0,0916 \pm 0,010$	$469,9 \pm 6,60$	$276,8 \pm 12,8$
P3	$0,161 \pm 0,003$	$0,103 \pm 0,002$	$1,898 \pm 0,121$		$0,0421 \pm 0,001$	$555,8 \pm 10,4$	$297,9 \pm 4,20$
P4	$0,142 \pm 0,001$	$0,102 \pm 0,001$	$0,950 \pm 0,061$		$0,0633 \pm 0,004$	$475,7 \pm 11,4$	$280,6 \pm 10,0$
Dihydrates							
DA2		$0,081 \pm 0,000$	$0,007 \pm 0,012$	$0,00029$			$280,2 \pm 0,4$
DA3		$0,082 \pm 0,000$	$0,137 \pm 0,020$	$0,00029$			$286,3 \pm 3,1$
DA4		$0,081 \pm 0,000$	$0,108 \pm 0,015$	$0,00029$			$283,3 \pm 0,1$
DB3		$0,081 \pm 0,001$	$0,230 \pm 0,003$	$0,00030$			$274,6 \pm 3,9$
DB4		$0,080 \pm 0,000$	$0,120 \pm 0,021$	$0,00029$			$275,4 \pm 4,3$
DB5		$0,085 \pm 0,001$	$0,029 \pm 0,043$	$0,00031$			$272,5 \pm 1,3$
DP2		$0,083 \pm 0,001$	$0,036 \pm 0,031$	$0,00030$			$274,1 \pm 2,8$
DP3		$0,081 \pm 0,001$	$0,060 \pm 0,034$	$0,00029$			$279,1 \pm 3,9$
DP4		$0,082 \pm 0,001$	$0,291 \pm 0,034$	$0,00030$			$273,8 \pm 2,0$

Table 6.15 Results for dissolution parameters of anhydrous and dihydrate groups of CBZs

Sample n=(3)	Initial slope ($\mu\text{g/ml min}$)	Final slope ($\mu\text{g/ml min}$)	Intercept ($\mu\text{g/ml}$)	k_t (per min)	k_r (per min)
A	$0,141 \pm 0,002$	$0,098 \pm 0,002$	$0,925 \pm 0,130$		$0,0649 \pm 0,016$
B	$0,152 \pm 0,002$	$0,090 \pm 0,001$	$0,870 \pm 0,084$		$0,0811 \pm 0,008$
P	$0,148 \pm 0,002$	$0,107 \pm 0,001$	$1,137 \pm 0,068$		$0,0583 \pm 0,002$
DA		$0,082 \pm 0,000$	$0,084 \pm 0,014$	0,00029	
DB		$0,082 \pm 0,001$	$0,126 \pm 0,029$	0,00030	
DP		$0,082 \pm 0,001$	$0,129 \pm 0,032$	0,00030	

The highest k_r value means that the sample has ability to undergo the fastest transformation from anhydrous to dihydrate form, which consequently shows the highest IDR. In the study of Ono et al, the k_r value was higher than the values obtained in this study, and the reason is probably because the conversion to dihydrate happened in first 5 minutes (Ono et al., 2002). In all examined samples, the highest k_r value was observed for CBZ B and the lowest one was observed for CBZ P samples. Considering these statements, the correlation between the intrinsic dissolution parameters and the rate of transformation is promising and may help to determine the kinetic of transformation for each examined CBZ and eventually can help to predict its behavior in the final formulation by verifying these parameters in the preformulation stage.

The intrinsic dissolution parameters were used for the calculation of estimated solubility of anhydrous CBZ (equation 6.2). The calculated solubilities were higher than the experimentally obtained equilibrium solubilities (measured after 72 h), because during the solubility measurements transformation of CBZ anhydrous to CBZ dihydrate took place. The estimated solubilities were ranked $C_A\text{CBZ B} > C_A\text{CBZ P} > C_A\text{CBZ A}$ and variations within each manufacturer were maximum 10%, i.e. for CBZ B 507.8 ± 26.1 (CV = 5.1%), for CBZ P 497.4 ± 48.2 (CV = 9.6%) and for CBZ A 491.1 ± 7.7 (CV = 1.4%). The estimated solubility data were in agreement with literature data of form III (Kobayashi et al., 2000).

Table 6.16 Results for solubility and IDR of anhydrous CBZs

Sample (n=3)	Solubility estimated ($\mu\text{g/ml}$) \pm SD	Solubility measured ($\mu\text{g/ml}$) \pm SD	IDR ($\mu\text{g/min/cm}^2$) \pm SD
A	491,1 \pm 7,70	277,4 \pm 4,10	69,11 \pm 1,96
B	507,8 \pm 26,1	284,9 \pm 3,90	77,45 \pm 2,04
P	497,4 \pm 48,2	283,7 \pm 11,2	73,92 \pm 2,00

Intrinsic dissolution rates were calculated from the initial part of each profile using the equation 3.8, see 6.5.3. The obtained results have the same ranking as reported in the estimated solubility, i.e. IDR CBZ B > IDR CBZ P > IDR CBZ A, see table 6.16. The values of IDR in this study were slightly higher than data for IDR of polymorphic form III found by Kobayashi et al (Kobayashi et al., 2000). The differences in the intrinsic dissolution rates described by a single value, for different samples were not relatively high. However, the differences in the intrinsic dissolution behavior described by a set of parameters were found to be of great importance. Considering that carbamazepine has narrow therapeutic index and very narrow dissolution range of acceptance criteria in USP monographs, the variation in the kinetics of conversion from anhydrate to dihydrate form among different raw material of CBZ are useful information. Therefore the point of transformation as well as the kinetics of the phase transformation may be considered as critical parameters which should be investigated during the characterization of carbamazepine.

6.2. Carbamazepine dihydrate characterization

CBZ dihydrate samples were prepared in order to calculate the IDR parameters of anhydrous form. For the calculation of the k_t value or rate constant of transport process, it was necessary to have information about the solubility of CBZ dihydrates and also to measure the intrinsic dissolution of the pure dihydrate form.

It was already seen that samples of the commercial anhydrous CBZ, although being form III, showed variations in DSC behavior, intensity of XRPD peaks, solubility (estimated) and intrinsic dissolution behavior. In particular, the variations in intrinsic dissolution behavior were similar to those found in the dissolution of CBZ immediate

tablet formulations in Bosnalijek's R&D. Therefore it was proposed to convert the anhydrous CBZ into their respective dihydrates and to evaluate the impact of this strategy on the variability seen in commercial CBZ products. Namely, it was already shown in the previous discussion, that variability due to previous history of the samples (e.g. manufacturing process, grinding etc) influenced their intrinsic dissolution behavior. Thus the question: Can the observed variability be eliminated or indeed “erased” from the previous history of anhydrous commercial products by converting them their dihydrate form? For this purpose, dihydrates of all commercial anhydrous samples were prepared and were fully characterized prior to subjecting them to intrinsic dissolution testing

6.2.1. X-ray powder diffraction of dihydrates

CBZ dihydrate has its own unique XRPD pattern. CBZ dihydrates prepared from the nine available samples (CBZ DA, DB, DP) had characteristic reflections at $2\theta = 8,9$; $18,9$ and $19,4$ which correspond to literature data for CBZ D (Carino et al., 2006, Kobayashi et al., 2000). It was therefore confirmed that CBZ dihydrate was properly formed. In addition it was also observed that the differences in the intensity of the peaks found on the X-ray diffractograms of CBZ A, B, and P disappeared after their conversion to dihydrate, see figure 6.29.

6.2.2. Loss on drying

Complete hydration of the anhydrous samples was confirmed by the loss on drying method. The water content of the anhydrous CBZ was $0.1 \pm 0.05\%$ whereas the, dihydrate samples had a loss on drying of $13,2\%$ for CBZ DA, $13,3\%$ for CBZ DB and $13,1\%$ for CBZ DP. These values are nearly equal to the stoichiometric value calculated for the water content of CBZ dihydrate ($13,2\%$ wt/wt) reported in literature (McMahon et al., 1996). The weight loss is attributed to the dehydration of CBZ D, i.e. removal of lattice water (Surana et al., 2003).

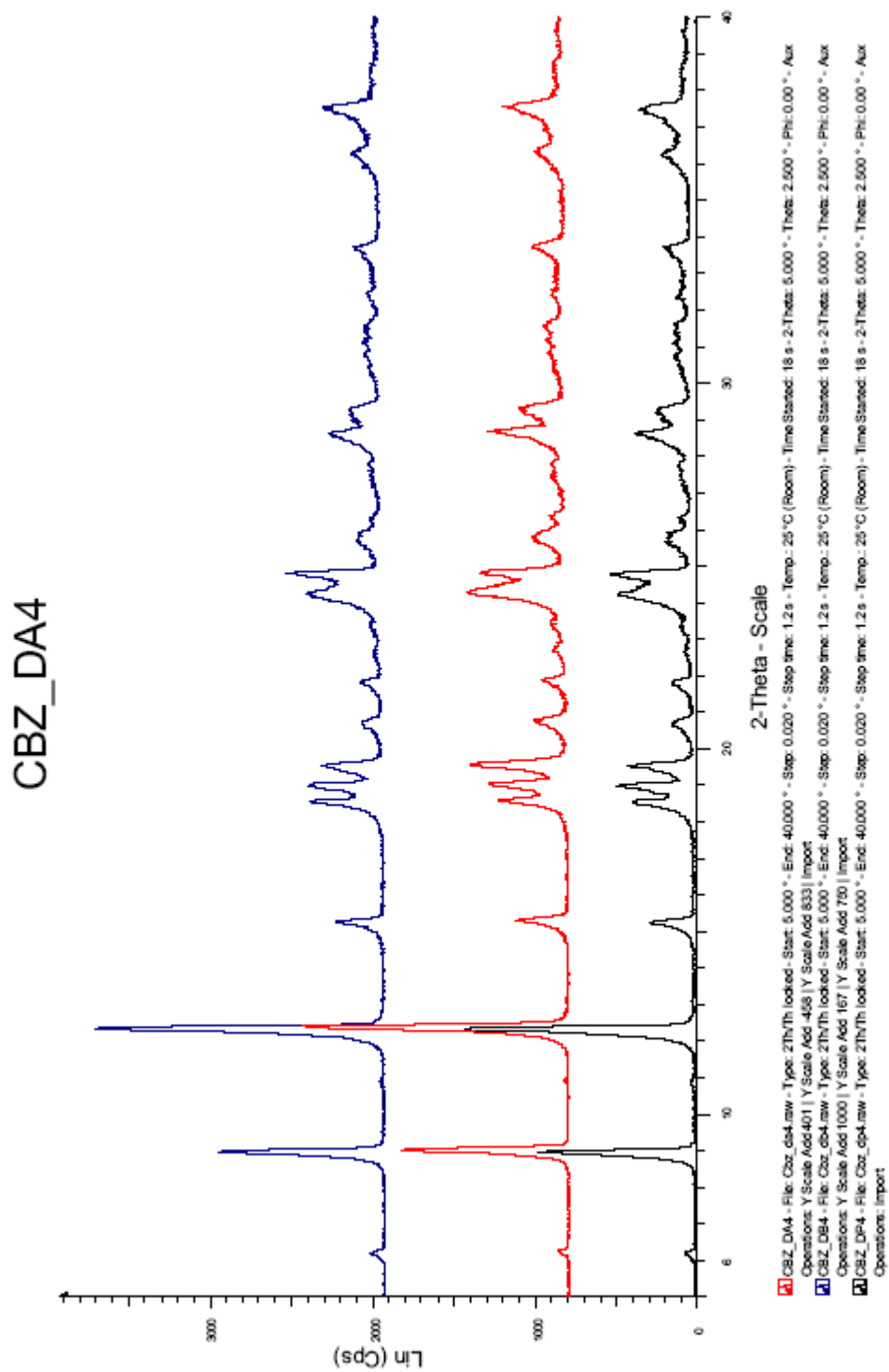


Figure 6.29 X-ray diffractograms of CBZ DA, CBZ DB, CBZ DP

6.2.3. Differential scanning calorimetry (DSC) of dihydrates

The DSC thermograms of dihydrate prepared from the USP standard (CBZ USP D) obtained at heating rate of 10°C/min showed two endotherm peaks (see figure 6.30): a broad peak in the range of 75-87°C representing dehydration/vaporization of water and a sharp peak at 192°C representing melting process of CBZ with enthalpy $\Delta H=95.8\text{J/g}$. These findings were in good agreement with the results reported for CBZ dihydrate (Li et al., 2000, Surana et al., 2003).

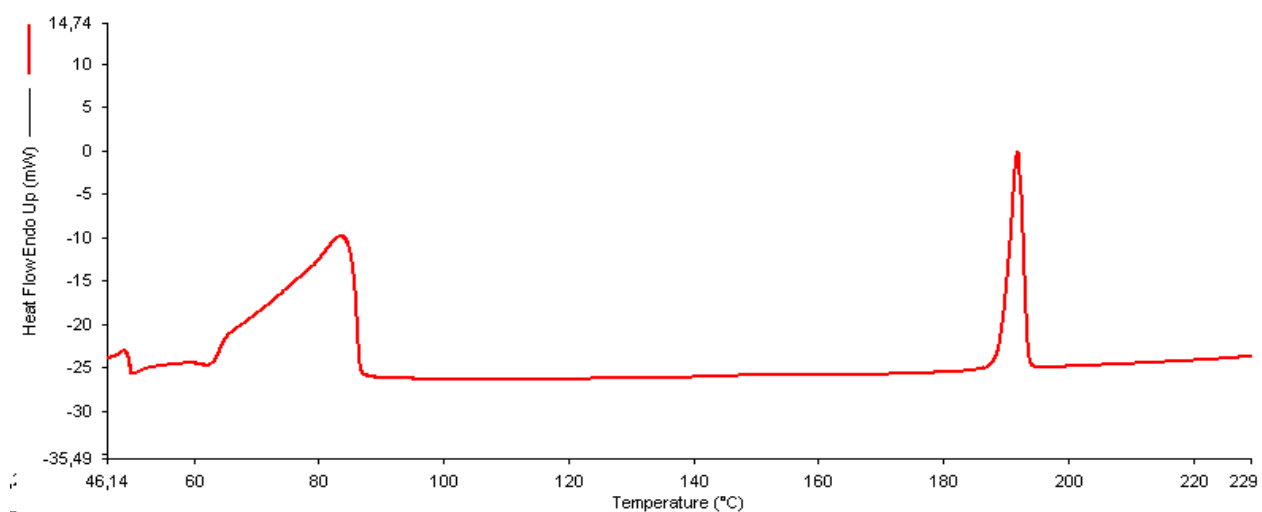


Figure 6.30 DSC thermogram of CBZ USP D at heating rate of 10°C/min

DSC results of the dihydrate samples prepared from nine CBZ anhydrous confirmed that dihydrates were formed successfully. All of them exhibited the same behavior as CBZ USP D, as illustrated in figure 6.30. Contrary to DSC results of CBZ anhydrous forms which exhibited the differences in enthalpies of melting of form I (among CBZ A, B and P) and shift of the peak for CBZ P, the DSC results of all dihydrate samples prepared from CBZ A, B and P showed no variation among each other, see figure 6.31 and table 6.17.

In other words, differences in the thermal behavior which were detected in same polymorphic forms of CBZ samples obtained from different sources were practically deleted by converting commercial anhydrous form to dihydrates.

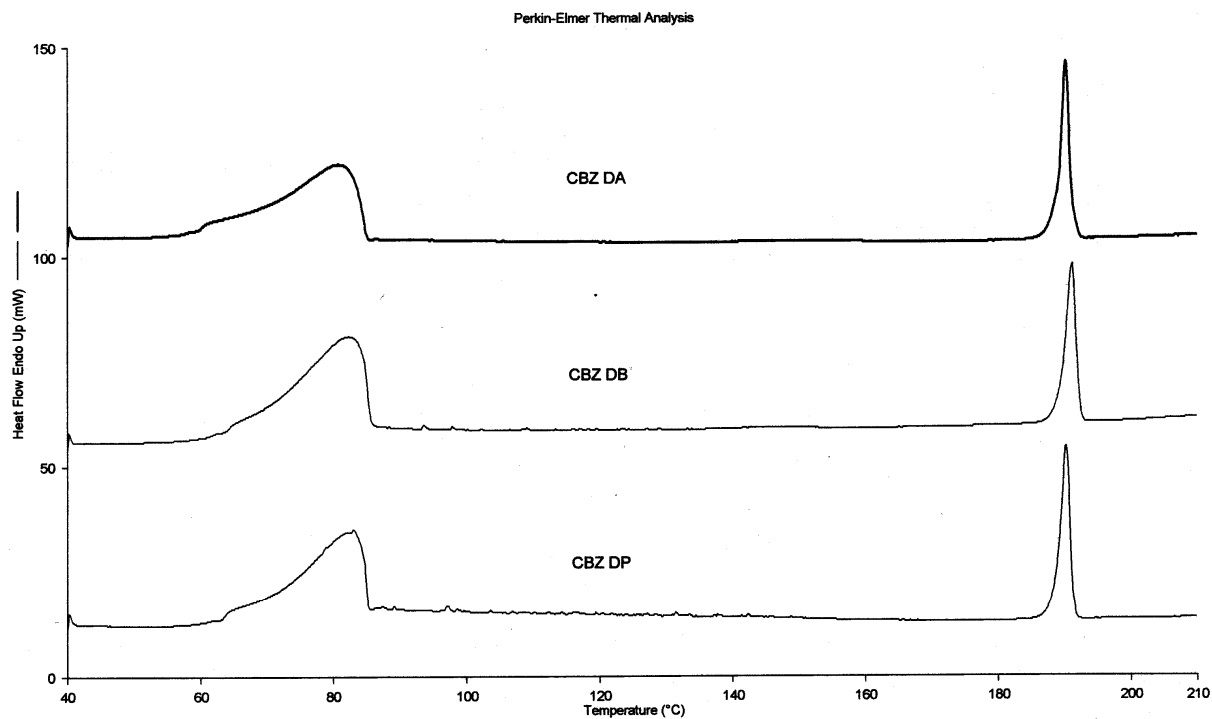


Figure 6.31 DSC thermograms of CBZ DA, DB and DP at heating rate of 10°C/min

Table 6.17 DSC results of CBZ USP D, DA, DB and DP at heating rate of 10°C/min

Sample (n=9)	Dehydration range ± SD (°C)	Dehydration ± SD (°C)	Dehydration $\Delta \pm$ SD (J/g)	Melting point of form I ± SD (°C)	Melting $\Delta \pm$ SD (J/g)
CBZ USP D	63.0 – 86.6 (± 1.2)	83.5 ± 1.1	299.2 ± 4.1	192.9 ± 0.4	95.9 ± 2.4
CBZ DA	73.5 – 84.4 (± 1.3)	81.2 ± 0.1	268.9 ± 11.5	190.4 ± 0.0	92.9 ± 1.5
CBZ DB	74.4 – 85.0 (± 1.1)	81.9 ± 0.1	290.2 ± 16.3	190.5 ± 0.0	92.3 ± 0.9
CBZ DP	71.6 – 84.9 (± 1.4)	81.9 ± 0.3	268.9 ± 10.3	190.1 ± 0.1	92.7 ± 2.5

DSC measurements on dihydrate samples were conducted also at the heating rate of 40°C/min as in the case of the anhydrous samples. As the heating rate was increased the dehydration process was shifted to higher temperature range. These profiles revealed that the faster the heating rate was chosen, the wider was the temperature range over which dehydration of water occurred. No significant differences between USP dihydrate (see figure 6.32 and table 6.18) and CBZ DA, DB and DP behavior were found (figure 6.33).

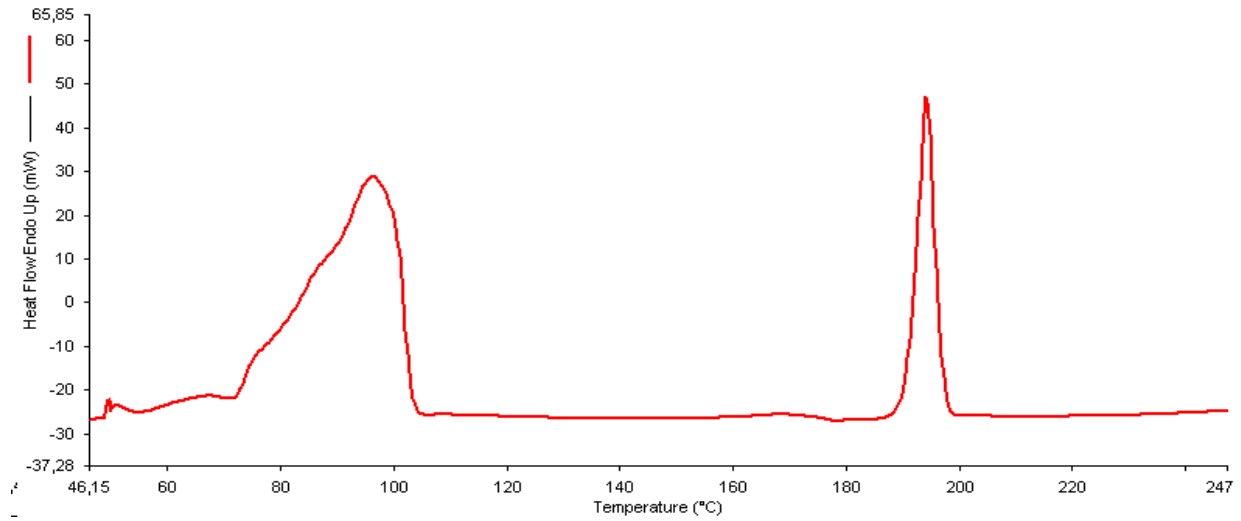


Figure.6.32 DSC thermogram of CBZ USP D at heating rate of 40°C/min

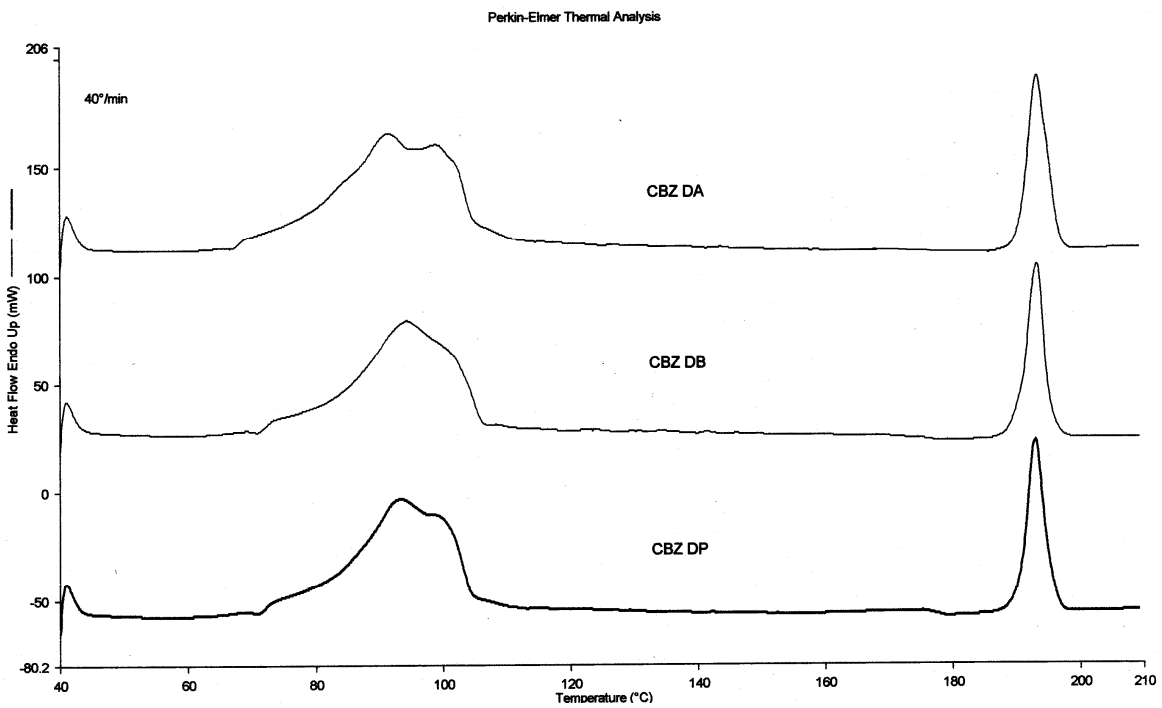


Figure 6.33 DSC thermograms of CBZ DA, DB and DP at heating rate of 40°C/min

Table 6.18 DSC results of CBZ USP D, DA, DB and DP at heating rate of 40°C/min

Sample (n=9)	Dehydration range ± SD (°C)	Dehydration ± SD (°C)	Dehydration Δ ± SD (J/g)	Melting point of form I ± SD (°C)	Melting Δ ± SD (J/g)
CBZ USP D	80.1 –103.2 (±0.3)	96.3 ± 1.1	307.5 ± 7.1	194.1 ± 0.2	95.5 ± 1.5
CBZ DA	80.0 –116.1 (±0.1)	92.1 ± 0.4	329.4 ± 8.5	193.2 ± 0.4	95.0 ± 3.7
CBZ DB	82.0 –107.0 (±0.3)	93.4 ± 2.0	310.3 ± 17.4	193.3 ± 0.1	94.6 ± 0.4
CBZ DP	81.9 –104.7 (±0.4)	92.7 ± 0.9	284.5 ± 3.5	192.9 ± 0.1	87.3 ± 1.9

6.2.4. Solubility of dihydrates

Dihydrate of CBZ is the stable form in aqueous conditions, therefore no phase transformation during this test was expected. The solubility of dihydrates was determined by supersaturation, where an excess amount of CBZ dihydrate solid phase was added to distilled water at 37±1°C and was shaken for 72h to equilibrium.

The obtained results are presented in following table 6.19, and are compared with the solubility data of “anhydrous” CBZ obtained previously with the same method.

Table 6.19 Solubility parameters after 72h

Sample (n=9)	Solubility ± SD (µg/ml) after 72h DIHYDRATE	Solubility ± SD (µg/ml) after 72h “ANHYDROUS”
CBZ A	283.3 ± 3.0	282.0 ± 4.1
CBZ B	274.2 ± 1.5	310.5 ± 3.9
CBZ P	275.7 ± 2.9	286.4 ± 11.2

One way ANOVA analysis showed that there were no significant differences in solubility between dihydrates prepared from CBZ A, CBZ B and CBZ P. Furthermore, no differences were found within dihydrates prepared from different batches of the same producers.

It can be noted that the solubility values of dihydrates measured after 72 hours were approximately equal to the values of anhydrous CBZ measured in the same time interval, except for CBZ B. The reason for this is that during the measurement time, the anhydrous CBZ was converted completely or almost completely to dihydrate. In the case of CBZ B, the measured solubility of the anhydrate was slightly higher than in the

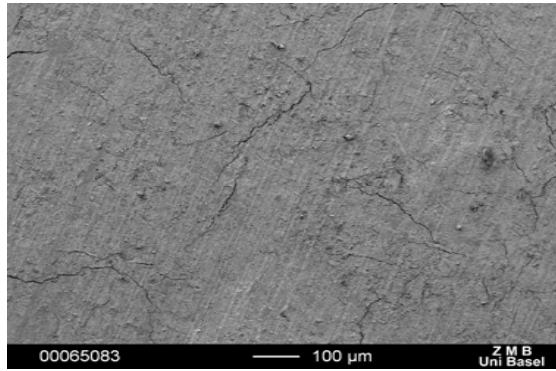
other samples, most likely because the transformation was not yet fully completed. Therefore, for correct determination of the disc intrinsic dissolution rate of the anhydrous forms, the estimated solubilities of the anhydrous forms should be taken into account, not the measured ones.

Comparing the solubilities of the dihydrates with the results of the respective anhydrous forms obtained by the estimation from IDR results, those of the dihydrate are 1.7 – 1.8 times lower, which is in agreement with literature data (Kaneniwa et al., 1987, Kobayashi et al., 2000).

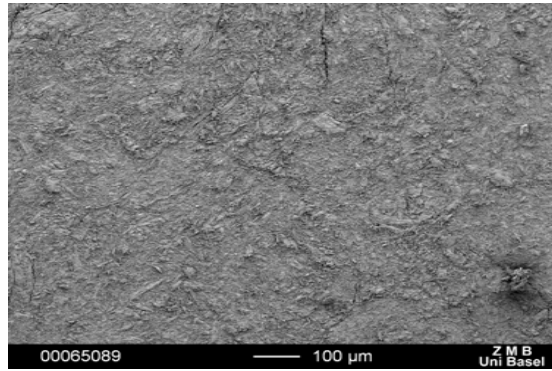
6.2.5. Disc intrinsic dissolution of dihydrates

Whereas, during the preparation of compacts for the intrinsic dissolution tests of anhydrous forms, carbamazepine showed poor compactibility properties, such as capping and lamination (lamination being major problem in the case of CBZ USP samples), after converting commercial CBZ samples to the respective dihydrate forms, their compactibility was improved. There were no problems with capping or fragmentation of the compacts edges. In order to obtain compacts with the same porosity of 12% as for the anhydrous CBZ, the applied compaction force was between 6 and 8kN. Dihydrate compact were robust, easy to handle and their crushing strength was much higher than that of anhydrous compacts (ranging between 120 and 135N).

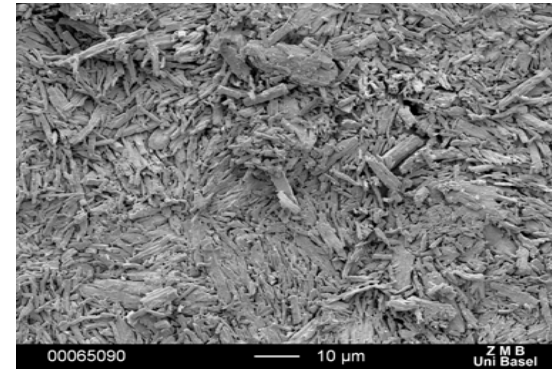
The surfaces of the dihydrate compacts were analyzed by SEM before and after dissolution and their pictures are presented in figure 6.34. As a result of the improved mechanical property, the surfaces of dihydrate compacts prior to dissolution appeared smoother and the gaps observed in the anhydrous compacts were not present. Moreover the surfaces of the dihydrates compacts did not show variations as was the case with their respective anhydrates. The SEM analysis confirmed as well that the dihydrate was prepared properly because no parts of prismatic particles (of form III) were present in the analyzed samples. Regarding the surface of the compacts after dissolution, only needle-like forms (dihydrate) were found at the end of dissolution tests (after 120 minutes).



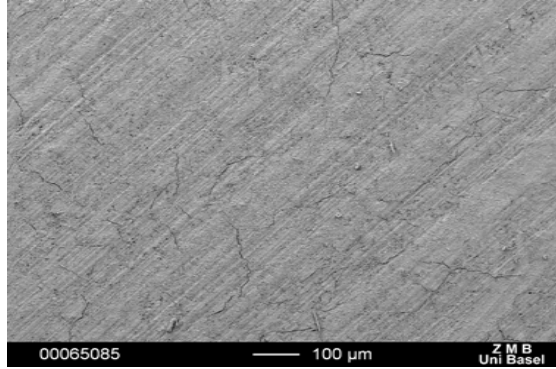
CBZ DA before (magnification 100)



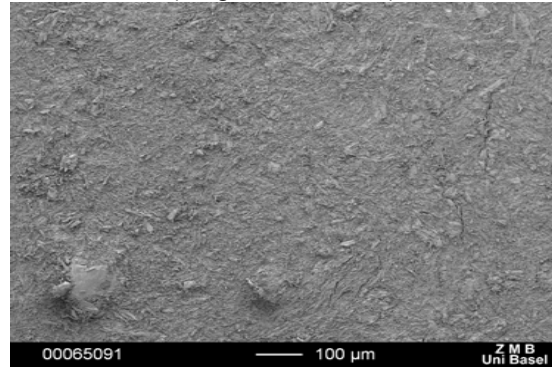
CBZ DA after (magnification 100)



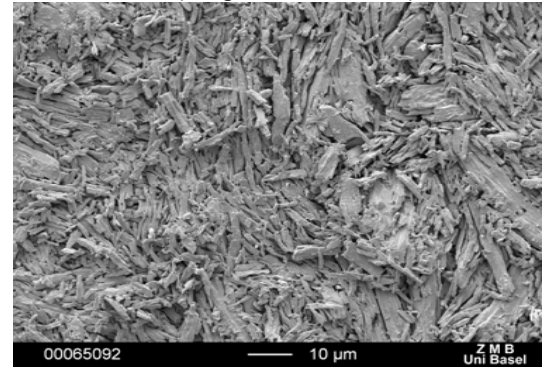
CBZ DA after (magnification 1000)



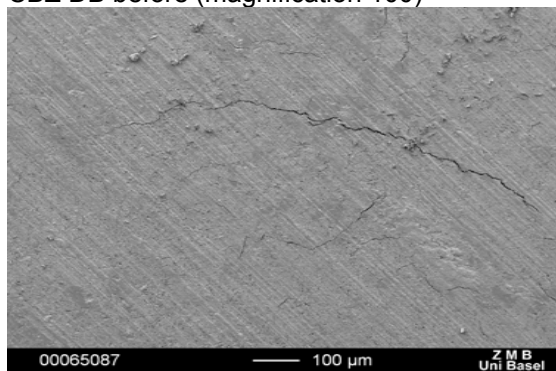
CBZ DB before (magnification 100)



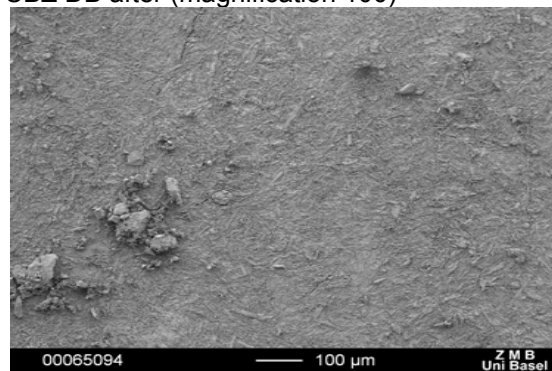
CBZ DB after (magnification 100)



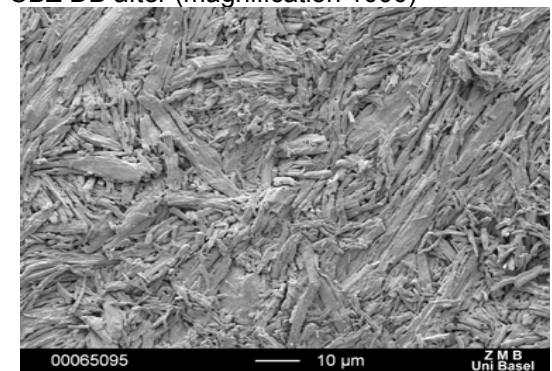
CBZ DB after (magnification 1000)



CBZ DP before (magnification 100)



CBZ DP after (magnification 100)



CBZ DP after (magnification 1000)

Figure 6.34 Surface of compacts before and after disc intrinsic dissolution

Under constant hydrodynamic conditions, the intrinsic dissolution rate is usually proportional to the solubility of the dissolving solid. Consequently, in a polymorphic system, the most stable form will ordinarily exhibit the slowest intrinsic dissolution rate. It also has been noted in the earliest dissolution work (Shefter et al., 1963) that, for many substances, the dissolution rate of an anhydrous phase usually exceeds that of any corresponding hydrate phase. These observations were explained by thermodynamics, where it was reasoned that the drug in the hydrates possessed a lower activity and would be in a more stable state relative to their anhydrous forms. This general rule was found to hold for anhydrous/hydrate phases of carbamazepine (Brittain, 1999).

The conditions for intrinsic dissolution of dihydrates were kept the same as for the intrinsic dissolution rate measurements of anhydrous forms.

During intrinsic dissolution of dihydrates, no phase transformation was expected, and therefore the dissolution profiles exhibited the characteristic linear shape. In respect to that, the initial and final segment of CBZ dihydrate IDR curve were the same, which means that estimated and measured solubility of dihydrate should be practically identical.

The intrinsic dissolution profiles of each group of different dihydrates (CBZ DA, DB and DP) are presented in figures 6.35, for time period of 20 minutes and in figure 6.36, for period of 120 minutes respectively. In these diagrams only CBZ DP2 sample showed faster dissolution in the first 20 minutes in comparison to the other DP samples, but during 120 minutes even that difference was not observed any longer.

One way ANOVA was used to evaluate of the dissolution profiles. It was confirmed that there was no significant difference within different batches and between dihydrates of CBZ DA, DB and DP. Also the observed faster dissolution of DP2 was not found to be significantly different from other CBZ DP dihydrates.

In the previous section (see 6.2.4), it was discussed that CBZ dihydrates, as the most stable form in aqueous solution, exhibited lower solubility than the respective CBZ anhydrites.

Consequently, because of lower solubility, the amount of CBZ dissolved from the surface of the compact decreased in comparison with the amount dissolved from anhydrate CBZ surfaces, and in addition the intrinsic dissolution rate was slower.

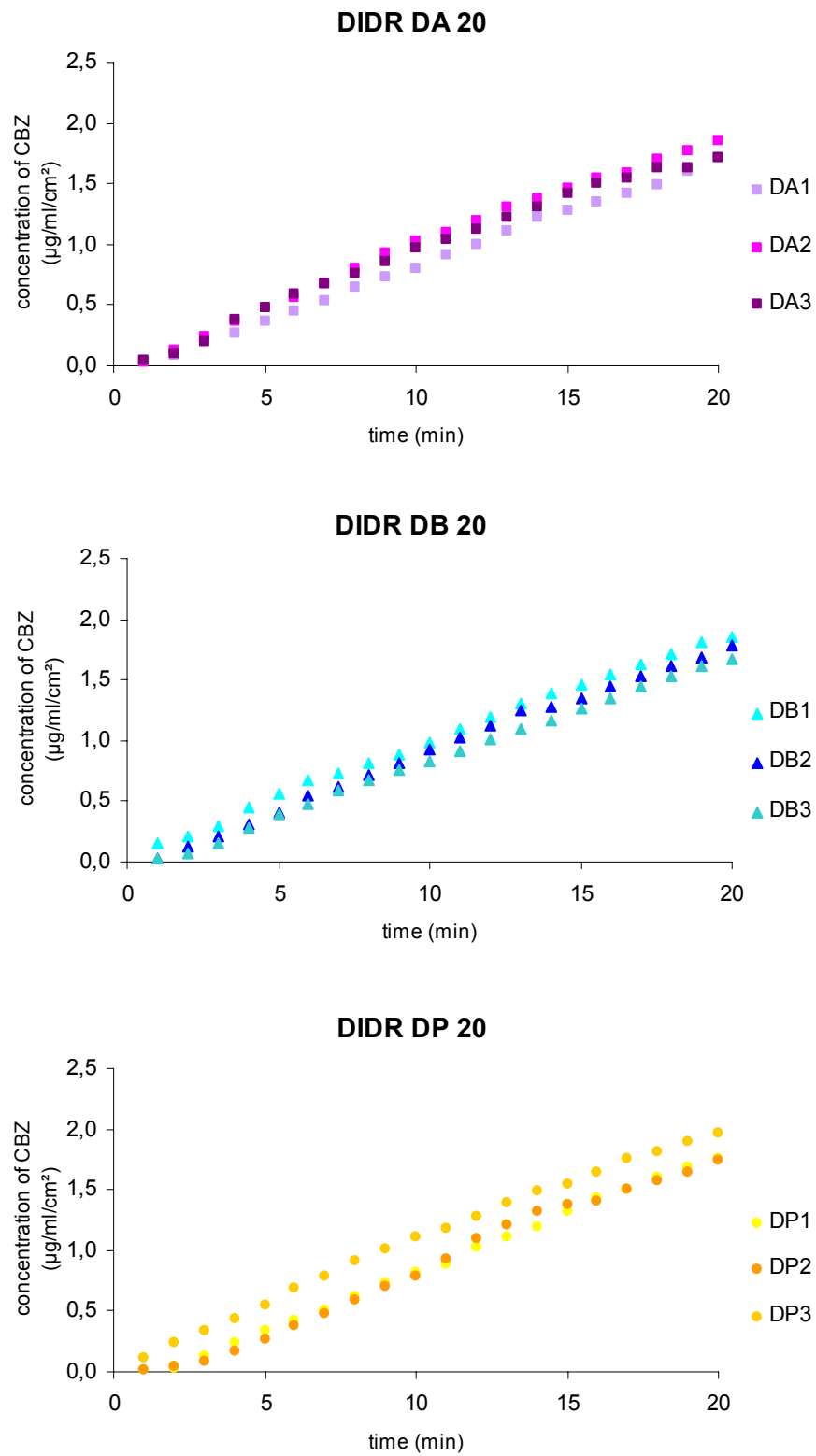


Figure 6.35 Intrinsic dissolution profiles of CBZ DA, DB and DP for first 20 minutes

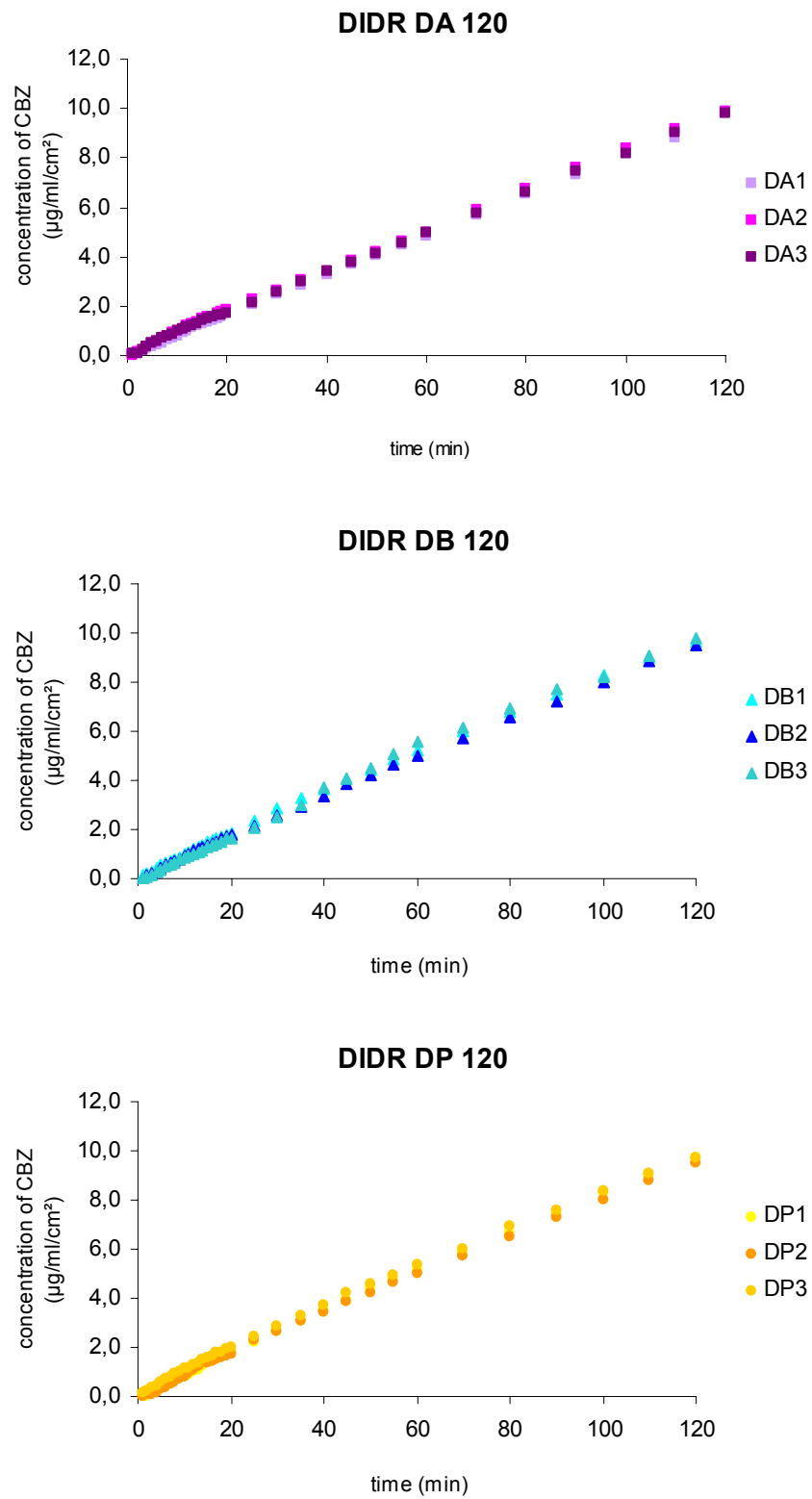


Figure 6.36 Intrinsic dissolution profiles of CBZ DA, DB and DP for 120 minutes

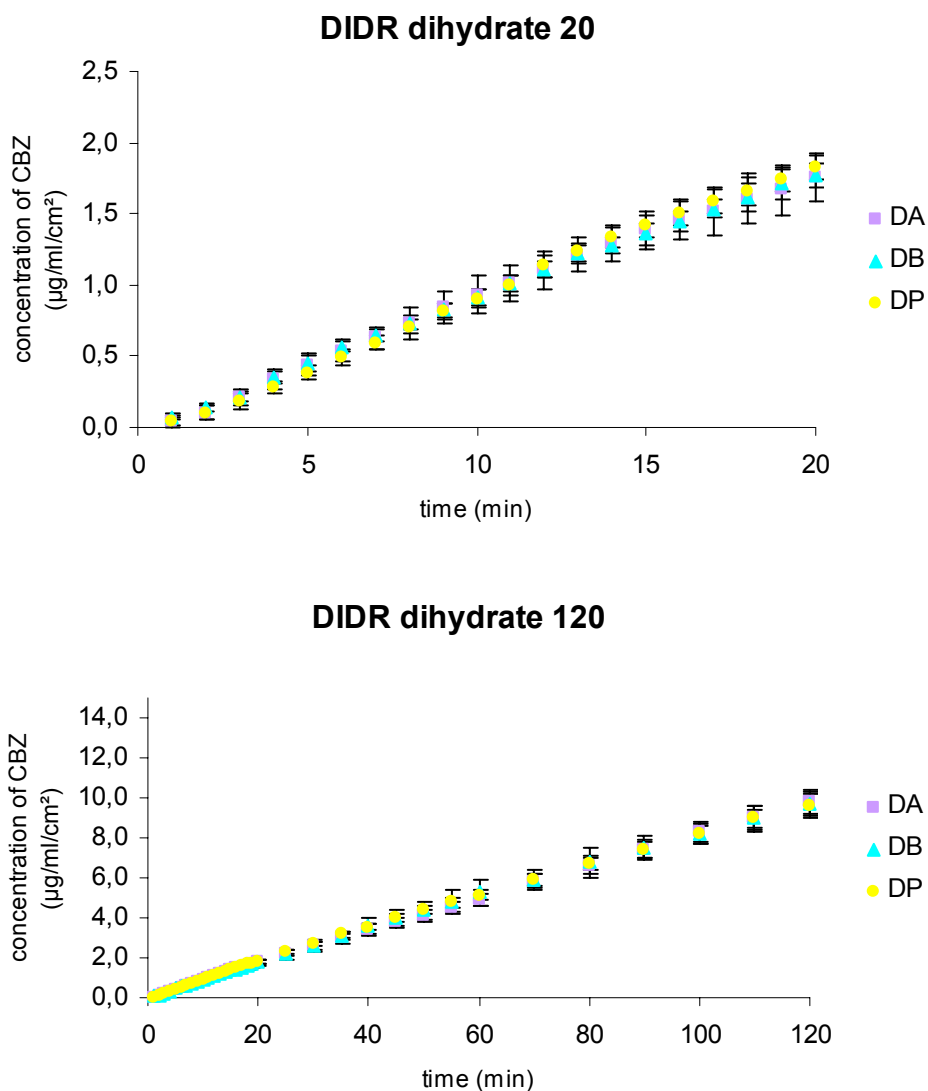


Figure 6.37 Intrinsic dissolution profiles of CBZ DA, DB and DP

It is well known that different polymorphic forms may show different dissolution behavior. In the case of the examined CBZ samples, differences in dissolution behavior were observed even the samples exhibited the same polymorphic form. Moreover, high standard deviations were found within each anhydrous CBZ. By converting the commercial CBZ samples to dihydrate form, the step of phase transformation A→D, as the most problematic and critical property of CBZ was skipped. Thus, the dissolution behavior of dihydrates was found to be more uniform. Furthermore, in all examined CBZ D samples standard deviation was found to be much lower than in their respective anhydrides, therefore the dissolution behaviors was considerably improved, figure 6.38.

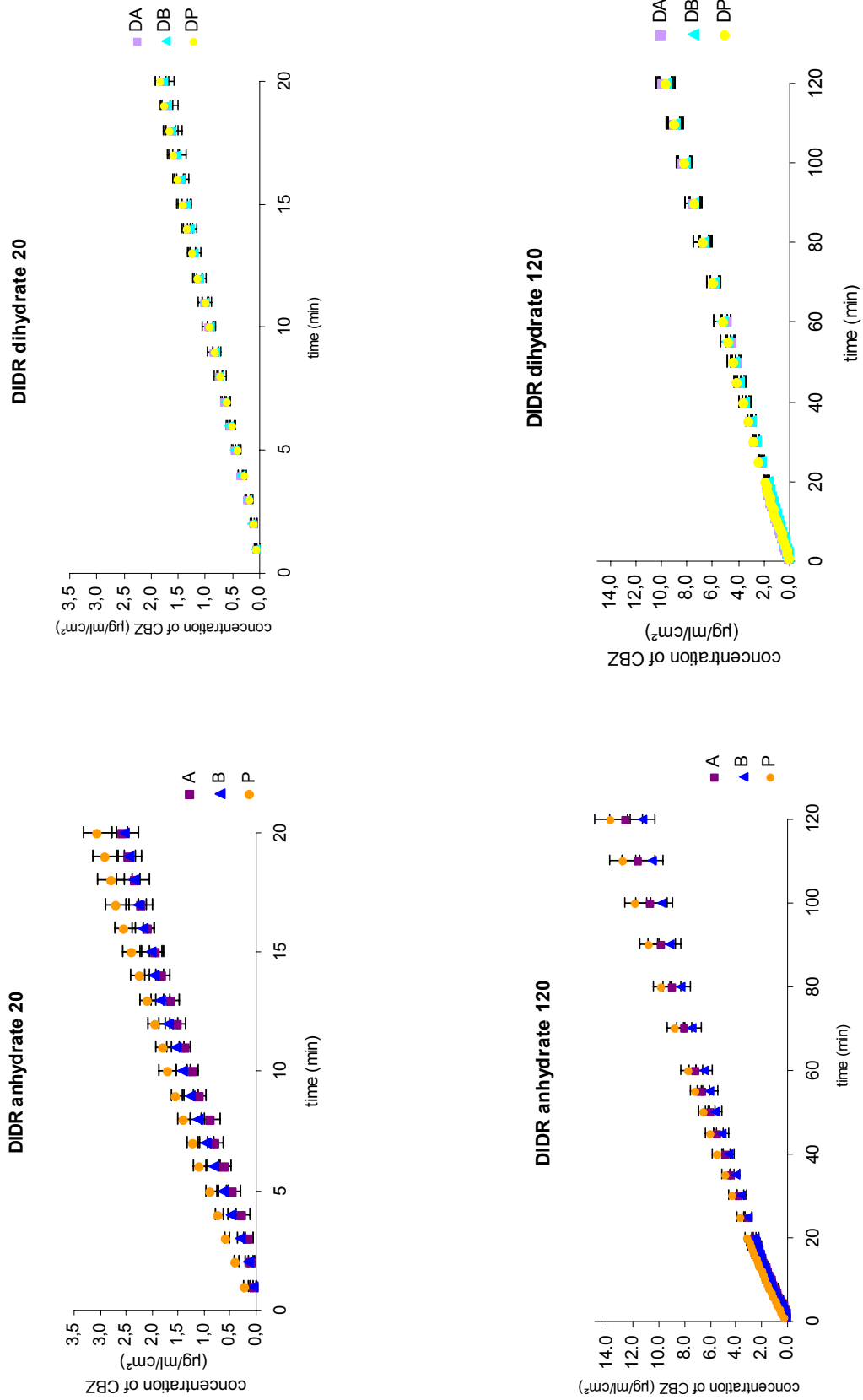


Figure 6.38 Comparison of the intrinsic dissolution profiles of anhydrous and dihydrates CBZ

Systat software was used to calculate intrinsic dissolution parameters, as presented in table 6.14. The slopes of CBZ DA, DB and DC were 0.082 ± 0.001 and that value was used in calculations of IDR (see figure 6.39 and table 6.20).

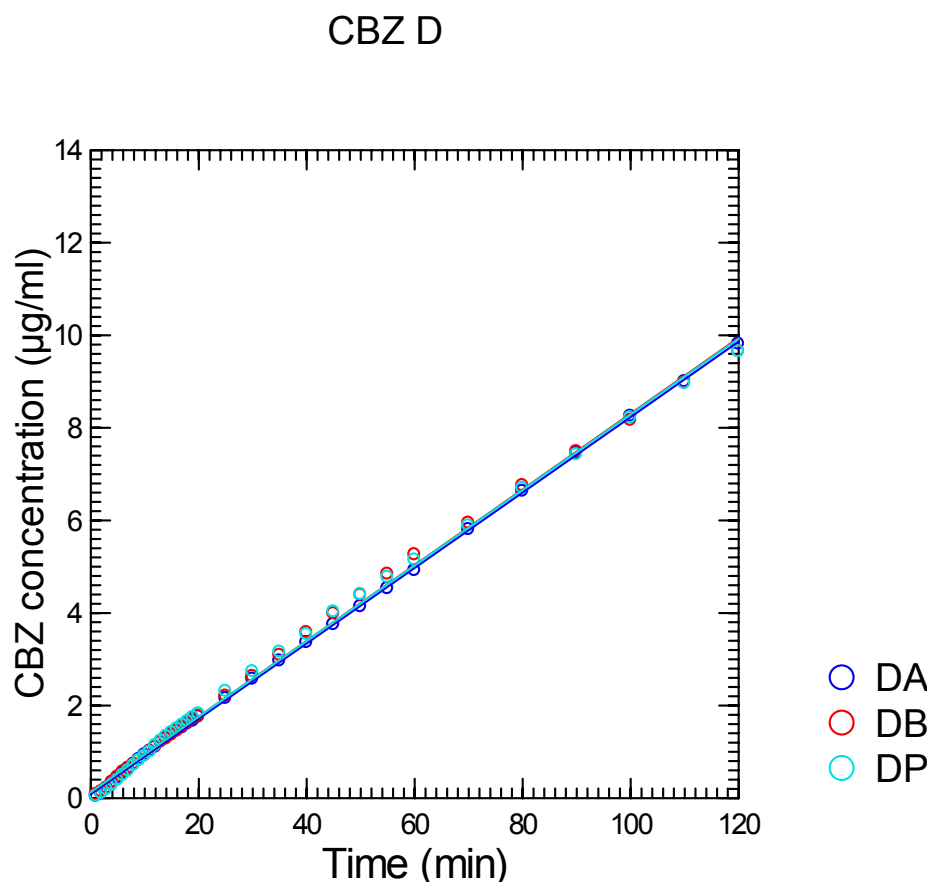


Figure 6.39 Intrinsic dissolution data of CBZ dihydrates analyzed by Systat software

IDR of CBZ DA, DB and DP showed no variations, but they were slightly higher than those reported by Murphy (Murphy et al., 2002). However, because of lower solubility of dihydrate form, the values were three times lower than the IDR of the anhydrous forms.

Table 6.20 Intrinsic dissolution rate of carbamazepine dihydrates

Sample	IDR ($\mu\text{g}/\text{min}/\text{cm}^2$) \pm SD
DA	$23,09 \pm 0,40$
DB	$22,43 \pm 0,63$
DP	$22,52 \pm 0,20$

6.3. The influence of particle size on IDR behavior

Disc intrinsic dissolution rate is a method for evaluating the intrinsic properties of the material in the dissolution medium, regardless of the size of starting particles, because they are compressed into a compact. However, because the SEM pictures showed that the surfaces of the CBZ compacts were affected by the particle size, it was necessary to test if the different particle sizes of the same material will have any influence on the IDR. Furthermore, since the solubility and the IDR of the metastable anhydrous form in water were estimated and calculated respectively from the initial part of the intrinsic dissolution curve, the effect of the size on the intrinsic dissolution of the samples with different particle size needs to be addressed.

One of the CBZ P samples was selected for this particular investigation. The sample P3 was divided in 4 fractions of particles with different size ranges:

- P3a from 125 to 180 μm ;
- P3b from 180 to 250 μm ,
- P3c from 250 to 355 μm
- P3d, where all the particles were bigger than 355 μm .

CBZ is known to undergo fragmentation during compaction (Bolourtchian et al., 2001). In respect to that no variation in compaction behavior was found in different fractions. All of them were compacted to constant porosity of $12\pm 0.3\%$. Crushing strength of produced compacts was between 35 and 40N. The surface morphology of compacts before and after the intrinsic dissolution was observed by SEM, see figure 6.40.

Variations in the starting surface of the compacts were observed. The compacts made of the biggest particles (P3d) had the flattest surface in comparison to others, but on the other hand they also showed areas with deep ruptures on the surface. Those ruptures could potentially parts which could increase the surface area of the tablet itself, and consequently larger amount of anhydrous CBZ will eventually be exposed to the dissolution medium. After the dissolution, the surfaces were more or less the same in all investigated samples with characteristic needles of CBZ dihydrate form. As it was seen previously in CBZ P samples, in some areas of examined compacts prepared from different particle size fractions, the anhydrous CBZ was not converted to dihydrate.

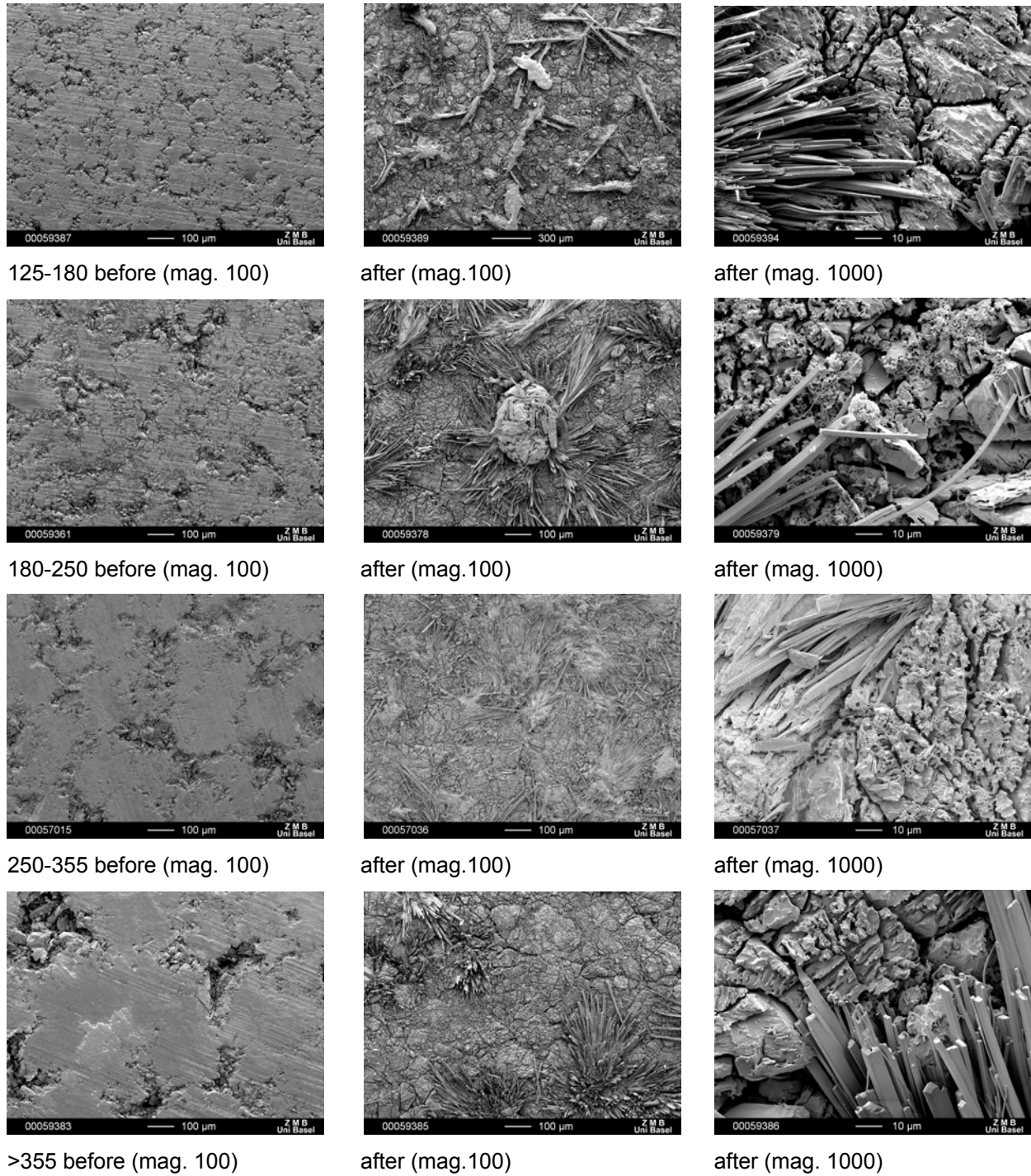


Figure 6.40 Compact surface for P3 samples made by compressing fractions of different particle size; before and after intrinsic dissolution

Systat software was used to divide the intrinsic dissolution profiles into initial (anhydrous dissolution) and final (dihydrate dissolution) segments, see figure 6.41.

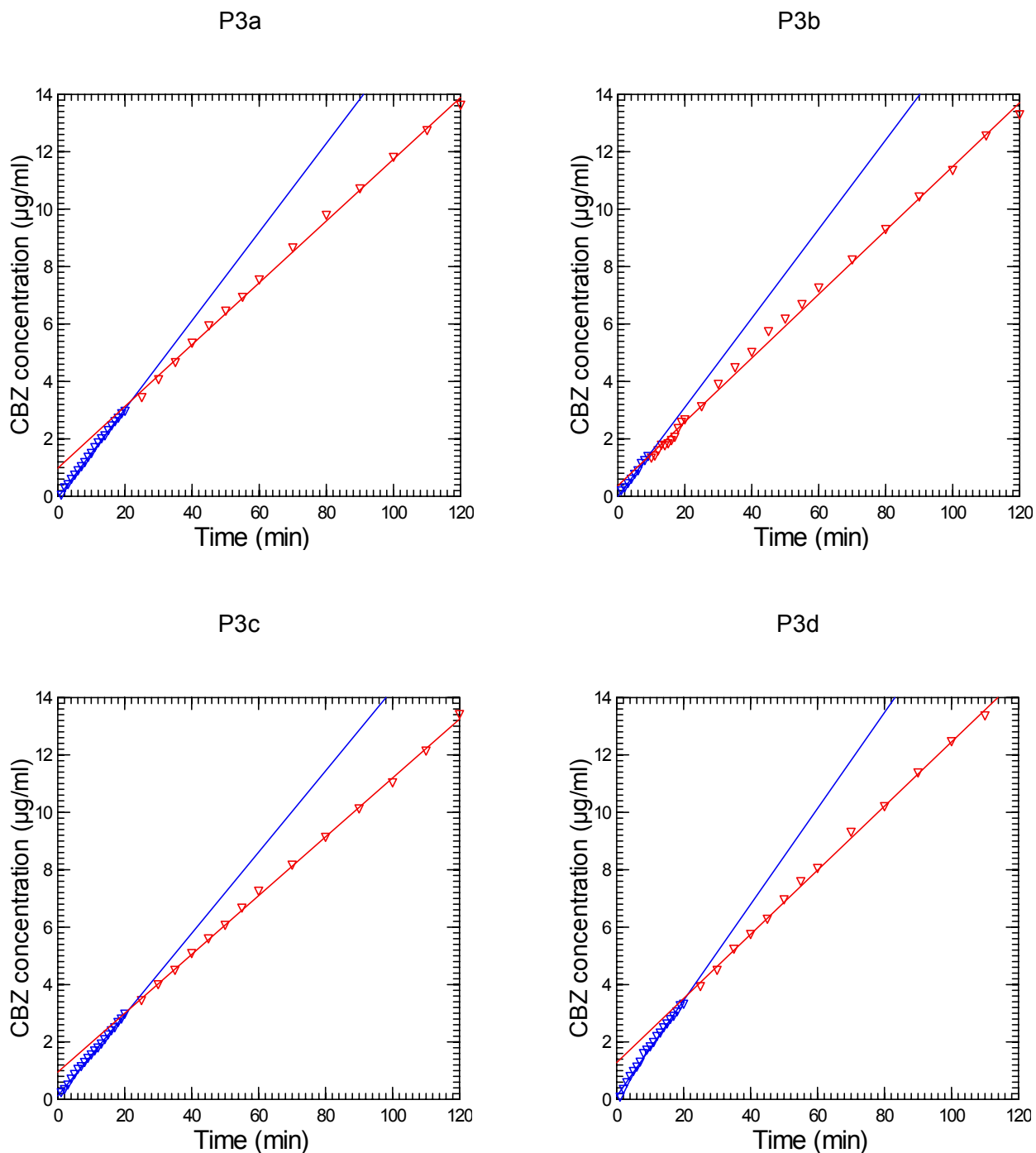


Figure 6.41 IDR profiles of P3 samples analyzed by Systat software

Variations in the transformation time of anhydrous to dihydrate were observed: in the case of P3b, this happened in 10 minutes, while for P3a, P3c and P3d took place in about 20 minutes (the time corresponded to the one measured in previous experiments using whole powder). This shorter time for transformation of P3b resulted in higher value of the constant of transformation (k_r).

The values obtained using Systat software for the initial slope, final slope and intercept for the calculated constants (k_r and k_t) are presented in table 6.21.

Table 6.21 Results for dissolution parameters of CBZ P3 samples

Sample	Initial slope ($\mu\text{g/ml min}$)	Final slope ($\mu\text{g/ml min}$)	Intercept ($\mu\text{g/ml}$)	k_t (per min)	k_r (per min)
125-180(μm)	0,154 \pm 0,001	0,108 \pm 0,001	0,980 \pm 0,096		0,0737 \pm 0,006
180-250(μm)	0,155 \pm 0,004	0,111 \pm 0,001	0,369 \pm 0,068		0,2019 \pm 0,027
250-355(μm)	0,145 \pm 0,001	0,104 \pm 0,002	0,801 \pm 0,065		0,0787 \pm 0,001
>355(μm)	0,167 \pm 0,003	0,111 \pm 0,001	1,339 \pm 0,085		0,0638 \pm 0,001
DP		0,082 \pm 0,001	0,291 \pm 0,034	0,00030	

While P3b sample had the highest standard deviation among all examined P3 samples, P3c fraction showed the most uniform dissolution (with the lowest standard deviation).

Intrinsic dissolution profiles of different fractions were compared by one-way ANOVA and no significant difference was observed. Because the solubility of the anhydrous form is difficult to measure, the initial part of the intrinsic dissolution curve was used to predict this parameter. In the case where the slopes of different fractions of the same samples were used for calculation, the value obtained for the solubility was found to vary. Solubility of sample P3 calculated from results of P3c and P3d was 486.3 and 560.4 $\mu\text{g/ml}$ respectively, but when calculated from results of P3a and P3b samples, solubility was found to be approximately the same (516.1 and 519.5 $\mu\text{g/ml}$). Consequently, the results for IDR varied from 70.6 to 93.7 $\mu\text{g/min/cm}^2$ in case of samples P3c and P3d respectively, and 79.7 and 80.6 $\mu\text{g/min/cm}^2$, for samples with smaller particle size, see table 6.22.

Table 6.22 Intrinsic dissolution rate of different fraction of CBZ P3

Sample	Solubility estimated ($\mu\text{g/ml}$) \pm SD	IDR ($\mu\text{g/min/cm}^2$) \pm SD
P3a 125-180(μm)	516,1 \pm 3,40	79,69 \pm 1,03
P3b 180-250(μm)	519,5 \pm 13,4	80,55 \pm 4,16
P3c 250-355(μm)	486,3 \pm 3,40	70,56 \pm 0,97
P3d >355(μm)	560,4 \pm 10,1	93,71 \pm 3,36

CBZ P (fractions)

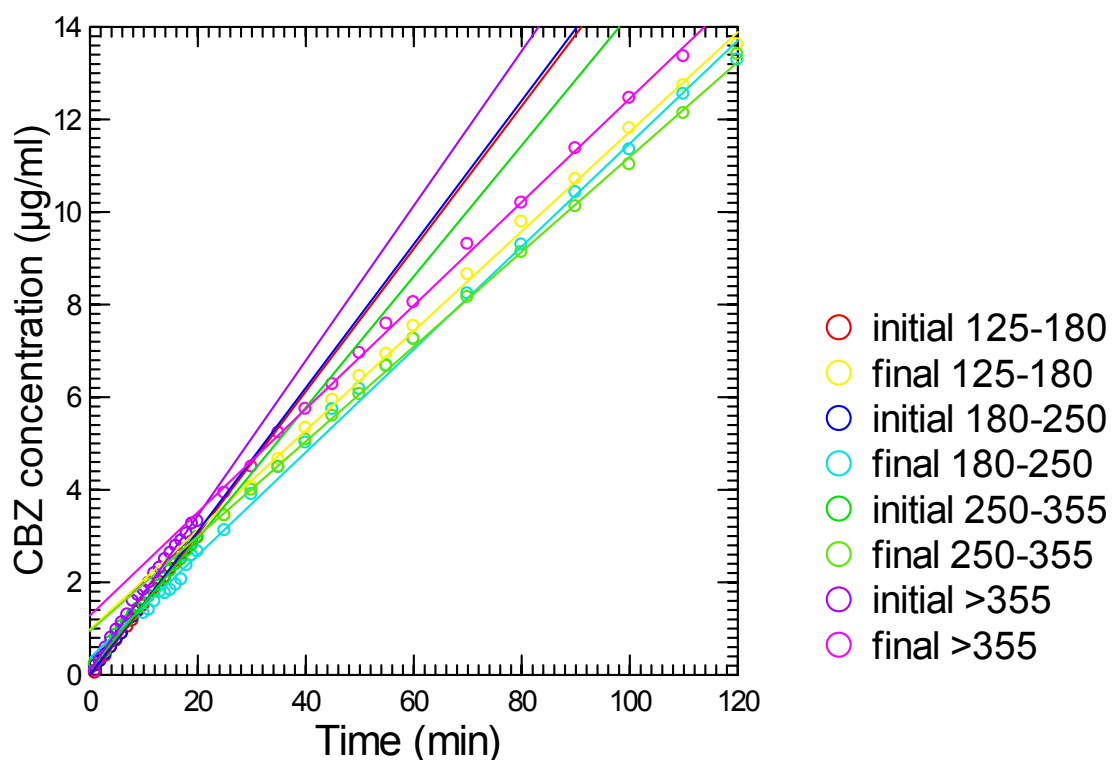


Figure 6.42 Intrinsic dissolution profiles of different P3 fraction calculated by Systat software

Thus it may be concluded that in case of CBZ, the particle size distribution can have an effect on the accurate estimation of solubility and determination of intrinsic dissolution rate of examined samples. Intrinsic dissolution profiles are presented in figure 6.42. Although the intrinsic dissolution method is assumed to reduce the effect of particle size on dissolution, when the material tends to express polymorphism or pseudopolymorphism, the effect of particle size should be considered as a possible source of error when performing accurate IDR studies.

6.4. Binary mixtures

Influence of excipients on the solution mediated transformation of CBZ anhydrate to dihydrate was investigated by many researchers (Hirasawa et al., 1999, Koester et al., 2003, Moneghini et al., 2001, Nair et al., 2002, Otsuka et al., 2000, Rodriguez-Hornedo et al., 2004, Tian et al., 2007) .

The final purpose of this CBZ study was aimed to investigate CBZ formulation prepared with different CBZ samples on dissolution behavior. Prior to that investigation, the behavior of CBZ in binary mixtures was analyzed. Lactose α -monohydrate for direct compression was selected as excipient because lactose is the most represented in the co-processed excipient Ludipress, which was planned to be used in the final formulations, see table 6.23 and figure 6.43. Lactose α -monohydrate for direct compression (spray dried Fast Flo[®] lactose) in comparison with α -lactose monohydrate has improved binding, flow and compaction properties. It consists mainly of spherical particles of α -lactose monohydrate which are glued together with amorphous lactose (responsible for better binding and compactibility properties). Spray dried lactose contains around 5% of moisture content, mainly bonded as crystal water.

Table 6.23 Characterization of Fast Flo[®] lactose

Sample (n=5)	Particle size distribution (μm)			True density (g/cm^3)	Loss on drying (%) 105°C, 2h
	d (0.1)	d (0.5)	d (0.9)		
Fast Flo lactose	< 45,70	<111,16	<209,75	1.564 \pm 0.004	3.8 \pm 0.0

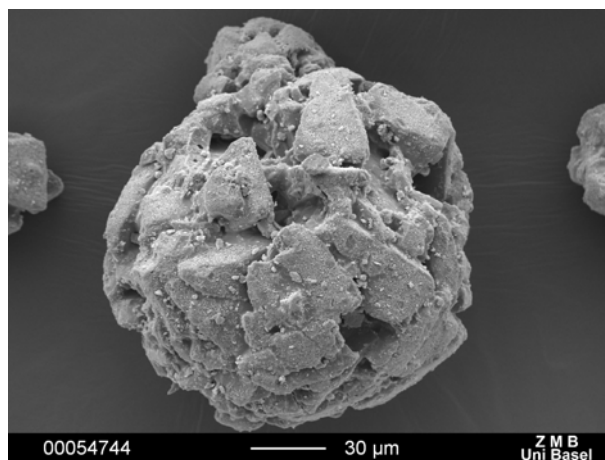
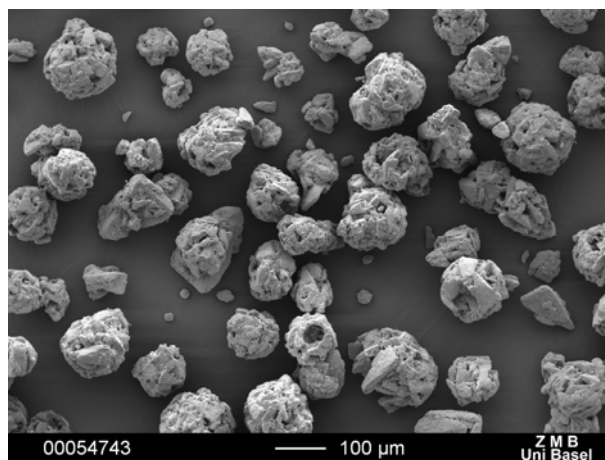


Figure 6.43 SEM pictures of Fast Flo[®] lactose

Preparation of tablets of binary mixtures with constant porosity for different mixture compositions (from mixture compositions see 5.2.3.1.) required changing the range of applied compaction force from 8 to 14kN in the case of CBZ B and P and from 10-16kN for binary mixtures with CBZ A and D. This increment of applied compaction force depended on the quantity of lactose in the mixture – for compacts containing higher amount of lactose, higher compaction force was required in order to have compacts with approximately the same porosity.

6.4.1. Disintegration of binary mixtures

Disintegration test was carried out on the mixtures 6, 7, 8 and 9 (the amount of CBZ was 40%, 30%, 20% and 10% respectively). Considering that lactose α -monohydrate has no disintegrating properties, it was impossible to measure disintegration time on the mixtures containing higher concentration of CBZ where no disintegration occurred. Mixture 6 from all CBZs disintegrated in more than 4 hours, and was excluded from the results presented in table 6.24. Logical tendency of having faster disintegration time by increasing the amount of excipient from mixture 7 to mixture 9 was present in all analyzed samples. However some discrepancies among binary mixture prepared from different CBZ were found. While in the case of mixtures 9 and 8 of CBZ A and CBZ B, compact disintegrated in 1 – 3 minutes, in the case of CBZ P for the same mixtures they disintegrated only after 9 to 10 minutes. In the case of CBZ P mixtures, although decreasing trend of disintegration time was found as in the others, variations in disintegration time between mixture 7, 8 and 9 were very small, see table 6.24 and figure 6.44.

Table 6.24 Disintegration time of compacts stored at 55% of relative humidity

Samples (n=6) (RH 55%)	Disintegration time (s)		
	Mix 7	Mix 8	Mix 9
CBZ A	4143 \pm 322	168 \pm 19	65 \pm 3
CBZ B	8282 \pm 194	126 \pm 37	47 \pm 6
CBZ P	754 \pm 120	575 \pm 75	534 \pm 48
CBZ D	4312 \pm 100	1358 \pm 77	181 \pm 24

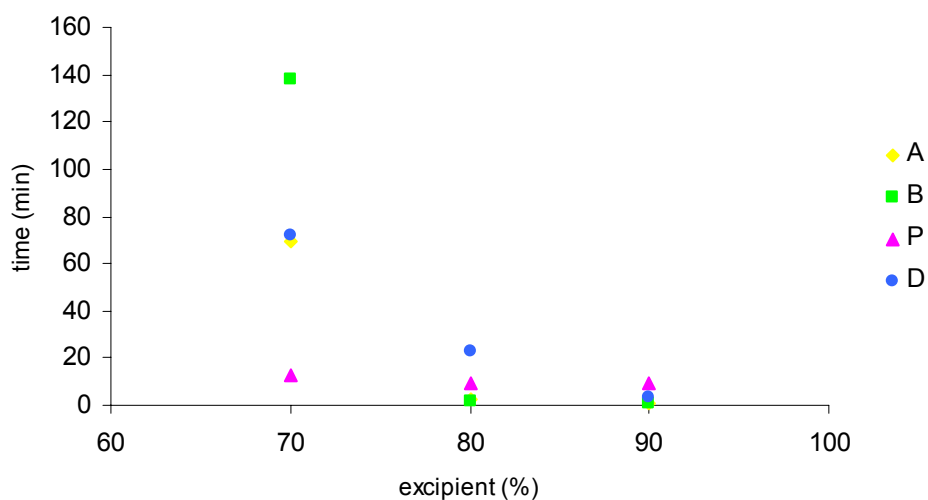


Figure 6.44 Disintegration time of compacts stored at 55% of relative humidity

Differences in disintegration time of examined mixtures are probably results of different morphology and particle size distribution between CBZ A, B and P. These results confirmed clearly the importance of raw material selection.

The effect of storage condition on disintegration time of tablets was studied at two different conditions of relative humidity. Generally it was noticed that upon storing the compacts of binary mixtures under higher humidity, the disintegration time increased, in other words longer time was required for the compacts to disintegrated. Mixtures of Fast Flo[®] lactose and CBZ dihydrate showed the longest disintegration time, which may lead to the conclusion that prolonged disintegration in samples stored at 85%RH was caused probably because during storage some anhydrous carbamazepine converted to CBZ dihydrate. The results are presented in table 6.25 and figure 6.45.

Table 6.24 Disintegration time of compacts stored at 55% of relative humidity

Samples (n=6) (RH 85%)	Disintegration time (s)		
	Mix 7	Mix 8	Mix 9
CBZ A	5636 ± 289	2541 ± 127	769 ± 72
CBZ B	7731 ± 114	3045 ± 52	1233 ± 234
CBZ P	4121 ± 172	1756 ± 39	412 ± 19
CBZ D	8195 ± 266	3145 ± 48	770 ± 103

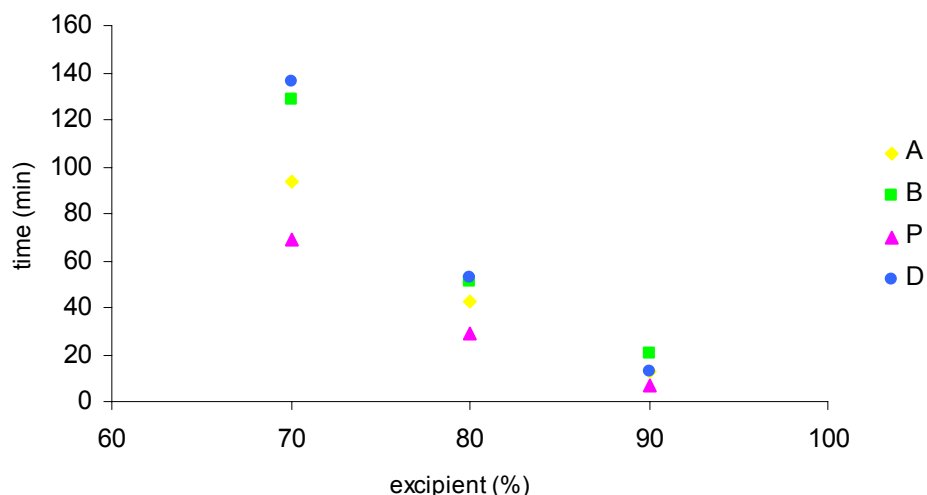


Figure 6.45 Disintegration time of compacts stored at 85% of relative humidity

Mixtures 1 to 5 (90 to 50 % of CBZ) did not show any tendency to disintegrate, which is important information for the following intrinsic dissolution tests.

6.4.2. Intrinsic dissolution rate of binary mixtures

Intrinsic dissolution behavior of CBZ in binary mixtures with Fast Flo[®] lactose was investigated in order to see if this specific excipient has any influence on intrinsic dissolution properties of active ingredient. In the case of mixtures 7, 8 and 9 which contained 70, 80 and 90% w/w of Fast Flo[®] lactose respectively, disintegration of the compact occurred. Because of the difficulty of keeping constant the area of the dissolving compact, the results of mixtures 7, 8 and 9 were not discussed.

In the case of pure CBZ, formation of CBZ dihydrate on the compacts surfaces slowed down the dissolution rate. During the intrinsic dissolution test of binary mixtures, the excipient was dissolving in the dissolution media with the time, and it can be assumed that, from time to time, new “untouched” particles of anhydrous CBZ were uncovered to be exposed to dissolution medium, accelerating the dissolution rate. This may be the reason why the amount of dissolved CBZ was not decreasing proportionally with the decreasing amount of the active in the binary mixtures.

Compacts after dissolution are presented in the following pictures, figure 6.46 and 6.47.

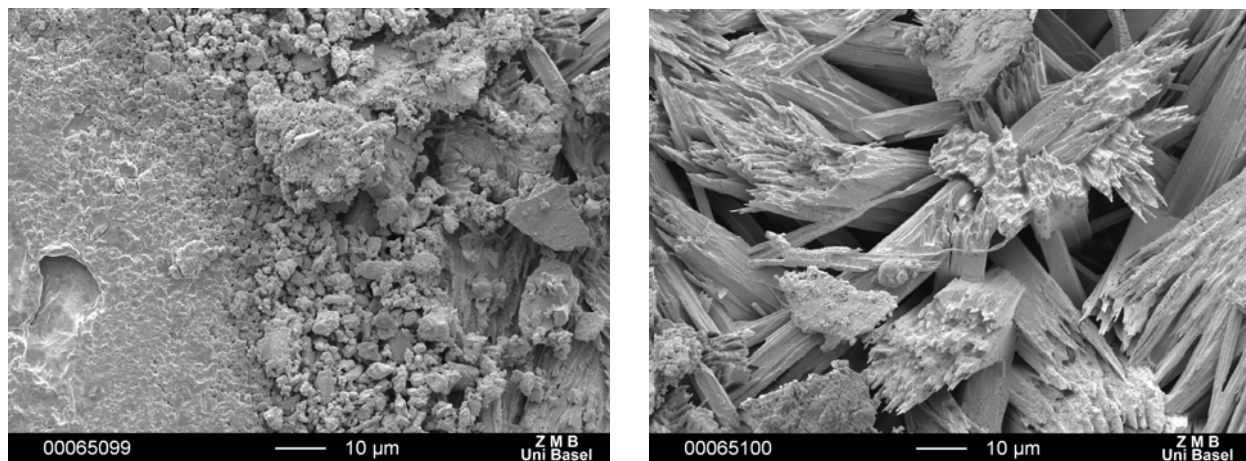


Figure 6.46 Mixture 3 CBZ P after intrinsic dissolution (70% CBZ P and 30% lactose Fast Flo[®])

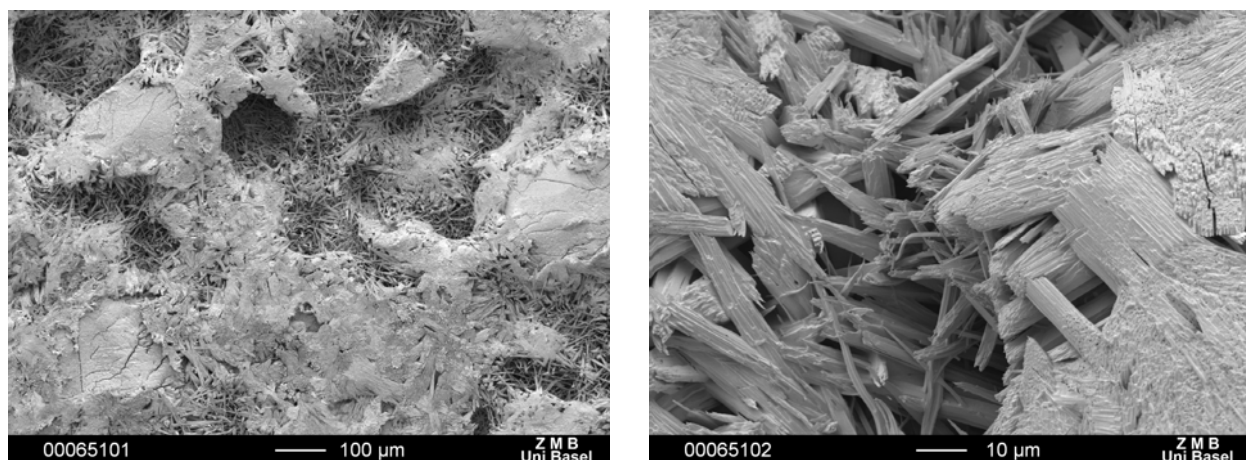


Figure 6.47 Mixture 4 CBZ P after intrinsic dissolution (60% CBZ P and 40% lactose Fast Flo[®])

The average value for IDR was determined by testing 5 tablets of each binary mixture (see table 6.25 and 6.26). In order to compare the obtained results only the initial part of the intrinsic dissolution rate was evaluated, which was considered to be the dissolution of anhydrous form. Fragmentation of intrinsic dissolution curve was done by Systat software, and the transition point was determined by splitting the data in such a way that linear regression lines for each segment resulted in the best correlation coefficient.

It was previously determined that CBZ A anhydrous convert to dihydrate in 20 minutes during the intrinsic dissolution, CBZ B in approximately 15 minutes, while for CBZ P this period was between 20 and 25 minutes. In the case of the binary mixtures, the time required for the transition varied for different mixtures.

At the storage condition of 55%RH, for CBZ A in all mixtures conversion to dihydrate was first noticed to be between 11 and 18 minutes; for CBZ B it was found to be between 13 and 15 minutes and for CBZ P between 17 and 25 minutes. It means that in case of CBZ B conversion to dihydrate in binary mixtures was at least influenced by the presence of excipients. At the storage conditions of 85%RH in all cases less time was required for conversion of anhydrous part to dihydrate, probably because during storage, the transformation partially already occurred, thus there was less anhydrate left to be converted. Transition time in binary mixtures after storage was found to be for CBZ A between 14 and 15 minutes, for CBZ B between 8 and 15 minutes and for CBZ P between 10 to 12 minutes.

Table 6.25 IDR of CBZ mixtures stored at 55%RH (in brackets is conversion time in minutes)

Sample	CBZ A IDR ($\mu\text{g}/\text{min}/\text{cm}^2$)	CBZ B IDR ($\mu\text{g}/\text{min}/\text{cm}^2$)	CBZ P IDR ($\mu\text{g}/\text{min}/\text{cm}^2$)	CBZ D IDR ($\mu\text{g}/\text{min}/\text{cm}^2$)
CBZ	70.4 \pm 1.9 (20)	79.6 \pm 3.5 (15)	67.4 \pm 1.8 (25)	47.8 \pm 0.3
Mix 1	73.4 \pm 2.9 (18)	103.8 \pm 6.9 (18)	42.8 \pm 2.7 (25)	23.0 \pm 1.9
Mix 2	96.7 \pm 4.3 (18)	80.3 \pm 4.6 (13)	45.1 \pm 2.5 (17)	29.8 \pm 0.7
Mix 3	80.8 \pm 3.1 (18)	60.3 \pm 2.9 (15)	56.1 \pm 4.3 (15)	30.1 \pm 0.9
Mix 4	80.9 \pm 4.2 (11)	55.6 \pm 3.7 (15)	51.3 \pm 3.6 (20)	43.8 \pm 0.9
Mix 5	98.7 \pm 3.6 (11)	56.6 \pm 2.5 (14)	53.2 \pm 2.3 (18)	59.6 \pm 1.2
Mix 6	74.4 \pm 4.9 (11)	67.1 \pm 1.9 (14)	48.0 \pm 3.7 (18)	48.1 \pm 1.3

Table 6.26 IDR of CBZ mixtures stored at 85%RH (in brackets is conversion time in minutes)

Sample	CBZ A IDR ($\mu\text{g}/\text{min}/\text{cm}^2$)	CBZ B IDR ($\mu\text{g}/\text{min}/\text{cm}^2$)	CBZ P IDR ($\mu\text{g}/\text{min}/\text{cm}^2$)	CBZ D IDR ($\mu\text{g}/\text{min}/\text{cm}^2$)
Mix 1	62.0 \pm 1.6 (15)	81.8 \pm 2.6 (11)	63.7 \pm 1.9 (12)	32.5 \pm 1.4
Mix 2	62.0 \pm 1.3 (14)	65.5 \pm 2.9 (18)	42.4 \pm 2.1 (12)	28.7 \pm 1.7
Mix 3	52.5 \pm 1.5(25)	68.7 \pm 1.9 (11)	53.2 \pm 2.6 (10)	26.2 \pm 1.8
Mix 4	55.1 \pm 1.7(14)	77.1 \pm 2.7 (8)	45.6 \pm 1.8 (12)	33.9 \pm 2.1
Mix 5	78.8 \pm 3.9(15)	75.1 \pm 3.5 (10)	49.0 \pm 3.2 (12)	28.4 \pm 1.9
Mix 6	59.0 \pm 4.1(15)	66.2 \pm 2.4 (11)	49.9 \pm 2.6 (20)	46.5 \pm 2.4

Generally, it may be noticed that after keeping compacts at the condition with higher humidity, IDR was lower than IDR of the same compacts stored at 55%RH, and standard deviation during dissolution decreased as well. This may lead to a conclusion that during the storage, at the surface of the compact which later was exposed to dissolution media, partial conversion to dihydrate occurred. IDR for examined mixtures is plotted against the amount of excipients in the figures 6.48. At 55%RH CBZ A mixtures 2 and 5 (with 20 and 50% of lactose) showed higher IDR than the other mixtures. CBZ B mixtures showed the tendency of decreasing IDR with increasing amount of excipients, with mixture 1 having the highest IDR. In the case of CBZ P, IDR was not affected by the amount of excipient present in the mixtures and it was almost constant in all investigated mixtures.

The results of the present work are in agreement with literature data (Hirasawa et al., 1999). Hirasawa et al were investigating CBZ and lactose monohydrate in binary mixtures and solid dispersions and they found that in binary mixtures the amount of dissolved CBZ is not affected by lactose presence, like in case of solid dispersion.

Lactose and carbamazepine solid can make a solid dispersion, by completely melting lactose, adding CBZ and subsequently rapid solidification. In solid dispersion, degree of crystallinity of CBZ is decreased and dissolution rate of drug is improved. In solid dispersion, there is reaction between the carbonyl group in the lactose and primary amide group of CBZ (Maillard reaction). Hirasawa et al. proved that in binary mixtures of CBZ and lactose, there is no influence of excipient on the release of CBZ, and the structure and crystallinity of active material are not affected by the presence of this excipient (Hirasawa et al., 1999).

The IDR of the samples stored at 55% for 2 weeks did not decrease with amount of excipients present in the mixtures, which means that lactose has no negative influence on the CBZ anhydrate to dihydrate transformation. IDR of tablets stored at 85% RH decreased probably because CBZ anhydrous at the surface of the compact was partially converted to dihydrate (the standard deviation was decreased as well which is another indication for the dihydrate formation).

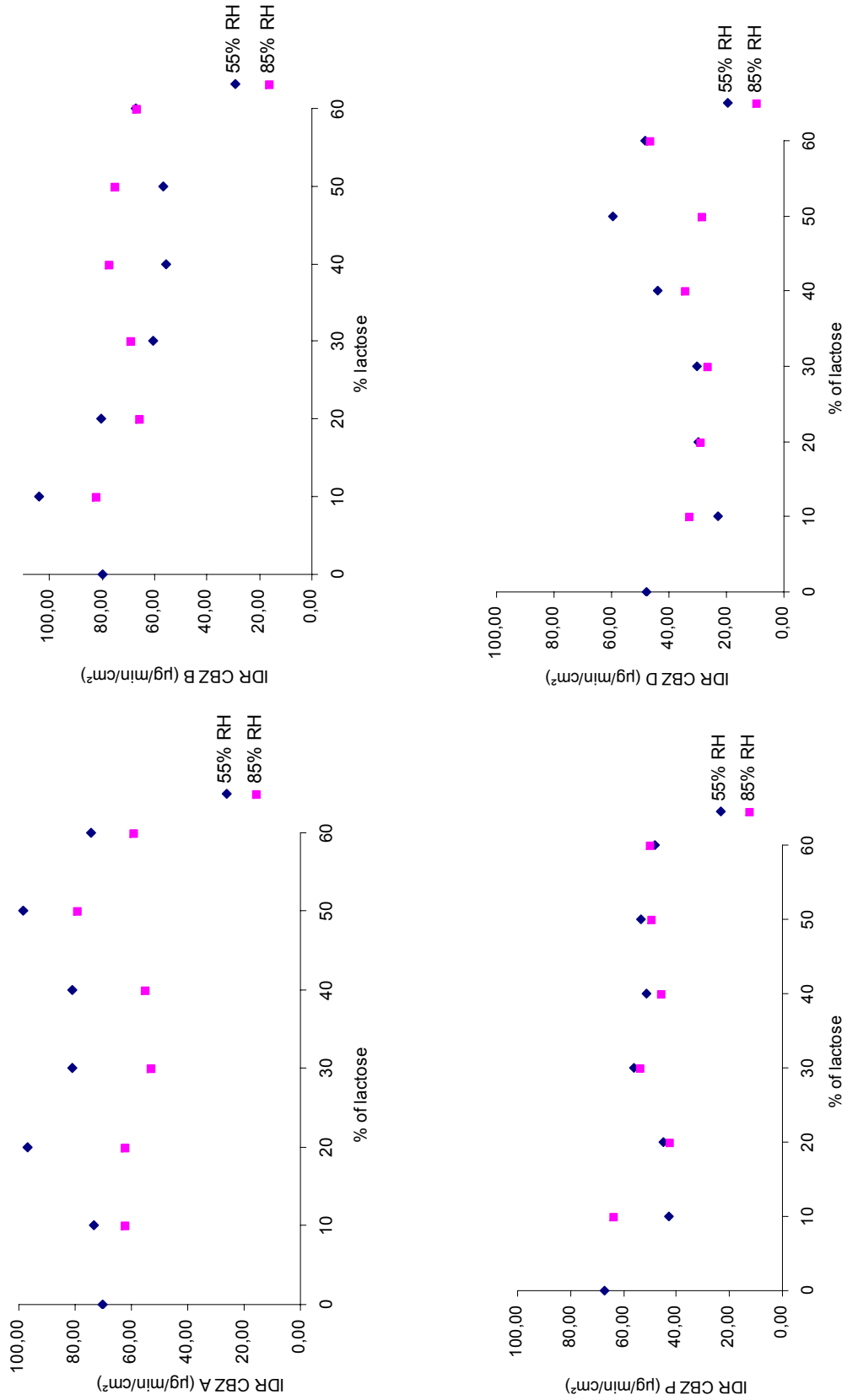


Figure 6.48 IDR vs. excipient content for CBZ A, B, P and D

However, lactose as excipients has no influence on the anhydrate dihydrate conversion. The amount of drug dissolved during the intrinsic dissolution test was increasing with the increased amount of lactose in the mixtures, simply because during the dissolution lactose was dissolving and new parts of anhydrous CBZ were exposed to dissolution media.

It is relevant to notice that tablets which coincidentally remained more than 4 weeks at conditions of 85% of RH (mixtures contained 60% of lactose and more) showed discoloration on their surfaces i.e. browning, which is probably caused by reaction of lactose and the amide group of CBZ.

6.5. Carbamazepine formulations

Carbamazepine presents formulation challenges due to its inherent poor compressibility and compactibility, high dose and low water solubility. The wet granulation process may be utilized to improve the flow and compression/compaction properties of the formulation. However, during wet granulation, if combination of ethanol and water was used, the solution-mediated transformation of CBZ occurs (Otsuka et al., 1999, Otsuka et al., 1997) and the amount of dihydrate formed during this process may be appreciable. In that case, during the drying process, dihydrate may convert back to initial form III, or eventually may convert in form I, thus a mixture of form I and III is created and that will influence on the dissolution process of the final product. If only aqueous solution is used, whole process has to be carefully controlled to insure that phase transformation does not occur. Therefore CBZ is a good example to illustrate how a wrong choice of the manufacturing process, may lead to an increased phase transformation, processing difficulties and problems with dissolution.

In order to avoid the possible phase transformation of CBZ, for this study direct compaction was chosen as process for producing CBZ tablets for this study, and therefore a co-processed excipient for direct compaction Ludipress[®] was selected.

Co-processed excipients are prepared by incorporating one excipient into the particle structure of another excipient by appropriate processes such as co-drying. Thus, they are simple physical mixtures of two or more existing excipients mixed at the particle level. Co-processing of excipients leads to the formation of excipient granulates with

superior properties compared with physical mixtures of components or with individual components. They have been developed primarily to address the issues of flowability, compressibility, and disintegration potential, with filler–binder combinations being the most commonly tried (Gohel, 2005). During the preparation of tablets, porosity was kept constant (see 5.2.3.2.). The only parameter set on Presster™ was the gap, and it is presented for each formulation, together with the measured compaction force, thickness of the tablets and calculated porosity in the following table 6.27.

Table 6.27 Settled gap in Presster™, obtained compaction force, and porosity of tablets

Sample (n=12)	Gap (mm)	Compaction (kN)	Thickness (mm)	Porosity (%)
formulation USP	2,85	9.5-10.9	3,62 ± 0,02	12,55 ± 0,62
formulation A	2,75	11.4-12.4	3,57 ± 0,01	12,71 ± 0,47
formulation B	2,85	9.6-9.8	3,59 ± 0,01	12,78 ± 0,29
formulation P	2,85	9.3-9.9	3,59 ± 0,02	12,75 ± 0,41
formulation D	2,90	8.7-10.1	3,64 ± 0,03	12,51 ± 0,75

Crushing strength test on the tablets was carried out. As it was already confirmed, compactibility properties of CBZ were improved in the case of CBZ dihydrate, consequently, formulation D had the highest hardness of the tablets ($132 \pm 4\text{N}$), see table 6.28. Regarding the commercial samples, the highest crushing strength of $105 \pm 5\text{N}$ was measured in the formulation A while for formulations B and P the crushing strengths were of $79 \pm 3\text{N}$ and $77 \pm 1\text{N}$, respectively. Differences in the found values are caused most probably by the differences in the morphological properties of commercial CBZ samples.

Table 6.28 Crushing strength and disintegration time

Sample (n=*3;**6)	Crushing strength* (N)	Disintegration time** (s)
formulation USP	90 ± 10	77 ± 15
formulation A	105 ± 5	14 ± 3
formulation B	79 ± 3	24 ± 4
formulation P	77 ± 1	24 ± 6
formulation D	132 ± 4	110 ± 20

On the other hand, disintegration time was longer for formulation B and P (24 ± 4 s and 24 ± 6 s respectively) than for formulation A (14 ± 3 s). It was expected that the harder tablet will need more time to disintegrate, but it was not the case for anhydrous samples. Formulation D had the longest disintegration time, due to the highest hardness of these tablets.

Dissolution of CBZ formulations was conducted according to USP monograph for the CBZ immediate release tablets (USP31, 2008). Six tablets were examined per all formulations. The apparatus and the method used were described previously (see 5.2.3.5.). The requirements for the time and tolerance for CBZ drug release in USP pharmacopoeia are the following:

- 45 – 75% of drug has to be dissolved in the first 15min
- >75% of drug has to be dissolved in 60min.

The first range is the critical one and a lot of previously investigated CBZ formulations failed to meet that requirement during the dissolution test.

According to USP monograph for CBZ, immediate release tablets will meet requirements if the dissolved amount of drug agrees with the interpretations specified in the Acceptance table 2 in USP pharmacopoeia (table 6.29).

For CBZ immediate release tablets the following exceptions are allowed:

- At 15 minutes: at L_2 , no unit is more than 5% outside the stated range; at L_3 , no unit is more than 10% outside the stated range; and not more than 2 of the 24 units are more than 5% outside the stated range;
- At 60 minutes at L_2 , no unit is less than $Q - 5\%$; at L_3 , no unit is less than $Q - 10\%$; and not more than 2 of the 24 units are less than $Q - 5\%$.

L_1 or L_2 are limits of the amounts of active ingredients dissolved and are expressed in terms of the percentage of labeled content of the dosage unit, and Q value is the amount dissolved at each specified fractional dosing interval specified in individual

monograph expressed as a percentage of the labeled content of the dosage unit (USP31, 2008).

Table 6.29 Acceptance table 2 from USP

Level	Number Tested	Criteria
L_1	6	No individual value lies outside each of the stated ranges and no individual value is less than the stated amount at the final test time.
L_2	6	The average value of the 12 units ($L_1 + L_2$) lies within each of the stated ranges and is not less than the stated amount at the final test time; none is more than 10% of labeled content outside each of the stated ranges; and none is more than 10% of labeled content below the stated amount at the final test time.
L_3	12	The average value of the 24 units ($L_1 + L_2 + L_3$) lies within each of the stated ranges, and is not less than the stated amount at the final test time; not more than 2 of the 24 units are more than 10% of labeled content outside each of the stated ranges; not more than 2 of the 24 units are more than 10% of labeled content below the stated amount at the final test time; and none of the units is more than 20% of labeled content outside each of the stated ranges or more than 20% of labeled content below the stated amount at the final test time.

In the first 15 minutes all 6 examined tablets of formulation A met the USP requirements (dissolved amount was in range from 67.5 until 74.7%). It may be emphasized that two tablets almost reached the upper limit (by dissolving 73.15% and 74.67% of drug). The variation (correlation coefficient) was at maximum 4.58%. After 60 minutes, the percentage of dissolved CBZ was 94.9-100.0%.

Dissolution profile of formulation A is presented in the following figure 6.49.

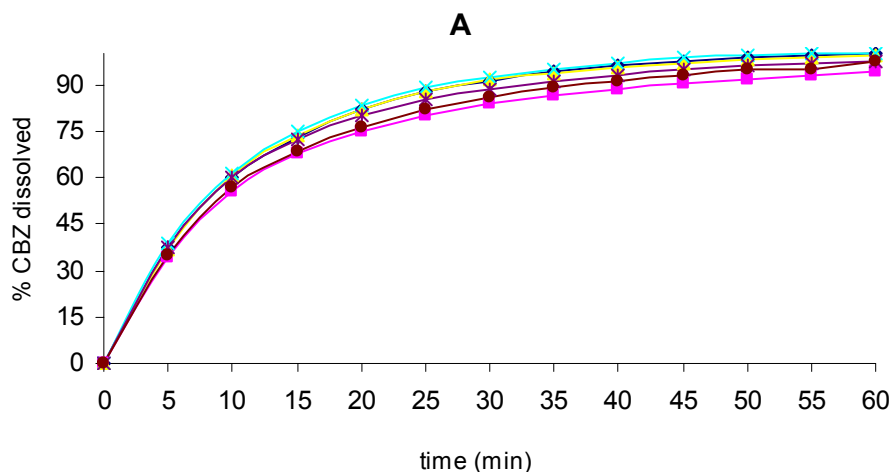


Figure 6.49 Dissolution profile of formulation A

Formulation B did not pass the first criteria of acceptance of dissolution, because more than 75% of drug was released. Actually, in the first 15 minutes dissolved carbamazepine was in the range between 70.7 and 79.2%, and two of six examined tablets which failed the requirement were dissolved between 78.61% and 79.19%. If dissolution was continued in the next step, considering the L_2 limit, the results would probably meet the requirement (because the variation was lower than 5% allowed). Correlation coefficient during the dissolution was at maximum of 5.61%. After 60 minutes, the percentage of dissolved CBZ was between 95.1 and 99.6%. Dissolution profile of formulation B is presented in figure 6.50.

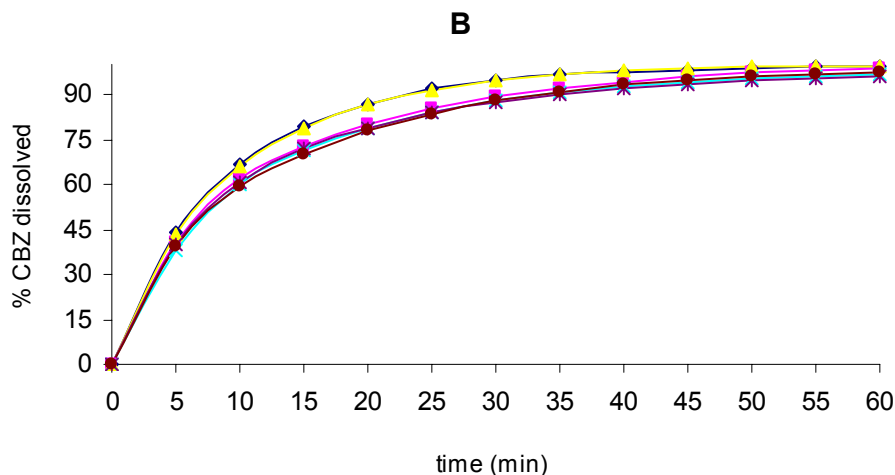


Figure 6.50 Dissolution profile of formulation B

Formulation P has showed the highest variation especially in the first 15 minutes where the correlation coefficient was 11.8%. This formulation had the lowest amount dissolved in the first 15 minutes which was within 53.2 and 66.9%, thus it met the USP requirements. After 60 minutes, within 86.3 and 100% of carbamazepine was dissolved. Dissolution profile of formulation P is presented in the figure 6.51.

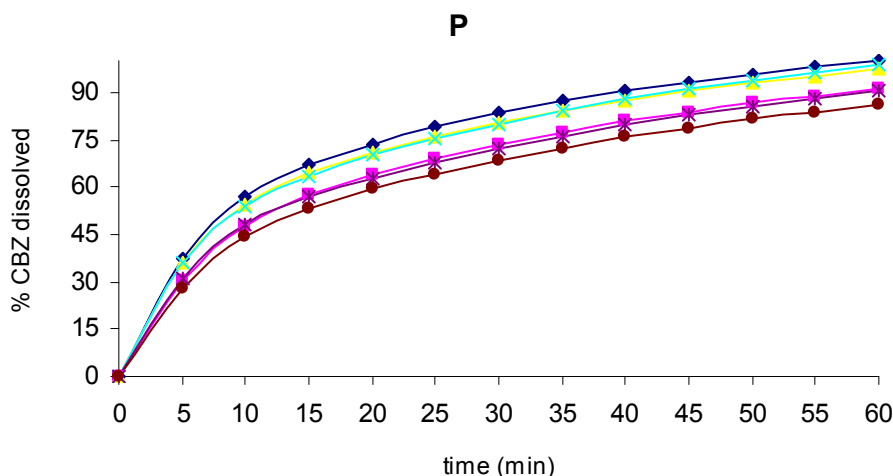


Figure 6.51 Dissolution profile of formulation P

Formulation made with USP CBZ showed the fastest dissolution, caused by micronized particles of USP standard, while the dissolution with CBZ dihydrates was the slowest because of the lower solubility of carbamazepine dihydrate but with the smallest variation within 6 examined tablets. During the first 15 minutes only $15 \pm 2.5\%$ of CBZ from formulation D was dissolved, and in 60 minutes the amount of measured drug in the dissolution media was $71.2 \pm 1.2\%$. The findings for CBZ dihydrate are in agreement with our previous statement, which means that although compactibility properties of the drug were improved and dissolution behavior was more uniform, the solubility of the drug decreased and this caused decrease in amount of drug dissolved.

Considering that in this study the same excipients were used in the preparation of formulations, the variation found in the formulation A, B and P are caused only by differences in the CBZ sample which was used.

Intrinsic dissolution behavior of examined carbamazepines showed differences in the phase transformation, and it was found that for CBZ B, the transition point is around 15min, for CBZ A around 20 minutes, and for CBZ P between 20 and 25 minutes. If direct compaction is the process which is used, all possible phase transitions during the manufacturing of CBZ dosage forms are avoided and CBZ should keep its intrinsic properties. In that case, using intrinsic dissolution it is possible to predict the dissolution behavior of CBZ in formulation. Intrinsic dissolution behavior of the drug may be one of the critical parameters during the preformulation study of CBZ.

Dissolution profiles were compared and presented in the following figure 6.52.

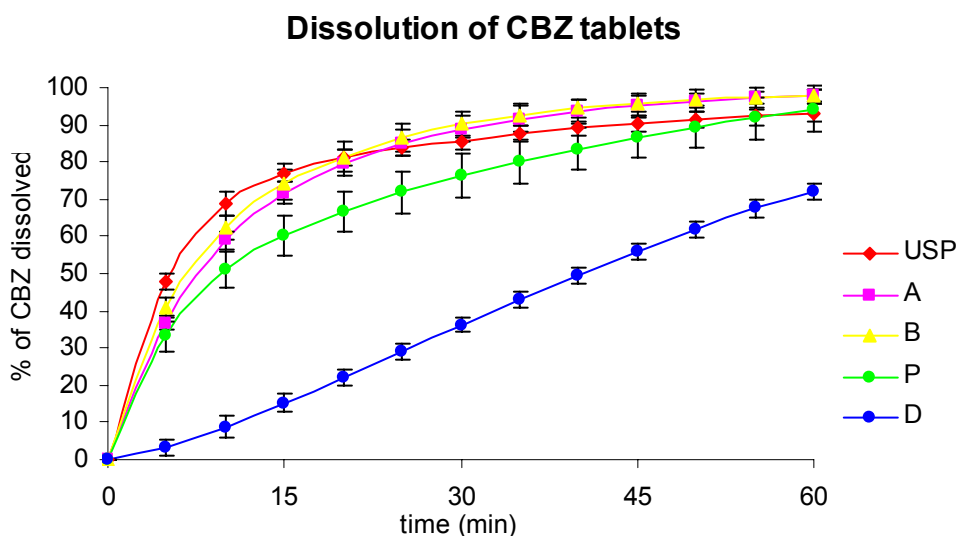


Figure 6.52 Dissolution profile of all formulation

7. Conclusions

Understanding variations in the characteristics of raw material during preformulation stage is necessary in order to ensure reproducibility of results, and correctly predict the cause of eventual instability or poor performance of a dosage form. One of the tasks of preformulation studies is defining the critical parameters which influence the product quality and furthermore to suggest a method to monitor it during development of a product.

The aim of this work was to suggest a robust formulation for CBZ immediate release tablets under the frame of PAT initiative, by building the quality into the product. For that purpose, carbamazepine raw material provided from three different sources, was fully investigated.

The first step in this study was to identify the polymorphic form of the available samples in order to approve or exclude the possibility of having pure starting material.

After characterization by thermal analysis, X-ray, and FTIR, nine analyzed samples of anhydrous CBZ obtained from different sources, were shown to exhibit the same polymorphic form (form III). Nevertheless, in the further investigation was found that CBZ anhydrous samples exhibited different morphology, had different particle size and size distribution all of which led to a variation in solubility and in the intrinsic dissolution behavior. The found variations were suggested to be attributed to various manufacturing processes most likely resulting from different solvents used in the crystallization process and drying and/or grinding regimes in the final stage of the manufacture of CBZ.

Investigated samples varied as well in particle size distribution. In order to compare their properties, intrinsic dissolution tests were conducted with samples containing the same particle size fraction. CBZ A, B and P showed different intrinsic dissolution behavior, and moreover for each sample exhibited different transition point for the transformation of anhydrous to dihydrate form.

This lead to the conclusion that selecting just a stable and pure polymorphic starting material is not alone the solution to assure the constant quality of a product, because

polymorphs can exist in different habits which can influence dissolution or stability of the final dosage form. Therefore, critical parameters for CBZ formulation which may assure the desired quality of the product beside the polymorphic form are particle size, size distribution and morphology.

All of these critical characteristics had an effect on the intrinsic dissolution behavior of CBZ and thus the intrinsic dissolution test is suggested as a valuable and simple monitoring tool. It also can be used for determination of anhydrous to dihydrate transition point for CBZ and therefore for prediction of CBZ behavior in the final dosage form.

During this study, properties of CBZ dihydrate were examined. As commercial samples were converted to CBZ dihydrate form, variations in solubility, thermal and intrinsic dissolution behavior were significantly reduced from batch to batch and within one sample. Due to the lower solubility of dihydrate, dissolution rate was decreased in comparison with dissolution of anhydrous form and this factor must be considered for the bioavailability of CBZ.

7.1. How to avoid problems with CBZ?

By determining the transition point of phase transformation of anhydrous to dihydrate CBZ, it became possible to predict the dissolution behavior. There are two possible strategies suggested at the raw material level in order to decrease the variability and improve constant dissolution of CBZ formulation:

- To control synthetic pathway of raw material and to keep it constant with no variation in order to produce the specific particle size (narrow distribution) and desired morphology of crystal which can help to control the dissolution (CBZ A to CBZ D transformation steps)
- To delete the prehistory of the active material by converting it to dihydrate form prior to formulation, in order to have a constant dissolution rate with less variation (this step then requires the improvement of solubility of dihydrate itself by co-crystallization or other methods).

7.2. Suggestions for a robust CBZ formulation

Information about the transition point of CBZ anhydrous to dihydrate form is important for selection of excipients and process which will be used for the CBZ final dosage form. This is especially important because the USP requires a dissolution of 45-75% after 15 min and >75% after 60 min. As the excipients play a key role in CBZ phase transformation from anhydrous to dihydrate form, they should be selected carefully on the base of all available information. In this respect, if CBZ raw material exhibit fast anhydrous to dihydrate transition point, then excipients which are capable of increasing the phase transition point of CBZ should be selected in order to meet the USP requirements.

Decisions regarding the process to be used for the preparation of CBZ immediate release tablets are also directly dependent on the properties of CBZ raw material.

Wet granulation can be a good solution for CBZ which has fast anhydrous to dihydrate transformation, because using that process the kinetic of transition can be decreased and thus the transition point is increasing. But it has to be taken into account that in every step of wet granulation process, polymorphic changes which are likely to occur, have to be controlled and monitored to assure that final product will have constant release of drug.

On the other hand, to avoid any polymorphic modification, then direct compaction should be the process of choice. In order to keep the dissolution rate constant, it is recommended to use starting material with narrow particle size distribution and furthermore with constant morphology.

Any exchange of CBZ raw material will most probably require development of a new formulation.

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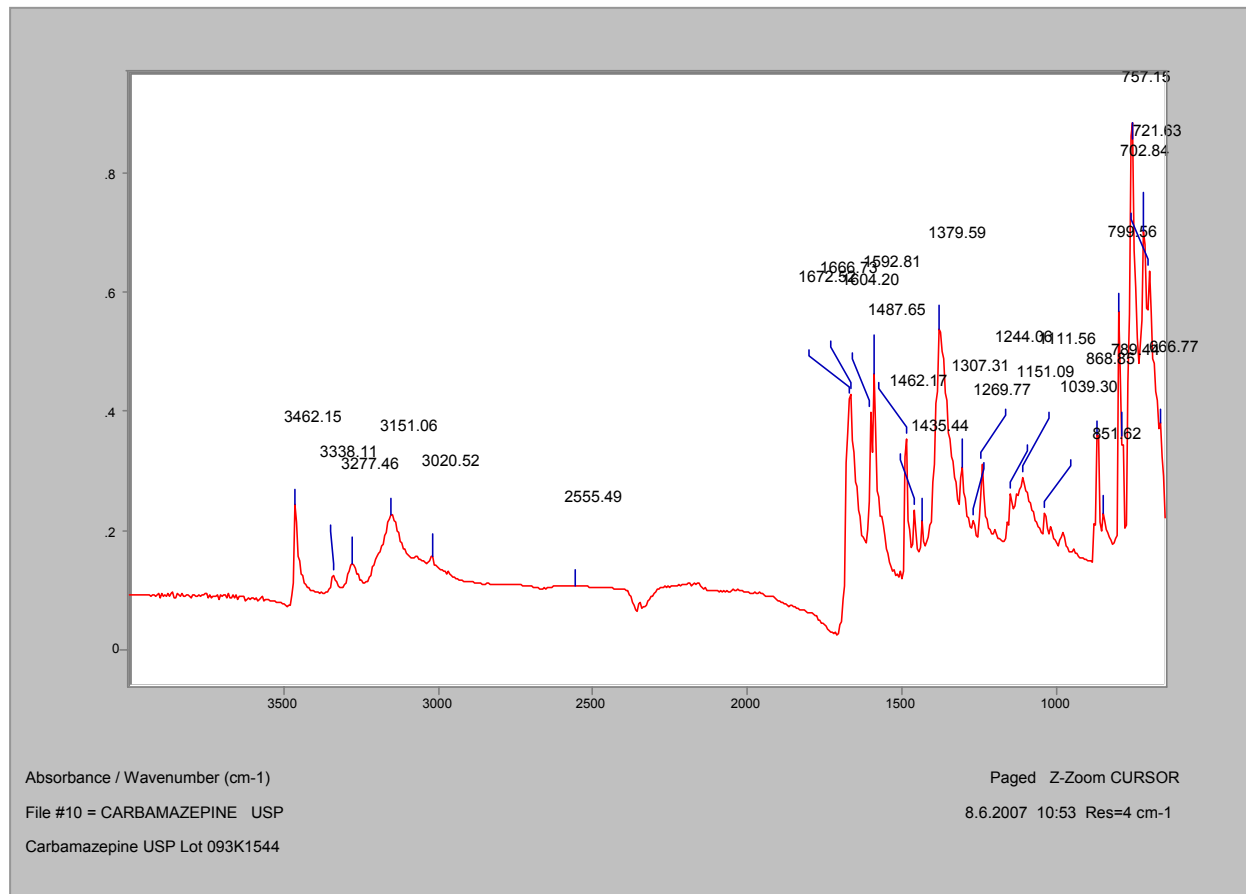
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9. Appendix

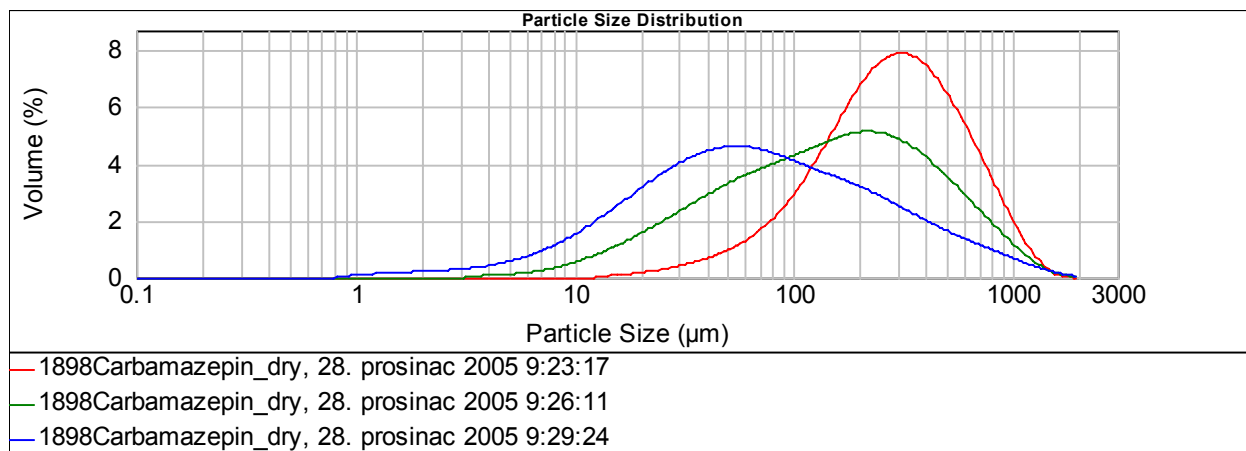
Table 9.1. Specification for CBZ raw material according to Eur.Ph. 5 or USPXXXI (USP31, 2008)

Appearance	White or almost white crystalline powder
Solubility at 25°C	Very slightly soluble in water, freely soluble in methylene chloride, sparingly soluble in acetone and in alcohol
Identification by IR and	
Melting point	189 – 193°C
Acidity/Alkalinity	Not more than 1ml of 0,01N NaOH/HCl is required for 1g of carbamazepine
Assay (calculated on dry substance)	98-102%
Related Substances/Impurities*:	Impurity A max. 0,1% Impurity E max. 0,1% Total impurities max. 0,5%
Chloride	Max. 140ppm
Heavy metals	Max. 20ppm
Loss on drying	Max. 0,5%
Sulphated ash	Max. 0,1%

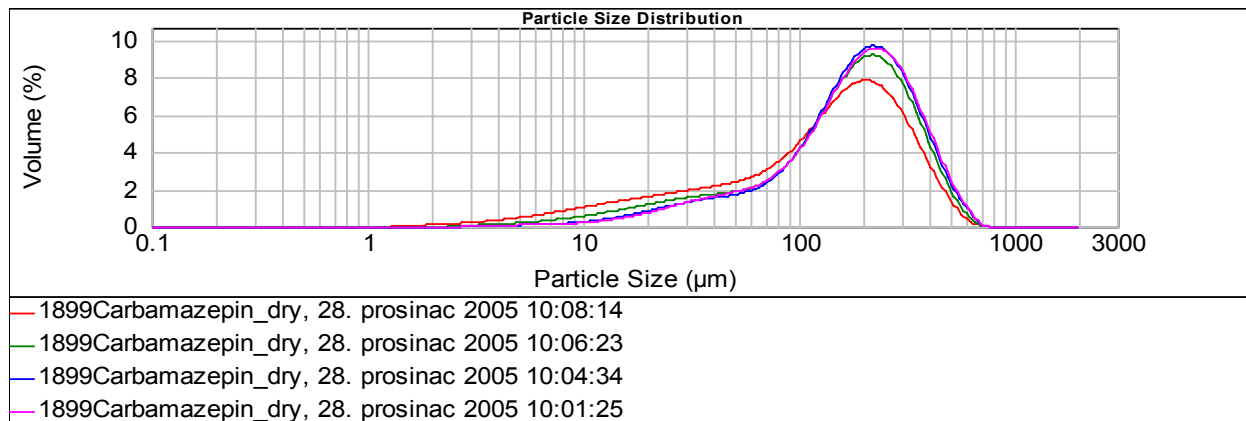
*Impurities: A–10,11dihydrocarbamazepine; B–9-methacrylidine; C–N-carbamoylcarbamazepine; D–iminostilbene and E–iminodibenzyl.



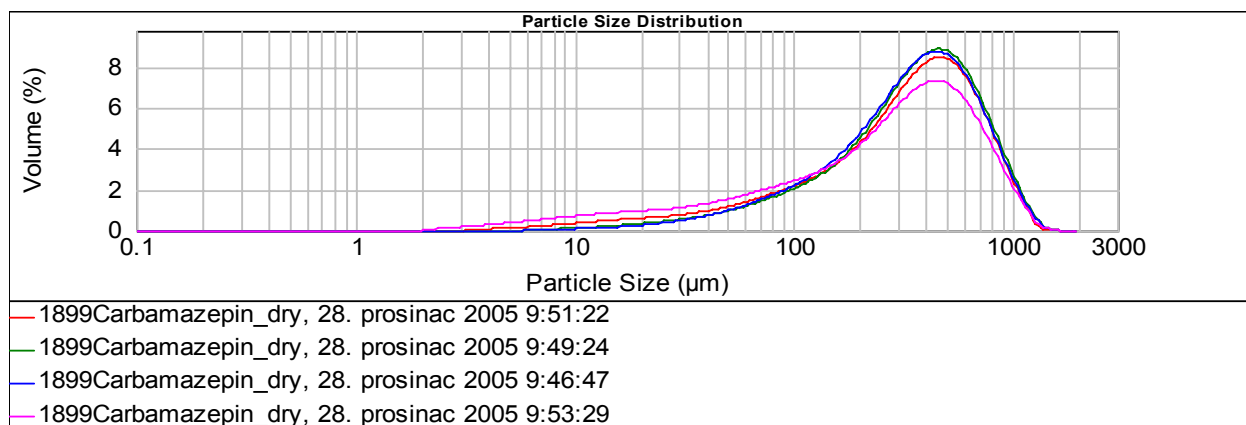
Appendix 9.2. FTIR spectrum of CBZ USP standard



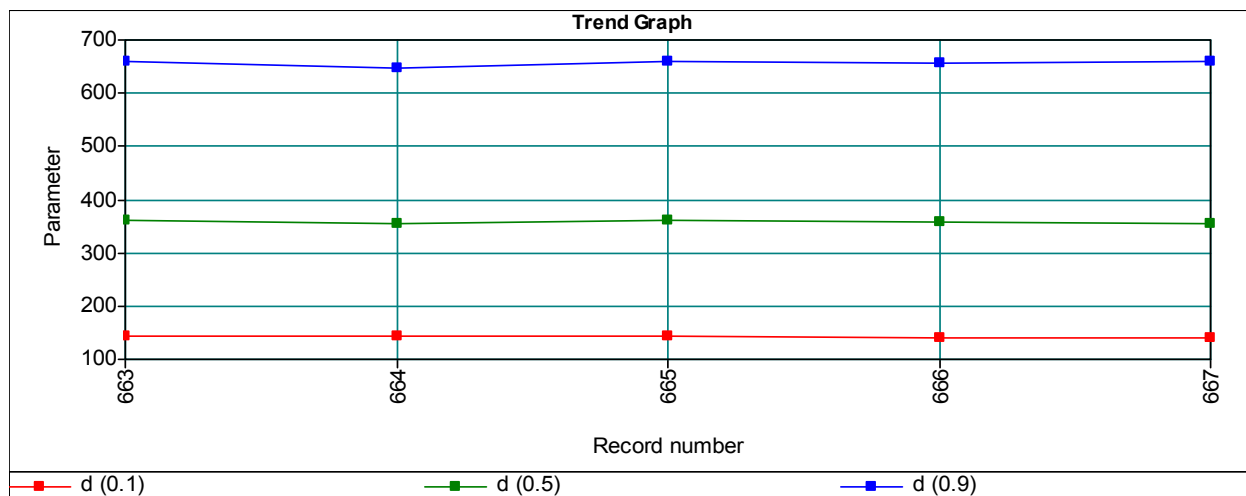
Appendix 9.3 Particle size distribution of CBZ A in function of applied pressure red 0.1bar; green 0.5bar; blue 1.0bar.



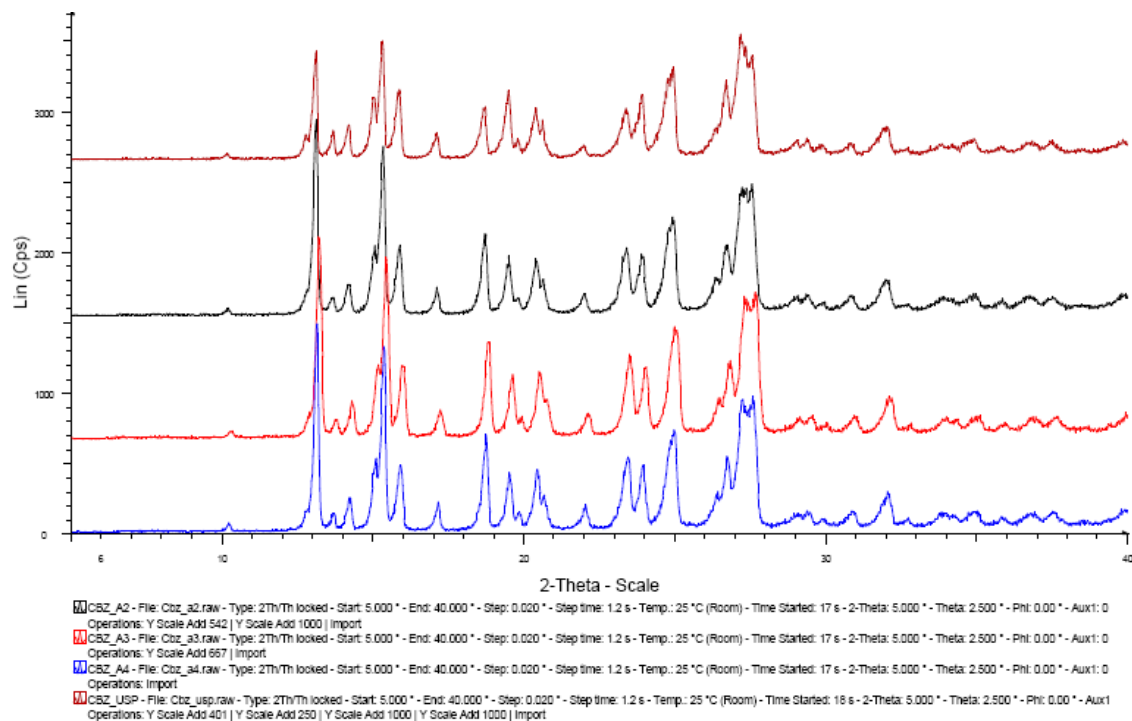
Appendix 9.4. Particle size distribution of CBZ B in function of applied pressure red 0.1bar; green 0.25bar; blue 0.5bar and pink 1.0bar.



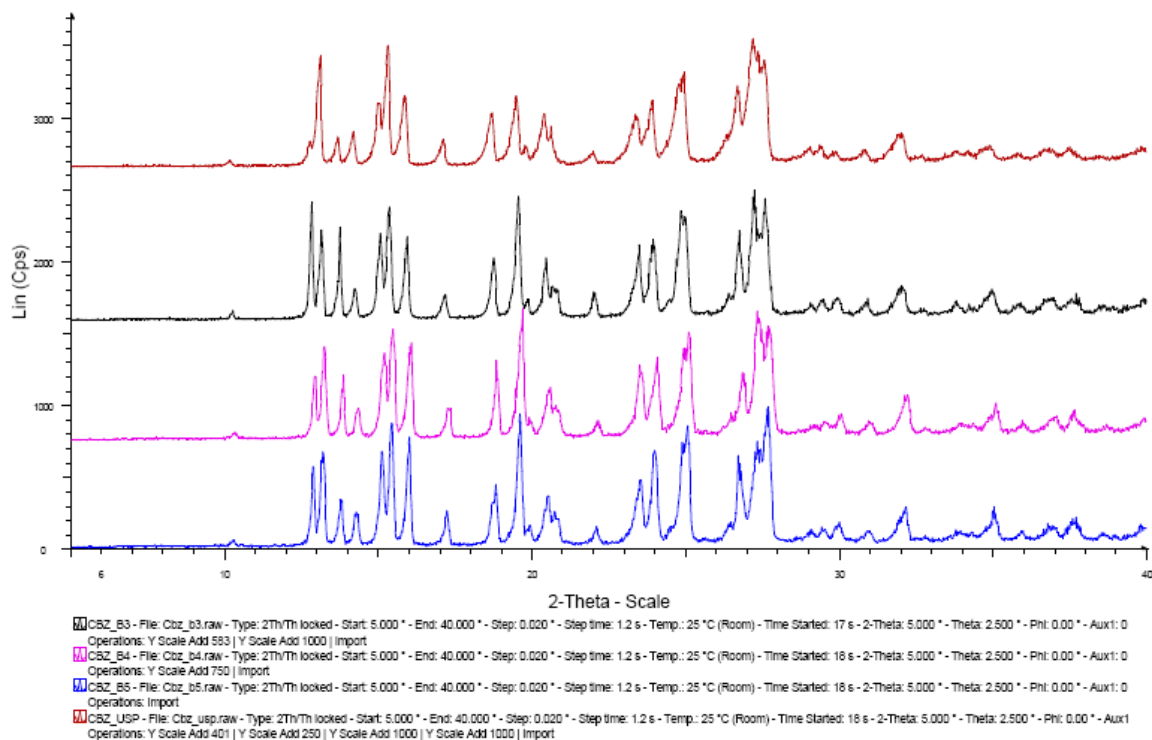
Appendix 9.5. Particle size distribution of CBZ P in function of applied pressure red 0.1bar; green 0.25bar; blue 0.5bar and pink 1.0bar



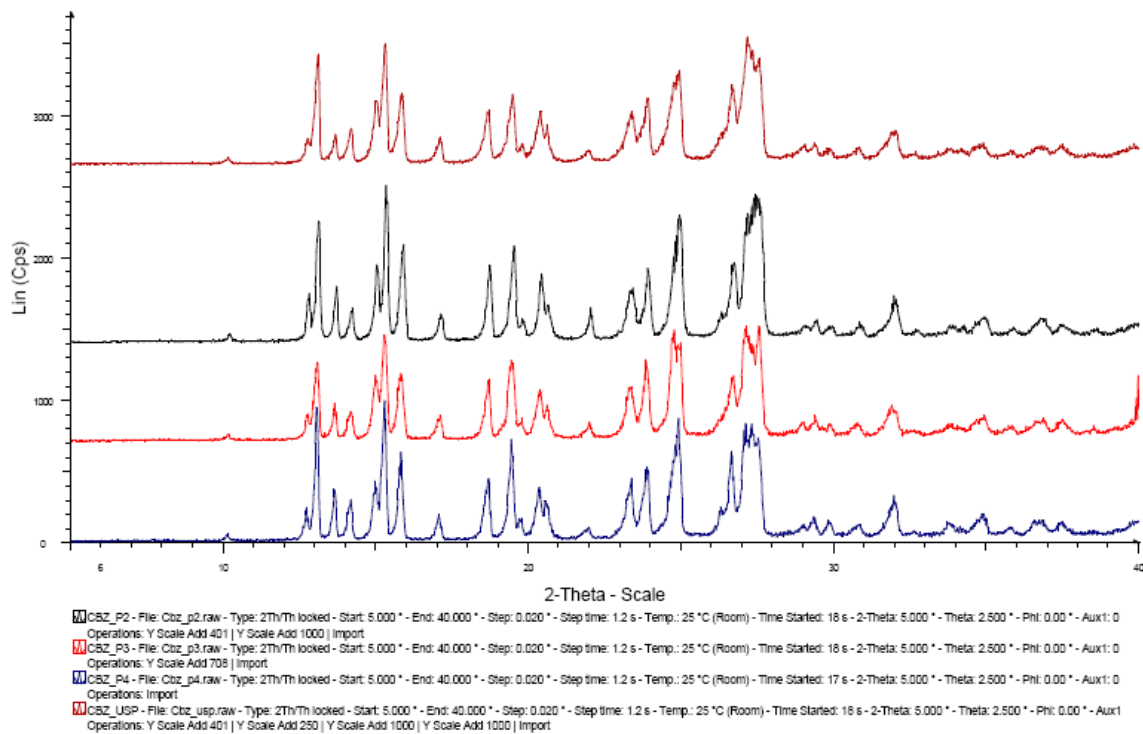
Appendix 9.6. Trend graph of 5 consecutive measurements of CBZ are showing stabile dispersion



Appendix 9.7. X-ray diffractograms of CBZ A samples in comparison with CBZ USP



Appendix 9.8. X-ray diffractograms of CBZ B samples in comparison with CBZ USP



Appendix 9.9. X-ray diffractograms of CBZ P samples in comparison with CBZ USP

Curriculum Vitae

Personal data:

Name	Selma Šehić
Date of birth	17 th of July 1977
Nationality	Bosnian

Education:

1992 – 1996	High school at Gymnasium, Visoko, Bosnia and Herzegovina
1996 – 2003	Study in Pharmacy at the University of Pharmacy in Sarajevo, Bosnia and Herzegovina
2004	State Exam in Pharmacy, Sarajevo, Bosnia and Herzegovina
2004 – 2008	PhD study at the University of Basel, Institute of Pharmaceutical Technology

Professional experience:

2003	Six month of practical work in the pharmacy “Apoteke Sarajevo”, Bosnia and Herzegovina
Since March 2003	In the pharmaceutical company “Bosnalijek dd”, Sarajevo, Bosnia and Herzegovina; (Development Department, Preformulation)
2003	1 year of the practical trainee in pharmaceutical technology in the Production Department, in “Bosnalijek dd”, Bosnia and Herzegovina
2005 - 2007	Assistant in practical courses of solid dosage formulations at the Institute of Pharmaceutical Technology, University of Basel